

Accepted Manuscript

Waste mitigation: From an effluent of apple juice concentrate industry to a valuable ingredient for food and feed applications

Marco G. Cruz, Rita Bastos, Mariana Pinto, João M. Ferreira, João F. Santos, Dulcineia Ferreira Wessel, Elisabete Coelho, Manuel A. Coimbra



PII: S0959-6526(18)31445-8

DOI: [10.1016/j.jclepro.2018.05.109](https://doi.org/10.1016/j.jclepro.2018.05.109)

Reference: JCLP 12966

To appear in: *Journal of Cleaner Production*

Received Date: 14 December 2017

Revised Date: 9 March 2018

Accepted Date: 14 May 2018

Please cite this article as: Cruz MG, Bastos R, Pinto M, Ferreira JoãM, Santos JoãF, Wessel DF, Coelho E, Coimbra MA, Waste mitigation: From an effluent of apple juice concentrate industry to a valuable ingredient for food and feed applications, *Journal of Cleaner Production* (2018), doi: 10.1016/j.jclepro.2018.05.109.

This is a PDF file of an unedited manuscript that has been accepted for publication. As a service to our customers we are providing this early version of the manuscript. The manuscript will undergo copyediting, typesetting, and review of the resulting proof before it is published in its final form. Please note that during the production process errors may be discovered which could affect the content, and all legal disclaimers that apply to the journal pertain.

Wordcount: 8039 words.

Waste Mitigation: from an effluent of apple juice concentrate industry to a valuable ingredient for food and feed applications

Marco G. Cruz¹, Rita Bastos¹, Mariana Pinto¹, João M. Ferreira¹, João F. Santos¹, Dulcineia Ferreira Wessel², Elisabete Coelho^{1,*}, and Manuel A. Coimbra¹

¹ QOPNA, Departamento de Química, Universidade de Aveiro, 3810-193 Aveiro, Portugal

² Escola Superior Agrária do Instituto Politécnico de Viseu, Estrada de Nelas, Ranhados, 3500-606 Viseu, Portugal

* Corresponding author. Tel.: +351 234 370706; fax: +351 234 370084.

E-mail address: ecoelho@ua.pt (Elisabete Coelho)

1 Abstract

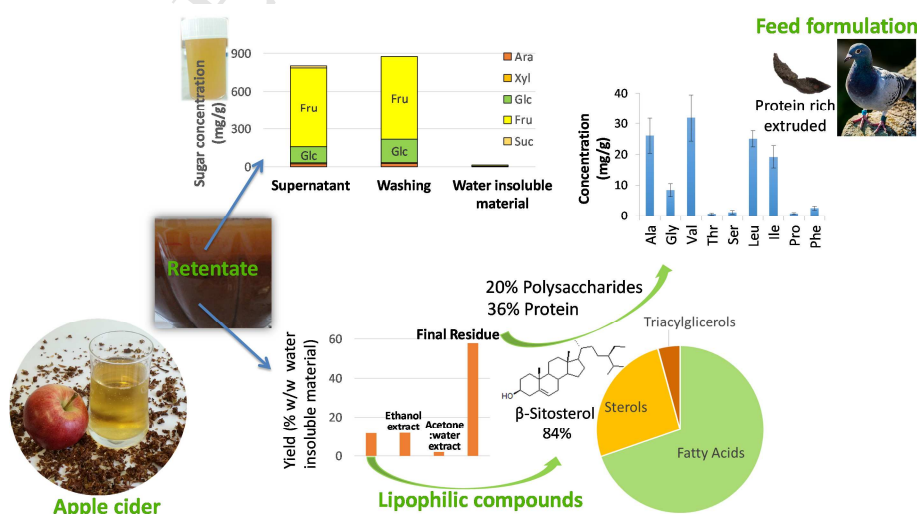
2 Retentate is a by-product of the concentrate apple juice industry, resultant from clarification through
 3 an ultrafiltration process. It has a liquid to sludgy appearance, with 8% of total solids content, usually
 4 discarded as industrial waste, conveyed as wastewater directly to the sewage plant. However, its
 5 origin and expected composition may allow to define its use as a source of valuable compounds as
 6 well as its application in food and feed. The present work shows that retentate is very rich in
 7 carbohydrates, namely 40% fructose (dry weight), glucose (8%), oligosaccharides (5%), and
 8 polysaccharides (3%). It is also rich in protein (8%) and an available and inexpensive source of β -
 9 sitosterol (0.6%). This was the major sterol identified, accounting for 21% of total lipophilic
 10 compounds recovered by *n*-hexane. The retentate suspension was successfully used as nutritive
 11 medium for production of cider by a microbrewery and the protein-rich water insoluble material
 12 (28% of protein) was successfully used in feed formulations for racing pigeons.

13

14

15 **Keywords:** Retentate; Carbohydrates; Amino acids composition; Lipophilic compounds; β -
 16 Sistosterol; Apple cider.

17



18

19 **1. Introduction**

20 According to the Food and Agriculture Organization (FAO) of the United Nations, the global
21 production of apples was 85 million tons in 2014 (FAOSTAT, 2017). The majority are consumed as
22 fresh fruit, while 25 to 30% are converted into processed products, with apple juice concentrate as
23 the main product (65%) (Bhushan et al., 2008).

24 Worldwide, the apple juice is the second most popular juice, after orange juice (European Fruit
25 Juice Association, 2014; Huebner and Kienzle, 2001; Protzman, 2016; United States Department of
26 Agriculture, 2016). After extraction of apple juice, large quantities of by-products are generated,
27 namely apple pomace, which accounts approximately to 25% of fresh apple weight. In recent years,
28 a broad range of applications have been described for apple pomace - namely animal feed, pectin
29 recovery (O'Shea et al., 2012), extraction of phytochemicals (Bhushan et al., 2008; O'Shea et al.,
30 2012), bioproduction of high value-added products, such as enzymes, organic acids, and biofuels
31 (Dhillon et al., 2013) and recently multi-valorisation including scaffold for tissue engineering (Yates
32 et al., 2017). As new environmental rules for industrial waste disposal have become stricter, the
33 reusing of residues and by-products is an advantage for economically viable solutions. Recently,
34 agro-industrial wastes and by-products reutilization has been adopted in a sustainable process, using
35 the biorefinery concept (Mirabella et al., 2014). The valuation of food industry wastes, using a multi-
36 valorisation approach with integral utilization of apple pomace (Yates et al., 2017) or an integrated
37 approach for pineapple waste valorisation (Seguí Gil and Fito Maupoey, 2018), has been proposed.

38 Since the majority of apple juice (90%) is consumed as clarified juice (Huebner and Kienzle,
39 2001), a mode of consumption that still persists nowadays, ultrafiltration is an important step in
40 large-scale industrial production, aiming to remove suspended solids and substances that cause haze
41 and turbidity (Bruijn and Bórquez, 2006). The accumulation of carbohydrates, polyphenols and/or
42 proteins on the ultrafiltration membrane, results in an organic filtration residue named retentate
43 (Bruijn and Bórquez, 2006). The retentate has liquid to sludgy appearance with a total solids content

44 between 5 and 15% whereas the permeate occurs as a concentrate of 70% of total solids and is the
45 main product of the concentrated apple juice industry. The profitability of the process is closely
46 related to the higher recovery of sugars from the fruits to the juice.

47 Unlike apple pomace, few applications have been described for the by-product released after
48 juice clarification. The retentate has been proposed for use in agriculture, mainly applied to fields or
49 as animal fodder, or applied directly into the soil (Huebner and Kienzle, 2001). However, this by-
50 product is usually disposed by landfill, incineration, or industrial wastewater treatment plants, which
51 have a cost to the producer and create environmental problems. The management of apple juice
52 wastewater has been improved, however, with low profitable solutions (Barrantes Leiva et al., 2014;
53 Virmond et al., 2012). The juice processing industry is claiming attention due to the generation of
54 large amounts of effluents with properties that turn them into potential pollution sources if
55 improperly discarded. In a sustainable process, reutilization should be adopted, namely by mitigation
56 of the amount of residue from juice clarification (retentate) that is conveyed directly to the sewage
57 plant. This will allow driving the retentate within the industrial process, maintaining its food grade,
58 into new applications in food and feed fields, with advantage of reducing the organic charge of
59 wastewater. The studies already available concerning the retentate valuation as a by-product,
60 described as apple pomace sludge, exploit its use for bioproduction of citric acid (Dhillon et al.,
61 2011; Dhillon et al., 2013) and insect diets (Dhillon et al., 2013).

62 The retentate has a total solids content of 115-135 g L⁻¹, from which 56-66 g L⁻¹ are
63 carbohydrates, 29-34 g L⁻¹ protein, and 5-6 g L⁻¹ lipids; it also contains a large range of micronutrient
64 elements (Dhillon et al., 2013). To enhance knowledge on the retentate composition, retentate
65 samples obtained directly from an apple juice concentrate industry were analysed concerning the
66 type of carbohydrates, amino acids, fat and sterols composition. This allowed to obtain fractions rich
67 in compounds with possible application in food and feed industry, namely its use as nutritive
68 medium for production of apple cider, as a β -sitosterol source for nutraceutical applications, and as

69 protein-rich material for production of feed formulations, driving towards a “zero waste” approach in
70 the apple juice industry.

71

72 **2. Materials and methods**

73 *2.1. Sequential extraction of the retentate*

74 The retentate samples were supplied by Indumape, S.A., Portugal, throughout one year. The
75 retentate resulted industrially from the ultrafiltration of the apple juice followed by the washing of
76 the retained material with water, in a process named diafiltration. From these, for the complete
77 analysis performed, two samples of retentate, collected in different seasons of the same year, were
78 used. The retentate suspensions (150 g) were centrifuged at 15,000 rpm, at 4 °C during 20 min to
79 separate soluble and insoluble material. Then, the insoluble material was sequentially washed with
80 water (40 °C, 120 mL, 15 min). Due to the yields reproducibility of the retentates analysed, only one
81 sample of water insoluble material was used for the extraction with: [1] *n*-hexane (soxhlet, 150 mL,
82 5 h); [2] ethanol with 1% (v/v) of acetic acid (20 °C, 25 mL, 1 h); [3] acetone:water (6:4, v/v) with
83 1% acetic acid (20 °C, 25 mL, 1 h). The 2nd and 3rd extraction steps were repeated five times each.
84 After each extraction, the soluble material was separated from the insoluble material by
85 centrifugation (15,000 rpm, 4 °C, 20 min) (Figure 1). Each extract and residue were frozen and
86 freeze-dried. Regarding to ethanol, acetone:water, and soxhlet extraction, the solvent was evaporated
87 to dryness by rotary evaporation.

88

89

Figure 1.

90 *2.2. Sugar analysis*

91 Neutral sugars were analysed by gas chromatography-flame ionization detection (GC-FID) after
92 conversion to their alditol acetates. The quantification was carried out using 2-deoxyglucose as
93 internal standard. Monosaccharides were released from polysaccharides with pre-hydrolysis of the

94 samples using 0.2 mL of 72% (w/w) H₂SO₄ for 3 h at room temperature followed by 2.5 h hydrolysis
95 in 1 M H₂SO₄ at 100 °C. After 1 h hydrolysis, it was collected 0.5 mL for uronic acids determination.
96 After hydrolysis, the reduction and acetylation of the monosaccharides were performed, and the
97 alditol acetates were analysed by GC-FID using a DB-225 column (30 m, 0.25 mm, 0.25 µm) and a
98 GC-FID PerkinElmer-Clarus 400 (Bastos et al., 2015). For the determination of free sugars
99 composition, including sucrose, the hydrolysis step was omitted and the alditol acetates formed were
100 analysed using a capillary column DB-1 (30 m, 0.25 mm, 0.15 µm). The oven temperature program
101 was as follows: 100 °C to 350 °C at a rate of 20 °C min⁻¹ (1 min). The temperature of injector was
102 250 °C and the detector was 300 °C. Hydrogen was used as the carrier gas. The free sugars were
103 identified and quantified based on their retention times and response factors obtained by injection of
104 standards. Uronic acid content was determined by 3-phenylphenol colorimetric method. The
105 quantification was performed using galacturonic acid as standard (Bastos et al., 2015).

106

107 2.3. Size exclusion chromatography

108 Preparative size exclusion chromatography was carried out on a Pharmacia Biotech XK 16
109 chromatography column (70 cm length × 1.6 cm diameter) containing Biogel P-2, using a flow rate
110 of 0.28 mL min⁻¹. Total (V_t) and void (V₀) volumes were calibrated with glucose (180 Da) and blue
111 dextran (2 MDa), respectively. The calibration with stachyose (DP4) and sucrose (DP2) was also
112 performed. The column was equilibrated with distilled water and the supernatant of the retentate
113 sludge (1 mL) was loaded. Fractions (1.5 mL) were collected and assayed for sugars with
114 evaporative light scattering detection (Coelho et al., 2016). Additionally, the absorbance was
115 measured at 280 nm. Based on the chromatographic profiles, the eluate was combined in 4 fractions
116 (A-D), evaporated, frozen, and freeze-dried.

117

118 2.4. Protein and amino acids analysis

119 The nitrogen content of retentate sludge, water insoluble material, and final residue were
120 determined by elemental analysis. In order to convert the nitrogen content in protein content, a
121 Kjeldahl factor for apple samples (5.72) was used (Sosulski and Imafidon, 1990).

122 The Bicinchoninic Acid Kit for Protein Determination (Sigma-Aldrich) was used to determine
123 the soluble protein in fractions A and B obtained from size exclusion chromatography.

124 The amino acids composition of the water insoluble material and final residue was determined
125 after acid hydrolysis of protein and derivatization for gas chromatography analysis (Coimbra et al.,
126 2011). 1 mL of HCl 6 M was added to the sample (5 mg) and acid hydrolysis was performed during
127 24 h at 110 °C, using norleucine 5.0 mM as internal standard. The derivatization was performed
128 with: [1] HCl 3 M in isobutanol (200 µL, 120 °C, 10 + 30 min); [2] 0.2 mg mL⁻¹ Butylated
129 hydroxytoluene (BHT) prepared in ethyl acetate (200 µL); [3] heptafluorobutyric anhydride (100 µL,
130 150 °C, 10 min). The amino acids were separated and analysed by GC–qMS using a Shimadzu
131 GCMS-QP2010 Ultra. The GC was equipped with a DB-1 (J&W Scientific, Folsom, CA, USA)
132 capillary column (30 m, 0.25 mm, 0.15 µm). The sample was injected in “split” mode with the
133 injector temperature of 250 °C, during 5 min. The temperature program used was as follows: initial
134 temperature was 70 °C for 1 min, increasing to 170 °C at a rate of 2 °C min⁻¹, followed by a linear
135 increase of 16 °C min⁻¹ until 250 °C, then maintained at 250 °C for 5 min. The GC was connected to
136 a mass quadrupole selective detector operating with an electron impact mode at 70 eV and scanning
137 the range *m/z* 40–500. Calibration curves for Ala, Val, Leu, Asx, and Glx were obtained in the
138 concentration range of 0–0.2 mg mL⁻¹; for Gly, Thr, Ser, Ile, Pro, Phe, Lys, and Tyr the concentration
139 range was 0–0.025 mg mL⁻¹.

140

141 2.5. *Lipophilic compounds analysis*

142 To quantify free lipophilic compounds, the dried soxhlet extract (20 mg) and accurate amount of
143 internal standard (tetracosane, 1 mg) were dissolved in 250 µL of pyridine. The compounds

144 containing hydroxyl and carboxyl groups were converted into trimethylsilyl (TMS) ethers and esters,
145 respectively, by adding 250 μL of N,O-bis(trimethylsilyl)trifluoroacetamide and 50 μL of
146 trimethylchlorosilane. The mixture was kept at 70 $^{\circ}\text{C}$ during 30 min (Vilela et al., 2014). Compounds
147 were identified as TMS derivatives by comparing their mass spectra with the GC-MS spectral
148 library and also with literature of MS fragmentation (Vilela et al., 2014). For correct quantification,
149 the chromatographic respective response factors of each compound family were calculated in
150 relation to tetracosane using (Z)-nonadec-10-enoic acid for fatty acids, cholesterol for sterols, decan-
151 1-ol for long chain aliphatic alcohols.

152 To quantify total lipophilic compounds (free and esterified), the alkaline hydrolysis reaction was
153 performed. Briefly, the dried soxhlet extract (30 mg) was dissolved in 10 mL of KOH 1 M in 10%
154 aqueous methanol. The mixture was kept at 100 $^{\circ}\text{C}$ during 60 min, under a nitrogen atmosphere.
155 After cool down, the mixture was acidified with HCl 1M until $\text{pH} \approx 2$ and then extracted three times
156 with dichloromethane. After evaporation of organic solvent, the lipophilic compounds were
157 converted into trimethylsilyl (TMS) ethers and esters and analysed as previously described. The
158 fraction of esterified compounds was calculated considering the concentration of lipophilic
159 compounds and the amount of free lipophilic compounds.

160 To quantify fatty acid methyl esters (FAME) 0.8 mL of the heptadecanoate methyl ester (0.5 g
161 L^{-1} in *n*-hexane) was added to the dried soxhlet extract (10 mg). Then, 0.2 mL of methanolic
162 solution of KOH (2 M) was added. The mixture was shaken and 2 mL of saturated sodium chloride
163 solution was added. The sample was centrifuged at 2,000 rpm during 5 min (Aued-Pimentel et al.,
164 2004). After that, 1 mL of organic phase was collected and analysed by a GC-FID PerkinElmer-
165 Clarus 400 equipped with a capillary column DB-FFAP (30 m, 0.32 mm, 0.25 μm). The FAMES
166 were identified based on their retention times obtained by injection of commercial FAMES mixture
167 ($\text{C}_8\text{-C}_{24}$).

168

169 2.6. *Total phenolic compounds and antioxidant activity*

170 The total phenolic compounds of the ethanol and acetone:water extracts were determined by the
171 Folin-Ciocalteu method (Singleton and Rossi, 1965). Solutions of ethanol extract (6 mg mL^{-1}) and
172 acetone:water extract (1 mg mL^{-1}) were prepared using the respective extraction solvent.
173 Quantification was obtained by correlation to the calibration curve of gallic acid standard solutions
174 and the total phenolic compounds were expressed as gallic acid equivalents.

175 The antioxidant activity of ethanol and acetone:water extracts was determined by DPPH
176 (Villaño et al., 2007) and ABTS (Re et al., 1999) methods. Additionally, for comparison purposes,
177 the antioxidant activity of ascorbic acid and quercetin was determined using both methods.

178

179 2.7. *Estimation of procyanidin DPn*

180 The procyanidins fractionation was performed according to methanol/chloroform graded
181 precipitations (Passos et al., 2010). The acetone:water extract (15 mg) was dissolved in 1.5 mL of
182 water with 5% (v/v) of acetic acid and the insoluble material was separated by centrifugation (15,000
183 rpm, $4 \text{ }^{\circ}\text{C}$, 20 min). A liquid-liquid extraction with ethyl acetate was performed to the supernatant,
184 three times. Both organic and aqueous phases were evaporated to dryness. Then, the residue from the
185 aqueous phase was redissolved in methanol (1 mL) and the insoluble material was separated by
186 centrifugation. The supernatant was submitted to successive additions of chloroform until a new
187 precipitate was formed (Supplementary Material Figure S1). The precipitate material was separated
188 by centrifugation. Each precipitate and final extract were then rotary-evaporated with several
189 additions of water to completely remove the organic solvent, frozen, and freeze-dried. The average
190 degree of polymerisation (DPn) was estimated from the calibration curve: $y = -0.0743x + 11.24$; $r^2 =$
191 0.7278 (Passos et al., 2010).

192

193 2.8. *Glycosidic-linkage analysis*

194 Glycosidic-linkage composition was determined by GC-qMS of the partially methylated alditol
195 acetates, using methyl iodide in NaOH/DMSO as alkylating agent and TFA 2 M for hydrolysis
196 (Bastos et al., 2015).

197

198 2.9. Cellulase hydrolysis

199 The enzymatic hydrolysis was performed based on the procedures described by Bastos et al.
200 (2015). The final residue (30 mg) was suspended in 20 mL of 20 mM acetate buffer pH 5.0 at 37 °C
201 and hydrolysed with cellulase (EC 3.2.1.4) from *Aspergillus niger* (Sigma-Aldrich) 1.44 U/mg.
202 Enzymatic hydrolysis was performed during 24 h followed by 24 h, in a total of 48 h. Every 24 h, the
203 hydrolysed material was separated from residue by centrifugation (15,000 rpm, 4 °C, 20 min) and the
204 reaction was stopped by boiling the test tube for 10 min. The material was purified by size exclusion
205 chromatography on Biogel P-2 and analysed by light scattering, as described in Section 2.3.

206

207 2.10. Exploitation of retentate for food and feed applications.

208 The retentate was used to prepare cider, allowing to develop a nutrient medium essential for
209 yeast metabolism during fermentation, by complementing apple juice concentrate, which is deficient
210 in amino acids and minerals. For this, an apple cider was prepared with 200 L of apple juice
211 concentrate diluted at 12 °Brix with the addition of 200 kg of retentate, both supplied from
212 Indumape, S.A., Portugal. Retentate was previously macerated with malt Pilsen at 45-50°C during 30
213 min, in a proportion of 10:1. Fermentation was carried out in Vadia microbrewery, Essência D'Alma
214 Lda, Portugal, using a lager yeast (saflager w-34/70, Fermentis) in a 1,000 L bioreactor at 10-12 °C,
215 during one week.

216 A feed formulation using 15% of dried retentate water insoluble material was also prepared for
217 racing pigeons, nutritionally adjusted for the competition period, containing approximately 3,400
218 kcal/kg, with 56% carbohydrates, 22% protein, 9% fat, 6% fibre, and 4% ash. The retentate used in

219 the new formulation replaced 20% of soymeal protein in the original formulation. The blend of the
220 sieved raw materials (1.5 kg) was extruded using a single screw extruder (Periplast model Ø25 x
221 25D) and the extrudates were then oven dried at 60 °C during 30 min until reaching a moisture
222 content of less than 10%. After cooling, the extruded feed was stored in plastic bags at room
223 temperature.

224

225 **3. Results and Discussion**

226 The water content of retentate (apple juice sludge) was 83% just after the ultrafiltration step,
227 increasing to 92% in the retentate, after diafiltration, which is in accordance with the 87-89%
228 described for apple juice sludge (Dhillon et al., 2013). When it is necessary to decolorize the juice
229 concentrate, due to a more brownish colour than that desirable, the industry uses activated charcoal,
230 which increases the amount of solids of the retentate, reaching 20%. In the present study, the
231 retentates used were not submitted to this decolorizing step. On a dry weigh basis, the retentates
232 under study were constituted by 53% of carbohydrates, of which 51% were free sugars, mainly
233 fructose (78 mol%), glucose (16 mol%), arabinose (3 mol%), and sucrose (2 mol%), in accordance
234 with the 49% of total carbohydrates, on a dry weigh basis, reported for the apple juice sludge
235 (Dhillon et al., 2013). They also contained 8% protein and 3% of lipophilic compounds. Although
236 the lipophilic compounds are in accordance to the amount of lipids reported for apple juice sludge
237 (4%), the amount of protein was much less than the reported 25% (Dhillon et al., 2013), showing that
238 the uncharacterized material of the retentates should be protein derived compounds.

239 The centrifugation of the retentate resulted in a supernatant containing 57% of the retentate total
240 solids and 89% of free sugars. The soluble protein accounted for 4%. The washing of the residue
241 allowed to recover an extra 6% of retentate total solids and 10% of free sugars. The remaining water
242 insoluble material accounted for 25% of retentate total solids, containing 16% of carbohydrates and
243 28% of insoluble protein.

244

245 *3.1. Free sugars*

246 The retentate supernatant and washing allowed to recover 99% of the retentate monosaccharides.
 247 Both fractions were rich in sugars, constituted by 79% and 88% of monosaccharides, respectively
 248 (Table 1). These monosaccharides are mainly fructose (79 mol% and 75 mol% for supernatant and
 249 washing) and glucose (16 mol% and 21 mol%). This sugar composition is in accordance with the
 250 apple juice composition reported in literature (Thavarajah and Low, 2006), as the liquid part of the
 251 retentate is apple juice not recovered through the ultrafiltration process because the ultrafiltration is
 252 stopped when 40% of solids are attained in the feed tank.

253

254 **Table 1.** Carbohydrate composition of the fractions obtained by the sequential extraction of retentate.

Sample	Carbohydrate (mol%)										Total carbohydrate* (mg g ⁻¹)	
	Rha	Fuc	Ara	Xyl	Man	Gal	Glc	Fru	Suc	UA		
Supernatant												
Monosaccharides			3	1			16	79	1			794±20
Washing												
Monosaccharides			3	1			21	75				877±24
Water insoluble material												
Monosaccharides			16	16			24	44				14±2
Polysaccharides	1	1	9	6	5	20	44			14		142±14
Final residue												
Polysaccharides	1	1	8	7	6	18	47			12		200±7

255 *Values expressed in mg of anhydrous sugars by g of sample.

256

257 Size-exclusion chromatography of the supernatant material showed a chromatographic profile
 258 (Fig 2a) that allows to observe that this material was constituted by a large amount of
 259 monosaccharides (Fraction D) and a small amount of disaccharides (DP2, fraction C). These results
 260 are in accordance with the high content of monosaccharides and 1% of sucrose determined by free
 261 sugar analysis (Table 1). Furthermore, two fractions (A, B) with molecular weight material lower

262 than 2 kDa, the exclusion limit of the gel, but higher than the molecular weight of fractions C and D,
263 were also observed, suggesting the presence of oligosaccharides with DP higher than 4. The high
264 absorbance at 280 nm of both fractions could also indicate the presence of protein. The protein
265 analysis showed that fraction B was composed by $59.5\pm 0.5\%$ of protein and fraction A was
266 constituted by $13.1\pm 1.4\%$. As apple juice is constituted also by several phenolic compounds (Spanos
267 and Wrolstad, 1992), the absorbance at 280 nm may also be indicative for the presence of phenolic
268 compounds in these two fractions. Nevertheless, these fractions are very rich in free sugars, which
269 can be returned to the apple juice processing line, increasing the profitability of the process by the
270 increase of the amount of soluble sugars and, consequently, the °Brix of apple juice concentrate.

271

272 Figure 2.

273

274 *3.2. Lipophilic compounds*

275 The retentate lipophilic fraction was obtained by soxhlet extraction with *n*-hexane from the
276 water insoluble material, yielding 3% on a dry weight basis of the whole retentate and 11.7% on a
277 dry weight basis of the retentate water insoluble material. The identification and quantification of the
278 lipophilic compounds, analysed by GC-qMS for silylated derivatives of free fatty acids, sterols and
279 long chain alcohols, and by GC-FID for methyl esters of transesterified fatty acids, is summarised in
280 Table 2. This approach allowed to identify 15 fatty acids, 6 sterols, 2 long chain aliphatic alcohols,
281 and one long chain diacid. Approximately 94% of all compounds were in free form, the free fatty
282 acids being the most predominant class (68.8%). Triacylglycerides represent only 4.1% of the
283 lipophilic compounds, mainly constituted with linoleic (C18:2), palmitic (C16:0), oleic (C18:1), and
284 stearic (C18:0) acids, in accordance with other reports of apple seed (Bada et al., 2014; da Silva and
285 Jorge, 2016). The high occurrence of free fatty acids shows that the majority of apple seed
286 triacylglycerides were deesterified. It is possible that deesterification occurs during the processing of
287 apple juice, although a large amount of free fatty acids have been reported to be constituent of

288 unprocessed apple seeds (Lu and Yeap Foo, 1998). Free fatty acids have also been reported as
 289 constituents of apple skin surface waxes, which may also be an origin of retentate free fatty acids
 290 (Verardo et al., 2003). Palmitic and linoleic acids correspond to the major fatty acids identified,
 291 accounting for 42.0% and 11.5% of the lipophilic compounds and 4.7% and 1.3% of the retentate
 292 water insoluble material, respectively. These high amounts of free fatty acids should be taken into
 293 account when using this material for feed formulations, requiring their removal or dilution in other
 294 fatty sources.

295 Sterols accounted to approximately 24% of the retentate lipophilic compounds, the second most
 296 abundant family. β -Sitosterol is the major free sterol identified and the second major component
 297 present in the sample, accounting for 20% of dry hexane extract and 2.4% of retentate water
 298 insoluble material. Stigmasterol was the only sterol occurring in an esterified form, accounting for
 299 2.0% of lipophilic compounds, and presenting 87% of esterification. These results are in accordance
 300 with the exclusive occurrence of fatty acid esters of phytosterols in cell membranes and the high
 301 abundance of stigmasterol esters in ripen fruits (Whitaker, 2012). Moreover, the two long chain
 302 aliphatic alcohols, which were present mainly in esterified form, may have origin from cuticle waxes
 303 (Belding et al., 1998; Verardo et al., 2003). This contrasts with the free sterols reported to be present
 304 in apple epidermal cortical tissue (Whitaker et al., 1997) and peel (Rudell et al., 2011). The reason
 305 why lipase did not act on wax-derived compounds seems to be also explained by the inhibitory
 306 activity due to the high ursenoic acid content of apple peels (McGhie et al., 2012).

307 Table 2. Lipophilic compounds identified in *n*-hexane extract of retentate water insoluble material (expressed
 308 on a dry weight basis).

Compounds	Concentration (mg.g ⁻¹)		
	Free	Esterified	Total
Fatty acids	647.6±77.2	40.7±11.5	688.3
Octanoic acid (C8:0)	5.3±1.2	0.0	5.3
Dodecanoic acid (C12:0)	0.3±0.00	0.9±0.1	1.2
Tetradecanoic acid (C14:0)	2.2±0.7	0.7±0.0	2.9
Pentadecanoic acid (C15:0)	2.6±0.2	0.2±0.05	2.8
Hexadecanoic acid (C16:0)	401.5±9.5	14.0±2.9	415.5
Heptadecanoic acid (C17:0)	4.3±2.0	0.0	4.3
Octadecanoic acid (C18:0)	53.9±20.6	3.3±0.6	57.2

Eicosanoic acid (C20:0)	26.9±8.5	1.1±0.4	28.0
Heneicosanoic acid (C21:0)	3.9±2.1	1.1±0.2	5.0
Docosanoic acid (C22:0)	8.1±3.1	0.0	8.1
Tricosanoic acid (C30:0)	3.3±3.1	0.0	3.3
Pentacosanoic acid (C25:0)	1.0±0.5	0.0	1.0
Octadec-9-enoic acid (C18:1)	24.6±7.7	3.5±1.0	28.1
Octadeca-9,12-dienoic acid (C18:2)	109.7±18.2	15.2±7.1	124.9
Octadeca-9,12,15-trienoic acid (C18:3)	0.0	0.7±0.0	0.7
Long chain diacids	20.0±2.2	0.0	20.0
Nonanedioic acid	20.0±2.2	0.0	20.0
Sterols	226.2±29.3	16.5	242.7±29.9
Campesterol	9.3±1.0	0.0	9.3±1.0
Fucosterol	2.5±0.8	0.0	2.5±0.8
Stigmasterol	2.4±1.0	16.5	18.9±0.1
β-Sitosterol	203.2±32.5	0.0	203.2±32.5
Stigmasta-3,5-dien-7-one	4.0±1.2	0.0	4.0±1.2
Lanost-8-en-3β-ol	4.8±2.0	0.0	4.8±2.0
Long chain aliphatic alcohols	0.5±0.0	3.8	4.3±0.6
Octadecan-1-ol (C18)	0.2±0.1	3.1	3.3±0.5
Octacosan-1-ol (C28)	0.3±0.0	0.7	1.0±0.1
Total lipophilic compounds	894.3±70.3	61.0	955.3

309

310 The results obtained show that the retentate is a very good source of β-sitosterol (203.2 g kg⁻¹ of
311 lipids) when compared to vegetable oils with high content in β-sitosterol, namely corn oil (3.2-14.7 g
312 kg⁻¹), rapeseed oil (0.4-6.9 g kg⁻¹), soybean oil (0.63-2.9 g kg⁻¹), and olive oil (0.5-2.4 g kg⁻¹)
313 (Alberici et al., 2016). Annona fruits, mainly the peel, contain 20.4-21.6 g kg⁻¹ of oil, which is also
314 reported as a good source of β-sitosterol (García-Salas et al., 2016). The 6.1 g kg⁻¹ content of β-
315 sitosterol found in apple retentate on a dry weight basis, is much higher than the yield reported for
316 rapeseed expeller cake, 0.5-0.6 g kg⁻¹, considered as a good source of this compound (Siger et al.,
317 2016). In addition, considering the apple juice retentate water insoluble material, easily separated by
318 centrifugation, the content of β-sitosterol represents 23.8 g kg⁻¹, which is a much higher figure. The
319 high availability of β-sitosterol in the retentate obtained from concentrated apple juice production
320 allows to propose this food industry by-product as an easy and rich source of β-sitosterol, a highly
321 valued compound as food ingredient, with known properties of cholesterol lowering agent (Gylling
322 and Nissinen, 2015). Easily β-sitosterol, as a neutral compound, can be separated from fatty acids,

323 the main components of *n*-hexane extract, by the deacidification processes used in the refining
324 process of the crude oil (Bhosle and Subramanian, 2005).

325

326 3.3. Procyanidins

327 The retentate phenolic compounds were sequentially extracted from the soxhlet insoluble
328 residue with ethanol and aqueous acetone (Figure 1). The mass yield obtained was 14 and 2.5%,
329 which correspond to 11.9 and 2.1%, respectively, of the retentate water insoluble material and 3.1
330 and 0.5% of the retentate sludge on a dry weigh basis.

331 The ethanol extracted a higher amount of mass, however contained only 1.9% of total phenolic
332 compounds estimated as acid gallic equivalents, whereas acetone:water extract contained 51.3% of
333 acid gallic equivalents (Figure 1). The ethanol soluble material comprised a wide range of
334 compounds that was not quantified as phenolic compounds. Ethanolic extracts of apple peels were
335 already described to contain mainly triterpenic compounds (McGhie et al., 2012). For the ethanolic
336 extract, the antioxidant activity determined as EC₅₀ was 577.6±65.9 µg/mL with DPPH and 273.3±
337 8.5 µg/mL with ABTS. However, the acetone:water extract showed much lower EC₅₀ (12.1±1.5 and
338 8.5±0.5 µg/mL), with the same methods. These values were comparable with the EC₅₀, using DPPH
339 and ABTS, obtained for ascorbic acid (3.7±0.7 and 6.5±0.5 µg/mL) and quercetin (3.8±0.2 and
340 2.1±0.1 µg/mL), showing relevant antioxidant activity. As the acetone:water extracts are usually rich
341 in polymeric procyanidins (Ferreira et al., 2002), to determine the degree of polymerization (DP), the
342 material was dissolved in methanol and fractionated by precipitation adding chloroform (for details,
343 see Supplementary Material Figure S1). The insolubility of 65% of the procyanidins in methanol
344 allowed to infer that the majority of the procyanidins of acetone:water extract had a DP higher than 8
345 (Passos et al., 2010) and the compounds soluble in methanol had the following DP distribution: 8
346 (6.7%), 7 (3.8%), 5 (7.4%), <5 (2.3%) (Supplementary Material Table S1). The low yield of the
347 ethanol and acetone:water retentate extracts seems similar to the results obtained in dried pears,

348 where 86% of the procyanidins remained in final residue (Ferreira et al., 2002). The industrial
349 process involved in the production of concentrated apple juice seems to promote modifications of
350 phenolic compounds that could result from oxidation and from reaction with other polyphenols and
351 polysaccharides that became irreversibly bound. They could no longer be extracted by the standard
352 methods, using methanol or aqueous acetone solvents (Ferreira et al., 2002). It was shown that
353 oxygenation of juice during processing resulted in a significant decrease of all classes of native
354 polyphenols. Catechins and procyanidins were particularly affected by oxidation leading *o*-quinone
355 derivatives catalyzed by polyphenol oxidase (Guyot et al., 2003). Moreover, the lower extraction of
356 procyanidins may result from the association of the procyanidins with the solid part of the fruits,
357 particularly cell-wall materials when fruits are crushed and pressed as was previously shown in a
358 model solution (Renard et al., 2001).

359

360 3.4. Insoluble protein and polysaccharides

361 The insoluble material recovered after water extraction was constituted by 16.1% of
362 carbohydrates, of which 14.2% are polysaccharides. These polysaccharides are composed by glucose
363 (44 mol%), galactose (20 mol%) and uronic acids (14 mol%) (Table 1), suggesting glucans and
364 pectic polysaccharides as the predominant polysaccharides. Additionally, this water insoluble
365 material is rich in protein (28.1±0.3%) and the amino acid composition (Table 3) shows that valine
366 (24.4 mg g⁻¹), leucine (23.6 mg g⁻¹), alanine (22.1 mg g⁻¹) and isoleucine (17.6 mg g⁻¹) were the
367 major amino acids quantified. These amino acids were also those identified in haze-active proteins in
368 apple juice (Wu and Siebert, 2002).

369 The final residue comprised 15.1% of the initial retentate mass weight and 57.9% of the water
370 insoluble material. The final residue was composed of 20.0% polysaccharides and 35.8±0.4% of
371 protein. The remaining 44% should be unextracted material probably containing modified
372 procyanidins bounded to polymeric material or/and products of Maillard reaction between reducing

373 sugars and protein (Coimbra et al., 2011), both giving origin to brownish products, consistent with
 374 the visual appearance of the retentate final residue. Only 30% of the proteic material was quantified
 375 as amino acids after acid hydrolysis. Table 3 shows that the major amino acids were valine (31.8 mg
 376 g⁻¹), alanine (26.0 mg g⁻¹), leucine (25.0 mg g⁻¹), and isoleucine (19.1 mg g⁻¹). The final residue,
 377 compared with the water insoluble residue, was enriched in the majority of the amino acids, with the
 378 exception of proline and hydrophilic amino acids (Table 3). It is possible that the decrease in proline
 379 could be related with the association of oligopeptides rich in proline and catechin or polyflavonoids,
 380 and their co-extraction with acetone:water (Hatano and Hemingway, 1996; Siebert, 1999).

381

382 Table 3. Amino acids content (mg g⁻¹ on a dry weight basis) of retentate water insoluble material and final
 383 residue.

Amino acids	Amino acids content (mg g ⁻¹)	
	Water insoluble material	Final residue
Ala	22.1±5.4	26.0±5.7
Gly	7.5±3.8	8.4±2.1
Val	24.4±1.3	31.8±7.6
Thr	0.5±0.4	0.6±0.4
Ser	1.3±0.7	1.2±0.6
Leu	23.6±3.9	25.0±2.6
Ile	17.6±1.1	19.1±3.6
Pro	4.5±1.2	0.7±0.3
Asx	2.4±1.1	
Phe	3.9±0.2	2.5±0.6
Glx	3.5±1.4	
Lys	1.5±0.9	
Tyr	0.7±0.1	
Total	113.5±17.0	115.3±18.5

384

385 The polysaccharides present in the final residue are composed mainly by glucose (47%),
 386 galactose (18%), uronic acids (12%), arabinose (8%), xylose (7%), and mannose (6%) (Table 1). The

387 main glycosidic linkage (53.5%) was (1→4)-glucose (Figure 3). In order to check if it is (β1→4)-
388 linked glucose, an enzymatic hydrolysis was performed with a cellulase during 24 h. The release of
389 mainly DP3 to the supernatant, with a less extent of DP4 and DP2 (Figure 2b), allowed to infer that
390 the polysaccharides were constituted by (β1→4)-Glucose residues. In addition, even after 48 h
391 hydrolysis, the oligosaccharide profile was similar, with a high release of DP3 and DP4. As the
392 abundance of DP2 oligosaccharides was very small, it can be inferred that the polysaccharide could
393 be branched, probably indicating the presence of xyloglucan fragments. In fact, the presence of 4-Glc
394 also with 4,6-Glc (5.8%), t-Xyl (3.9%), 2-Xyl (2.7%), t-Gal (2.6%), t-Fuc (0.3%), and 2-Gal (0.3%)
395 are diagnostic linkages of xyloglucan-type polysaccharides. The proportions of the side chains
396 residues (t-Xyl, 2-Xyl, t-Gal, t-Fuc and 2-Gal) to the branched glucose (4,6-Glc), also with the same
397 proportion of 2-Gal to terminally-linked fucose and 2-Xyl to terminally-linked galactose (Figure 3)
398 support the xyloglucan structure (Quéméner et al., 2015; Ray et al., 2014; Vincken et al., 1996). The
399 presence of xyloglucans were already reported in apple juices produced by enzymatic pomace
400 liquefaction with pectinases and cellulases (Mehrländer et al., 2002). The presence of xyloglucan
401 fragments in the retentate of the apple juice clarification could be explained by the high solubility of
402 this branched polysaccharide in the juice but, due to the high molecular weight, it is retained in the
403 ultrafiltration membranes.

404 Retentate is also rich in 3-Gal (4.0%), 6-Gal (2.4%), 3,6-Gal (4.1%), t-Araf (3.7%), 3-Araf
405 (2.2%) and 5-Araf (0.3%). These linkages are characteristic of type II arabinogalactans, already
406 described in apple juice (Brillouet et al., 1996; Will and Dietrich, 1992). In minor amounts, it is also
407 present in retentate 4-Man and 4,6-Man linkages probably from galactoglucomannan, already
408 reported in apple flesh (Nara et al., 2004; Ray et al., 2014).

409 Figure 3.

410

411 *3.5. Food and feed applications*

412 In order to find industrial applications for the apple juice retentate, apple cider production (10
413 hL) in an industrial scale was performed. The cider was fermented using the premium concentrate
414 product from the apple juice industry, which was diluted to obtain 12° Brix, and mixing it with the
415 retentate in a proportion of 4:1 (v/v), reconstituting the original juice. Due to the presence of protein,
416 the retentate could supplement in amino acids the nutritional medium for the yeasts growth. For the
417 formulation of the nutritive medium, a hydrolysis of proteins was promoted through the proteolytic
418 enzymes present in the barley malt. The nutritive medium attained a free amino acid concentration of
419 1.6 g/L. After dilution in the reconstituted juice (0.6 g/L of amino acids), the concentration of the
420 amino acids was 0.9 g/L in the fermentative broth, allowing a more efficient fermentation (Malherbe
421 et al., 2004). The fermentation attained the stationary phase with 8 days, allowing to obtain a cider
422 product containing 5.2% of ethanol and total soluble solids of 9.4° Brix. A consumer sensorial
423 evaluation revealed a good acceptance of the final product that have already been commercialised
424 under the brand Vadia. From the evaluation of 65 consumers that visit the cider spot in a local
425 market exhibition, 91% manifested purchase intention. The cider was globally evaluated by the
426 consumers from 1 to 10 values, where 32% attributed the score 8 and 73% of consumers attributed a
427 score higher or equal to 7 (7-10).

428 Furthermore, as the retentate is composed by a large amount of monosaccharides, almost half of
429 the dry weight, their recovery into the apple juice can increase the total soluble solids and,
430 consequently, the °Brix of apple juice concentrate. This can easily be performed in an industrial
431 environment by centrifugation in order to refeed the concentrator.

432 The retentate water insoluble material being rich in protein can be exploited as a source of
433 protein for the animal feed industry, that looks for alternative sources of protein as feedstock, namely
434 in feed for pets, racing pigeons, and aquaculture. The feed is adapted to different life periods of the
435 racing pigeons, where the animal keepers spend high financial resources in the physical preparation
436 of the pigeons. The pigeons have meals prepared as a comparable level of a high competition athlete,

437 which require a high protein intake (20%). The extruded feeds for pigeons is a market in expansion
438 in order to improve the nutritional balance of the feed. The extrusion process allows the combination
439 of seeds with other raw materials, namely soybean meal, the elected protein source, a by-product
440 from food industry. In order to evaluate the feasibility of using the residue obtained after
441 centrifugation of the retentate, 15% was incorporated into feed formulations for racing pigeons in
442 period of competition, replacing the use of 20% of soybean meal. It was observed that the
443 formulation with retentate had the same extrusion behaviour as the control sample. However, the
444 colour observed for the formulation with retentate was dark brown, contrasting with the light brown
445 control sample. These results show that it is possible to use the retentate water insoluble material in
446 extrusion processes but formulations should include lower amounts than 15%. The decrease of the
447 incorporation to 5% will allow it to obtain an acceptable colour. The substitution of 20% soybean
448 meal with the retentate showed a different amino acid profile with an increase in molar % of
449 essential amino acids. In addition, because the retentate has a relatively high content of free fatty
450 acids (Table 2), the incorporation of 5% will be within the recommended limit for these compounds
451 without the need of a saponification pre-treatment for their removal.

452

453 **4. Conclusion**

454 The retentate, by-product of apple juice ultrafiltration, is a sludge with 8% of dissolved and
455 suspended solids that can be exploited as a source of free sugars, protein, polysaccharides, amino
456 acids, fatty acids, sterols, triacylglycerides, and procyanidins. Free sugars represent 56% of retentate,
457 mainly fructose and glucose, able to be valorised within the industrial process. Retentate is also
458 constituted of 3% lipophilic compounds, where 20% is β -sitosterol, a valuable nutraceutical
459 ingredient, and is composed by 15% of insoluble material, rich in protein (36%) and polysaccharides
460 (20%). The use of retentate for cider and feed production show the potential for its valuation.

461

462 Acknowledgements

463 The authors acknowledge the funding through the Project ProfitApple 38162, QREN I&DT in co-
464 promotion 2013, FEDER, COMPETE. Thanks are due to FCT/MEC for the financial support to the
465 QOPNA research Unit [FCT UID/QUI/00062/2013], through national funds and where applicable
466 co-financed by the FEDER, within the PT2020 Partnership Agreement. Elisabete Coelho
467 [SFRH/BPD/70589/2010] was supported by FCT/MEC grants. Authors also thank Oswaldo Trabulo
468 from Indumape, S.A., for apple juice concentrate products and by-products supply, Susana Santos
469 from Ovargado, S.A., for the preparation of feed formulations, Nicolas Billard from Vadia
470 microbrewery, Essência D'Alma Lda, for cider production. They also thank Dean Holley from
471 London, UK, for revising the English of the manuscript.

472

473

474

475 **References**

- 476 Alberici, R.M., Fernandes, G.D., Porcari, A.M., Eberlin, M.N., Barrera-Arellano, D., Fernández,
477 F.M., 2016. Rapid fingerprinting of sterols and related compounds in vegetable and animal
478 oils and phytosterol enriched- margarines by transmission mode direct analysis in real time
479 mass spectrometry. *Food Chem.* 211, 661-668.
- 480 Aued-Pimentel, S., Lago, J.H.G., Chaves, M.H., Kumagai, E.E., 2004. Evaluation of a methylation
481 procedure to determine cyclopropenoids fatty acids from *Sterculia striata* St. Hil. Et Nauds
482 seed oil. *J. Chromatogr. A* 1054, 235-239.
- 483 Bada, J.C., León-Camacho, M., Copovi, P., Alonso, L., 2014. Characterization of apple seed oil with
484 Denomination of Origin from Asturias, Spain. *Grasas Aceites* 65, e027.
- 485 Barrantes Leiva, M., Hosseini Koupaie, E., Eskicioglu, C., 2014. Anaerobic co-digestion of
486 wine/fruit-juice production waste with landfill leachate diluted municipal sludge cake under
487 semi-continuous flow operation. *Waste Manage.* 34, 1860-1870.
- 488 Bastos, R., Coelho, E., Coimbra, M.A., 2015. Modifications of *Saccharomyces pastorianus* cell wall
489 polysaccharides with brewing process. *Carbohydr. Polym.* 124, 322-330.
- 490 Belding, R.D., Blankenship, S.M., Young, E., Leidy, R.B., 1998. Composition and variability of
491 epicuticular waxes in apple cultivars. *J. Am. Soc. Hortic. Sci.* 123, 348-356.
- 492 Bhosle, B.M., Subramanian, R., 2005. New approaches in deacidification of edible oils—a review. *J.*
493 *Food Eng.* 69, 481-494.
- 494 Bhushan, S., Kalia, K., Sharma, M., Singh, B., Ahuja, P.S., 2008. Processing of Apple Pomace for
495 Bioactive Molecules. *Crit. Rev. Biotechnol.* 28, 285-296.
- 496 Brillouet, J.-M., Williams, P., Will, F., Müller, G., Pellerina, P., 1996. Structural characterization of
497 an apple juice arabinogalactan-protein which aggregates following enzymic
498 dearabinosylation. *Carbohydr. Polym.* 29, 271-275.
- 499 Bruijn, J., Bórquez, R., 2006. Analysis of the fouling mechanisms during cross-flow ultrafiltration of
500 apple juice. *LWT-Food Sci. Technol.* 39, 861-871.
- 501 Coelho, E., Rocha, M.A.M., Moreira, A.S.P., Domingues, M.R.M., Coimbra, M.A., 2016. Revisiting
502 the structural features of arabinoxylans from brewers' spent grain. *Carbohydr. Polym.* 139,
503 167-176.
- 504 Coimbra, M.A., Nunes, C., Cunha, P.R., Guiné, R., 2011. Amino acid profile and Maillard
505 compounds of sun-dried pears. Relation with the reddish brown colour of the dried fruits.
506 *Eur. Food Res. Technol.* 233, 637-646.
- 507 da Silva, A.C., Jorge, N., 2016. Bioactive compounds of oils extracted from fruits seeds obtained
508 from agroindustrial waste. *Eur. J. Lipid Sci. Technol.* 119, 1600024.
- 509 Dhillon, G.S., Brar, S.K., Verma, M., Tyagi, R.D., 2011. Apple pomace ultrafiltration sludge – A
510 novel substrate for fungal bioproduction of citric acid: Optimisation studies. *Food Chem.*
511 128, 864-871.
- 512 Dhillon, G.S., Kaur, S., Brar, S.K., 2013. Perspective of apple processing wastes as low-cost
513 substrates for bioproduction of high value products: A review. *Renew. Sust. Energ. Rev.* 27,
514 789-805.
- 515 European Fruit Juice Association, 2014. 2014 Market Report, AIJN – Association of the Industry of
516 Juices and nectars from Fruits and Vegetables of the European Union. AIJN – Association
517 of the Industry of Juices and nectars from Fruits and Vegetables of the European Union,
518 Brussels.
- 519 FAOSTAT, 2017. FAO Statistical Database, <http://www.fao.org/faostat/en/#data/QC>.
- 520 Ferreira, D., Guyot, S., Marnet, N., Delgadillo, I., Renard, C.M.G.C., Coimbra, M.A., 2002.
521 Composition of phenolic compounds in a portuguese pear (*Pyrus communis* L. Var. S.
522 Bartolomeu) and changes after sun-drying. *J. Agric. Food Chem.* 50, 4537-4544.

- 523 García-Salas, P., Verardo, V., Gori, A., Caboni, M.F., Segura-Carretero, A., Fernández-Gutiérrez,
524 A., 2016. Determination of lipid composition of the two principal cherimoya cultivars
525 grown in Andalusian Region. *LWT - Food Sci. Technol.* 65, 390-397.
- 526 Guyot, S., Marnet, N., Sanoner, P., Drilleau, J.F., 2003. Variability of the polyphenolic composition
527 of cider apple (*Malus domestica*) fruits and juices. *J. Agric. Food Chem.* 51, 6240-6247.
- 528 Gylling, H., Nissinen, M.J., 2015. Phytosterol therapy, in: Garg, A. (Ed.) *Dyslipidemias:
529 Pathophysiology, Evaluation and Management*. Humana Press Inc., Totowa, NJ, pp. 343-
530 354.
- 531 Hatano, T., Hemingway, R.W., 1996. Association of (+)-catechin and catechin-(4 α \rightarrow 8)-catechin
532 with oligopeptides. *Chem. Commun.*, 2537-2538.
- 533 Huebner, M., Kienzle, M., 2001. Retentate-waste or a valuable product? New solutions. *Food
534 Process.* 12, 358-363.
- 535 Lu, Y., Yeap Foo, L., 1998. Constitution of some chemical components of apple seed. *Food Chem.*
536 61, 29-33.
- 537 Malherbe, S., Fromion, V., Hilgert, N., Sablayrolles, J.M., 2004. Modeling the effects of assimilable
538 nitrogen and temperature on fermentation kinetics in enological conditions. *Biotechnol.
539 Bioeng.* 86, 261-272.
- 540 McGhie, T.K., Hudault, S., Lunken, R.C.M., Christeller, J.T., 2012. Apple peels, from seven
541 cultivars, have lipase-inhibitory activity and contain numerous ursenoic acids as identified
542 by LC-ESI-QTOF-HRMS. *J. Agric. Food Chem.* 60, 482-491.
- 543 Mehrländer, K., Dietrich, H., Sembries, S., Dongowski, G., Will, F., 2002. Structural
544 characterization of oligosaccharides and polysaccharides from apple juices produced by
545 enzymatic pomace liquefaction. *Am. Chem. Soc.* 50, 1230-1236.
- 546 Mirabella, N., Castellani, V., Sala, S., 2014. Current options for the valorization of food
547 manufacturing waste: a review. *J. Clean. Prod.* 65, 28-41.
- 548 Nara, K., Ito, S., Kato, K., Kato, Y., 2004. Isolation of Galactoglucomannan from Apple
549 Hemicellulosic Polysaccharides with Binding Capacity to Cellulose. *J. Appl. Glycosci.* 51,
550 321-325.
- 551 O'Shea, N., Arendt, E.K., Gallagher, E., 2012. Dietary fibre and phytochemical characteristics of
552 fruit and vegetable by-products and their recent applications as novel ingredients in food
553 products. *Innov. Food Sci. Emerg. Technol.* 16, 1-10.
- 554 Passos, C.P., Cardoso, S.M., Barros, A.S., Silva, C.M., Coimbra, M.A., 2010. Application of Fourier
555 transform infrared spectroscopy and orthogonal projections to latent structures/partial least
556 squares regression for estimation of procyanidins average degree of polymerisation. *Anal.
557 Chim. Acta* 661, 143-149.
- 558 Protzman, E., 2016. *Fresh Deciduous Fruit: World Markets and Trade (Apples, Grapes, & Pears)*,
559 United States Department of Agriculture. Foreign Agricultural Service, Office of Global
560 Analysis, Washington, DC.
- 561 Quémener, B., Vigouroux, J., Rathahao, E., Tabet, J.C., Dimitrijevic, A., Lahaye, M., 2015. Negative
562 electrospray ionization mass spectrometry: a method for sequencing and determining
563 linkage position in oligosaccharides from branched hemicelluloses. *J. Mass Spectrom.* 50,
564 247-264.
- 565 Ray, S., Vigouroux, J., Quémener, B., Bonnin, E., Lahaye, M., 2014. Novel and diverse fine
566 structures in LiCl-DMSO extracted apple hemicelluloses. *Carbohydr. Polym.* 108, 46-57.
- 567 Re, R., Pellegrini, N., Proteggente, A., Pannala, A., Yang, M., Rice-Evans, C., 1999. Antioxidant
568 activity applying an improved ABTS radical cation decolorization assay. *Free Radic. Biol.
569 Med.* 26, 1231-1237.
- 570 Renard, C., Baron, A., Guyot, S., Drilleau, J.F., 2001. Interactions between apple cell walls and
571 native apple polyphenols: quantification and some consequences. *Int. J. Biol. Macromol.* 29,
572 115-125.

- 573 Rudell, D.R., Buchanan, D.A., Leisso, R.S., Whitaker, B.D., Mattheis, J.P., Zhu, Y., Varanasi, V.,
574 2011. Ripening, storage temperature, ethylene action, and oxidative stress alter apple peel
575 phytosterol metabolism. *Phytochemistry* 72, 1328-1340.
- 576 Seguí Gil, L., Fito Maupoey, P., 2018. An integrated approach for pineapple waste valorisation.
577 Bioethanol production and bromelain extraction from pineapple residues. *J. Clean. Prod.*
578 172, 1224-1231.
- 579 Siebert, K.J., 1999. Effects of Protein–Polyphenol Interactions on Beverage Haze, Stabilization, and
580 Analysis. *J. Agric. Food Chem.* 47, 353-362.
- 581 Siger, A., Michalak, M., Rudzińska, M., 2016. Canolol, tocopherols, plastochromanol-8, and
582 phytosterols content in residual oil extracted from rapeseed expeller cake obtained from
583 roasted seed. *Eur. J. Lipid Sci. Technol.* 118, 1358-1367.
- 584 Singleton, V.L., Rossi, J.A., 1965. Colorimetry of total phenolics with phosphomolybdic-
585 Phosphotungstic acid reagents. *Am. J. Enol. Vitic.* 16, 144-158.
- 586 Sosulski, F.W., Imafidon, G.I., 1990. Amino acid composition and nitrogen-to-protein conversion
587 factors for animal and plant foods. *J. Agric. Food Chem.* 38, 1351-1356.
- 588 Spanos, G.A., Wrolstad, R.E., 1992. Phenolics of apple, pear, and white grape juices and their
589 changes with processing and storage. A review. *J. Agric. Food Chem.* 40, 1478-1487.
- 590 Thavarajah, P., Low, N.H., 2006. Adulteration of Apple with Pear Juice: Emphasis on Major
591 Carbohydrates, Proline, and Arbutin. *J. Agric. Food Chem.* 54, 4861-4867.
- 592 United States Department of Agriculture, 2016. Citrus: World Markets and Trade, United States
593 Department of Agriculture. Foreign Agricultural Service, Office of Global Analysis,
594 Washington, DC.
- 595 Verardo, G., Pagani, E., Geatti, P., Martinuzzi, P., 2003. A thorough study of the surface wax of
596 apple fruits. *Anal. Bioanal. Chem.* 376, 659-667.
- 597 Vilela, C., Santos, S.A.O., Villaverde, J.J., Oliveira, L., Nunes, A., Cordeiro, N., Freire, C.S.R.,
598 Silvestre, A.J.D., 2014. Lipophilic phytochemicals from banana fruits of several *Musa*
599 species. *Food Chem.* 162, 247-252.
- 600 Villaño, D., Fernández-Pachón, M.S., Moyá, M.L., Troncoso, A.M., García-Parrilla, M.C., 2007.
601 Radical scavenging ability of polyphenolic compounds towards DPPH free radical. *Talanta*
602 71, 230-235.
- 603 Vincken, J.P., Beldman, G., Messen, W.M.A., Voragen, A.G.J., 1996. Degradation of apple fruit
604 xyloglucan by endoglucanase. *Carbohydrate Polym.* 29, 75-85.
- 605 Virmond, E., De Sena, R.F., Albrecht, W., Althoff, C.A., Moreira, R.F.P.M., José, H.J., 2012.
606 Characterisation of agroindustrial solid residues as biofuels and potential application in
607 thermochemical processes. *Waste Manage.* 32, 1952-1961.
- 608 Whitaker, B.D., 2012. Membrane lipid metabolism and oxidative stress involved in postharvest
609 ripening, senescence, and storage disorders of fruits. *Acta Hort.* 945, 269-282.
- 610 Whitaker, B.D., Klein, J.D., Conway, W.S., Sams, C.E., 1997. Influence of prestorage heat and
611 calcium treatments on lipid metabolism in 'Golden Delicious' apples. *Phytochemistry* 45,
612 465-472.
- 613 Will, F., Dietrich, H., 1992. Isolation, purification and characterization of neutral polysaccharides
614 from extracted apple juices. *Carbohydr. Polymers* 18, 109-117.
- 615 Wu, L.-C., Siebert, K.J., 2002. Characterization of Haze-Active Proteins in Apple Juice. *Am. Chem.*
616 *Soc.* 50, 3828-3834.
- 617 Yates, M., Gomez, M.R., Martin-Luengo, M.A., Ibañez, V.Z., Martinez Serrano, A.M., 2017.
618 MultivalORIZATION of apple pomace towards materials and chemicals. *Waste to wealth. J.*
619 *Clean. Prod.* 143, 847-853.
- 620

622 **Figure captions**

623

624 **Figure 1.** Schematic representation of sequential extraction of the retentate. (Yields expressed in dry
625 weight basis, the values between brackets correspond to yields calculated in water insoluble material
626 weight basis).

627

628 **Figure 2.** Size-exclusion chromatographic profile on Bio-Gel P2 of (a) retentate supernatant material
629 and (b) oligosaccharides obtained after 24 and 48 h cellulase hydrolysis of the insoluble material
630 after the sequential extraction with *n*-hexane, ethanol, and acetone:water (final residue). V_0 - void
631 volume, DP_4 and DP_2 correspond to the elution volume of stachyose and sucrose, respectively and V_i
632 -total volume. Letters A–D refer to fractions of the retentate supernatant material.

633

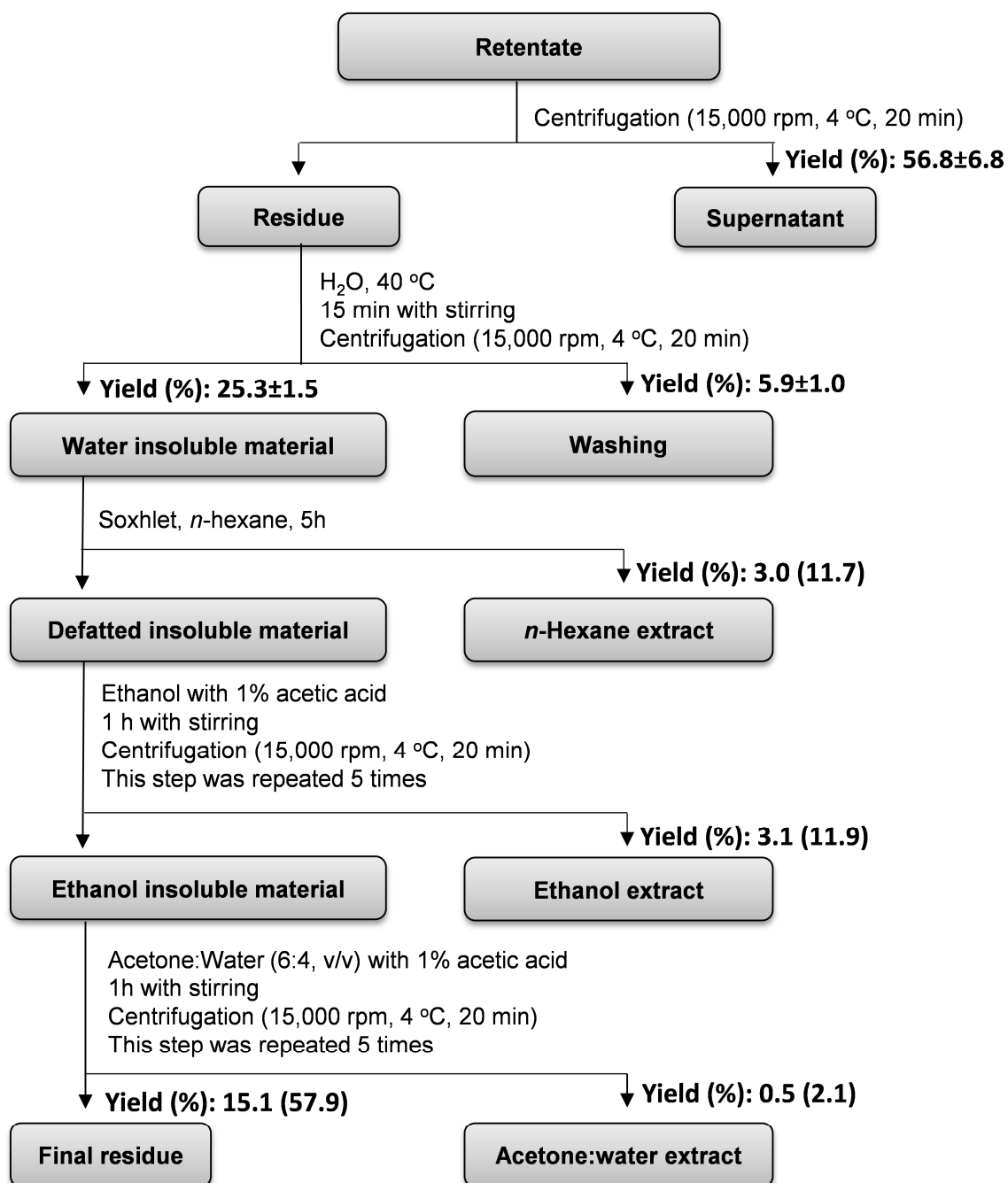
634 **Figure 3.** Glycosidic-linkage composition (mol%) of final residue.

635

636

637 **Figures**

638

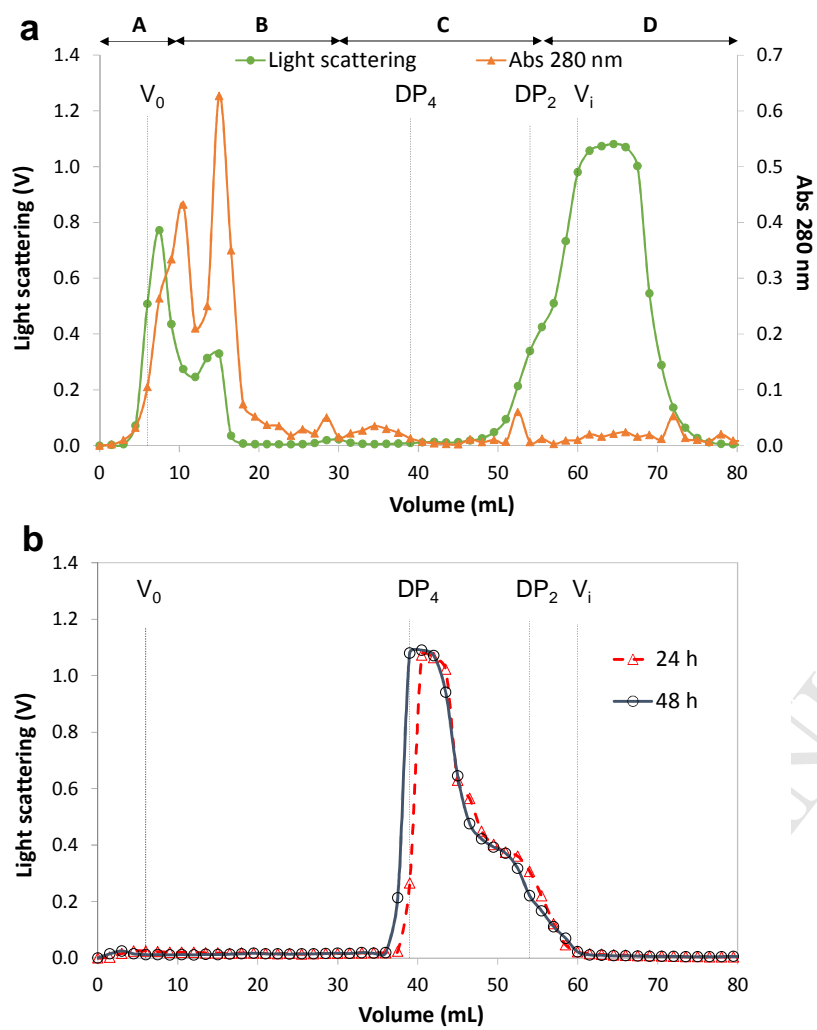


639

640

Figure 1

641

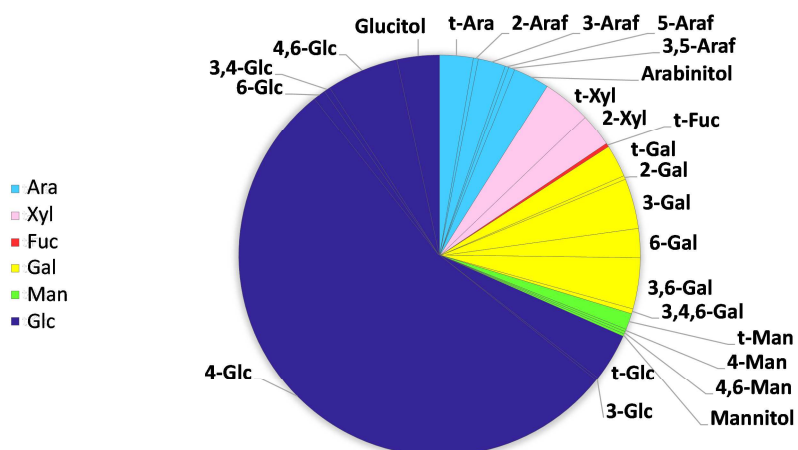


642

643

Figure 2

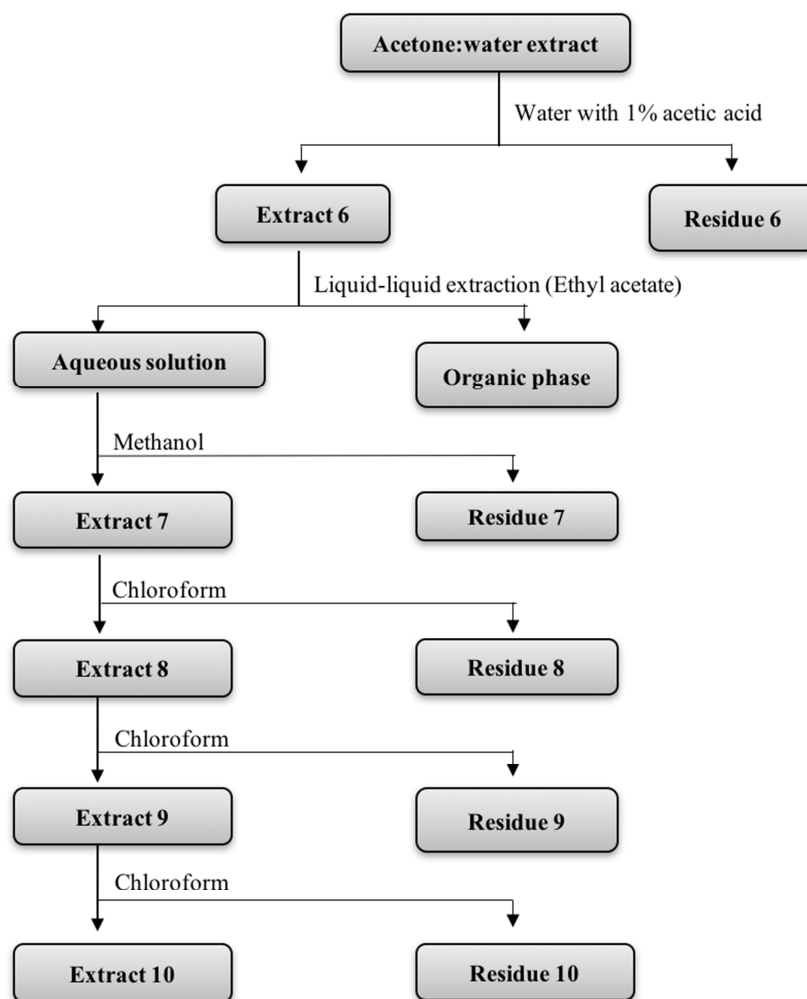
644



645

Figure 3

646

647 **Supplementary material**

648

649 **Figure S1.** Extraction and fractionation of procyanidin present in acetone:water extract.

650

651

652 **Table S1.** Procyanidin composition of the fractions obtained by fractionation of acetone:water extract.

	DP_n	Yield (% w/w)	CHCl₃ (%)
Residue 6	-	45.3	-
Organic phase	-	1.9	-
Residue 7	-	17.7	-
Residue 8	8	6.7	40
Residue 9	7	3.8	60
Residue 10	5	7.4	80
Extract 10	<5	2.3	-

653

654

655

Highlights

- Retentate is a source of free sugars, protein, polysaccharides, and sterols.
- Very rich in carbohydrates (53%), where 40% is fructose and 8% glucose, DW.
- An available and inexpensive source of β -sitosterol (6 g kg^{-1} of retentate, DW).
- Retentate was used as a nutritive source for production of artisanal cider.
- Water insoluble material (28% of protein) was used in feed formulations.