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Optimization of phycobiliprotein pigments extraction from red algae *Gracilaria gracilis* for substitution of synthetic food colorants

Tatiana Pereira, Sónia Barroso, Susana Mendes, Renata A. Amaral, Juliana R. Dias, Teresa Baptista, Jorge A. Saraiva, Nuno M. Alves, Maria M. Gil

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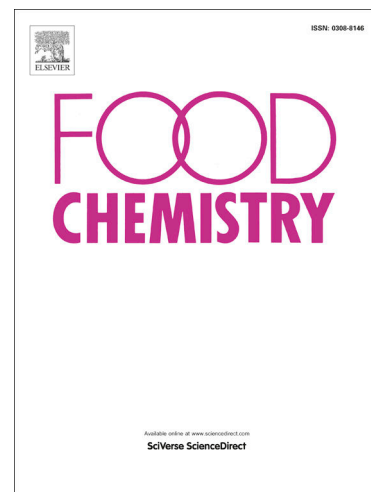
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1 **Optimization of phycobiliprotein pigments extraction from red algae *Gracilaria gracilis***  
2 **for substitution of synthetic food colorants**

3 Tatiana Pereira <sup>a</sup>, Sónia Barroso <sup>a\*</sup>, Susana Mendes <sup>a</sup>, Renata A. Amaral <sup>c</sup>, Juliana R. Dias <sup>b</sup>,  
4 Teresa Baptista <sup>a</sup>, Jorge A. Saraiva <sup>c</sup>, Nuno M. Alves <sup>b</sup>, Maria M. Gil <sup>a</sup>

5  
6 <sup>a</sup> MARE – Marine and Environmental Sciences Centre, Polytechnic of Leiria, Cetemares, 2520-620  
7 Peniche, Portugal

8 <sup>b</sup> CDRSP – Centre for Rapid and Sustainable Product Development, Polytechnic of Leiria, 2430-028  
9 Marinha Grande, Portugal

10 <sup>c</sup> QOPNA & LAQV-REQUIMTE, Department of Chemistry, University of Aveiro, 3810-193 Aveiro,  
11 Portugal

12  
13  
14 **Abstract**

15 The extraction of phycobiliprotein (PBP) pigments from red algae *Gracilaria gracilis* was  
16 optimized using maceration, ultrasound-assisted extraction (ultrasonic water bath and ultrasonic  
17 probe), high pressure-assisted extraction, and freeze-thaw. The experimental conditions, namely  
18 homogenization time (t1), buffer concentration (C), treatment time (t2), biomass: buffer ratio  
19 (R), and pressure (P), were optimized using Response Surface Methodology (RSM). The yield  
20 of phycoerythrin (PE) extracted, determined spectroscopically, was used as the response  
21 variable. Maceration was the most efficient extraction method yielding 3.6 mg PE /g biomass  
22 under the optimal conditions (t1 = t2 = 10 min; C = 0.1 M; R = 1:50). Scanning Electron  
23 Microscopy (SEM) analysis of the biomass before and after the cell disruption treatments  
24 revealed a more efficient cell wall rupture with maceration.

25

26 **Keywords:** natural pigments; Phycobiliproteins; *Gracilaria gracilis*; Response Surface  
27 Methodology; extraction optimization.

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## 31 **1 Introduction**

32 Phycobiliproteins (PBPs) are non-toxic water-soluble proteins mostly found in Rhodophyta (red  
33 algae), Cyanobacteria, and Cryptophyta. Due to their strong absorbance and fluoresce properties  
34 as well as antioxidant and free-radical scavenging activities, PBPs have been widely employed  
35 in food, cosmetics, pharmaceutical, and biomedical industries (Sonani, Rastogi, Patel, &  
36 Madamwar, 2016). Since purified PBPs are expensive, the search for more effective extraction  
37 and purification methods is desirable. PBPs are present in the thylakoid membrane in the stroma  
38 inside the seaweed's chloroplast so their efficient extraction typically requires the use of  
39 appropriate solvents and cell disruption methods (Beattie, Morançais, Déléris, Fleurence, &  
40 Dumay, 2018). Red algae of the *Gracilaria* genus are a rich source of PBPs, namely  
41 phycoerythrin (PE), being valuable resources for industrial and biotechnological applications  
42 (Francavilla, Franchi, Monteleone, & Caroppo, 2013).

43 The most widely used solvents in PBPs extraction are phosphate buffer, distilled water, and  
44 seawater (Sudhakar, Jagatheesan, Perumal, & Arunkumar, 2015). Several methods have been  
45 studied for protein extraction such as homogenization (Dumay, Morançais, Nguyen, &  
46 Fleurence, 2015), maceration in presence of liquid nitrogen (Munier et al., 2014), maceration  
47 with mortar and pestle (Sudhakar et al., 2015), freeze grinding (Fleurence, 2003; Galland-  
48 Irmouli et al., 2000), freezing and thawing (Senthilkumar, Kurinjimalar, et al., 2013), and  
49 ultrasonication (Le Guillard et al., 2015).

50 Among conventional extraction methods, maceration is one of the most used, due to its low  
51 economic impact, short extraction time, and easy setup (Beattie et al., 2018). Freeze-thaw is  
52 another conventional method widely used for cellular disruption with advantages such as high  
53 reproducibility and robustness, achieving higher purity extracts (Kannaujiya, Sundaram, &  
54 Sinha, 2017). As a non-conventional extraction methodology considered a 'green technology',  
55 ultrasound-assisted extraction presents a significant reduction in extraction time, solvent  
56 consumption, with higher extraction yields at lower temperatures, being suitable for  
57 thermolabile compounds (Juin et al., 2015; Mittal, Tavanandi, Mantri, & Raghavarao, 2017).  
58 Another modern, non-conventional alternative is high pressure-assisted extraction. It can be a  
59 fast and highly efficient extraction method, easily operated and highly mechanized, requiring

60 low amounts of solvent. Moreover, it can be operated at room temperature, protecting the  
61 bioactivity of compounds with low thermal stability, which is useful in the extraction of heat-  
62 sensible chromoproteins (Alexandre et al., 2017; Huang, Hsu, Yang, & Wang, 2013; Santos,  
63 Salvador, Domingues, Cruz, & Saraiva, 2013).

64 The extraction yield is highly influenced by numerous factors, such as the biomass: solvent  
65 ratio, the cellular disruption method, the solvent used, and the extraction time (Beattie et al.,  
66 2018). The optimization of the influence of such experimental conditions may be exhaustive  
67 and laborious (Bezerra, Santelli, Oliveira, Villar, & Escaleira, 2008). Response Surface  
68 Methodology (RSM) is a statistical tool that can be used to determine and optimize the optimal  
69 experimental conditions to achieve maximum yields with minimum time and resources  
70 consumption (Asfaram, Ghaedi, Abidi, et al., 2018; Asfaram, Ghaedi, Javadian, & Goudarzi,  
71 2018; Khuri A. I., 2017; Taofiq et al., 2019). In the present study, *Gracilaria gracilis*, a red alga  
72 from the Portuguese coast, was used as a natural source for the extraction of PBP pigments for  
73 application as food colorant. Several extraction techniques were used, namely maceration,  
74 ultrasounds, freeze-thaw, and high pressure, and the experimental conditions optimized using  
75 RSM.

76

## 77 **2 Materials and Methods**

### 78 **2.1 Biomass**

79 Red macroalgae *Gracilaria gracilis* was collected in October 2018 from the intertidal zone of  
80 Buarcos, Figueira da Foz (40.1773° N, 8.8749° W), Portugal. The algae were washed with salt  
81 water (35% (w/v)), frozen at -80 °C and freeze-dried. The freeze-dried biomass was ground  
82 using a mixer and stored in a dry recipient in the absence of light until further studies.

### 83 **2.2 Chemicals**

84 Sodium phosphate buffer pH 6.8 ( $\text{Na}_2\text{HPO}_4/\text{NaH}_2\text{PO}_4$ ) was prepared using disodium hydrogen  
85 phosphate dodecahydrate ( $\text{Na}_2\text{HPO}_4 \cdot 12\text{H}_2\text{O}$ ) and sodium phosphate monobasic anhydrous  
86 ( $\text{NaH}_2\text{PO}_4$ ) purchased from Scharlau and AMRESCO, respectively.

## 87 **2.3 Extraction procedure**

88 Different extraction methods and conditions were tested. The extraction methods used were both  
89 conventional, such as maceration and freeze-thaw, and non-conventional, like ultrasound-  
90 assisted extraction (ultrasonic water bath and ultrasonic probe) and high pressure-assisted  
91 extraction. The extraction conditions optimized were homogenization time ( $t_1$  =  
92 homogenization of biomass in phosphate buffer), buffer concentration (C), treatment time ( $t_2$  =  
93 time of application of the extraction method), biomass: buffer ratio (R) and pressure (P) (for  
94 high pressure-assisted extraction).

95 Extractions were performed using procedures adapted from Beattie et al. (2018), Mittal et al.  
96 (2017) and Alexandre et al. (2017). For all the runs, freeze-dried *G. gracilis* (100 mg) was  
97 suspended in different phosphate buffer concentration ( $0.01 \text{ M} < C < 1 \text{ M}$ , pH 6.8), at different  
98 biomass: buffer ratios (R) ( $V_{\text{buffer}} = 0.5\text{-}5 \text{ mL}$ ,  $1:5 < R < 1:50$ ) and homogenized, with the help  
99 of a magnetic stirrer, at room temperature for different lengths of time ( $5 \text{ min} < t_1 < 30 \text{ min}$ ).  
100 Then, an extraction treatment was applied for different periods of time (defined below for each  
101 method) to the suspension to promote/increase cell disruption and pigment release. Extractions  
102 were carried out using sodium phosphate buffer at pH 6.8 as several studies have shown that it  
103 is efficient for phycoerythrin extraction (Sharmila Banu, Santhosh, Hemalatha,  
104 Venkatakrishnan, & Dhandapani, 2017; Sudhakar et al., 2015). The diverse combinations of  
105 conditions were defined using the Response Surface Methodology (RSM) as described below.  
106 After extraction, the samples were centrifuged (Eppendorf Centrifuge 5810R, Billerica, EUA)  
107 at 10.000 rpm for 20 min at 4 °C and the pellet discarded. The supernatant was further filtered  
108 through a PTFE 0.45  $\mu\text{m}$  membrane (VWR, North America) and analyzed in a UV-Vis  
109 equipment (Thermo Scientific Evolution 201, Thermo Fisher Scientific Inc.).

### 110 **2.3.1 Maceration**

111 The biomass/buffer suspension was ground with a mortar and pestle for different periods of time  
112 ( $10 \text{ s} < t_2 < 10 \text{ min}$ ).

### 113 **2.3.2 Ultrasound-assisted extraction**

114 The biomass/buffer suspension was placed either in an ultrasonic bath (Ultrasonic Cleaner,  
115 VWR USC 600 TH, Radnor, USA; 45 kHz, 400 W) or subjected to sonication with an ultrasonic

116 probe (S2500 Branson Digital Sonicator, Danbury, CT, USA; 50/60 kHz, 200 W) for different  
 117 periods of time ( $10 \text{ s} < t_2 < 10 \text{ min}$ ). In the last case, the probe was inserted in the sample  
 118 container at about 0.5 cm from the bottom. The sample was cooled in an ice bath to avoid  
 119 overheating and an ultrasonic pulse ‘on and off’ cycle of 30/20 seconds was used.

### 120 **2.3.3 Freeze-thaw**

121 Samples of the biomass/buffer suspension ( $C = 0.1 \text{ M}$ ,  $R = 1:50$ , and  $t_1 = 10 \text{ min}$ ) were frozen  
 122 for 18h at  $-20$  or  $-80 \text{ }^\circ\text{C}$  and thawed for 24h at  $4 \text{ }^\circ\text{C}$  or at room temperature (approximately 19  
 123  $^\circ\text{C}$ ).

### 124 **2.3.4 High Pressure-assisted extraction**

125 The biomass/buffer suspension ( $C = 0.1 \text{ M}$ ) was poured into PA/PE vacuum sealing bags and  
 126 the extraction was carried out on a pilot-scale high-pressure equipment (Model 55, Hyperbaric,  
 127 Burgos, Spain) for different periods of time ( $5 \text{ min} < t_2 < 30 \text{ min}$ ) at different pressures ( $0.1$   
 128  $\text{MPa} < P < 600 \text{ MPa}$ ). In this case, the homogenization time was the time necessary to prepare  
 129 the suspension in the PA/PE bags ( $t_1 = 2\text{-}5 \text{ min}$ ), prior to high-pressure treatment.

## 130 **2.4 Phycobiliprotein quantification**

131 The absorption spectra of the extracts were measured between 200 and 900 nm in a UV-Vis  
 132 spectrophotometer (Thermo Scientific Evolution 201, Thermo Fisher Scientific Inc.).

133 The quantification of R-phycoerythrin (PE) and R-phyococyanin (PC) extracted was performed  
 134 using the Beer & Eshel equations (1985):

$$135 \quad \text{PE} = [(A_{564} - A_{592}) - (A_{455} - A_{592}) * 0.2] * 0.12 \quad (\text{Eq. 1})$$

$$136 \quad \text{PC} = [(A_{618} - A_{645}) - (A_{592} - A_{645}) * 0.5] * 0.15 \quad (\text{Eq. 2})$$

137 where  $A_{564}$  is the maximum absorbance of PE,  $A_{618}$  is the maximum absorbance of PC, and  
 138  $A_{592}$ ,  $A_{455}$  and  $A_{645}$  are absorbance minimums for baseline correction. 0.12 and 0.15 are the  
 139 absorption coefficients for PE and PC, respectively, and 0.2 and 0.5 are correction constants  
 140 (Beer & Eshel, 1985).

141 PE and PC yields are expressed in mg PE/g biomass and mg PC/g biomass, respectively.

142 The purity of the extracts was determined using the purity index (Mensi & Romdhane, 2014):

$$143 \quad \text{PI} = A_{564}/A_{280} \quad (\text{Eq. 3})$$

144 where  $A_{564}$  is the maximum absorbance of PE and  $A_{280}$  is the absorbance of total proteins.

## 145 **2.5 Experimental design and Response Surface Methodology (RSM)**

146 Response Surface Methodology (RSM) considering a central composite rotatable design  
147 (CCDR) was employed for the evaluation of variables effect on the PE yield extracted with  
148 maceration and ultrasonic waves. The independent variables tested were homogenization time  
149 ( $t_1$ , 5-30 min), treatment time ( $t_2$ , 10 s-10 min), biomass/buffer ratio (R, 1:5-1:50) and buffer  
150 concentration (C, 0.01-1 M), as defined in section 2.3. The independent variables and their levels  
151 are presented in Table S1 (Supplementary material). For the high pressure-assisted extraction,  
152 a Box-Behnken design was employed, using the treatment time ( $t_2$ , 5-30 min), biomass/buffer  
153 ratio (R, 1:5-1:50), and pressure (P, 0.1-600 MPa) as independent variables in order to evaluate  
154 the relationship between the measured responses and the individual and combined effects of the  
155 conditions. The independent variables and their levels are presented in Table S2 (Supplementary  
156 material). The ranges of the independent variables were defined considering similar work  
157 described in the literature (Marinho-Soriano, 2012; Sudhakar et al., 2015) and experimental  
158 limitations (time of manual maceration, minimum amount of biomass possible to suspend in  
159 buffer, time of uninterrupted equipment operation).

160 A statistical model for the condition's optimization was determined by RSM. For maceration  
161 and ultrasounds-assisted extractions 24 experimental runs with different combinations of four  
162 factors and two central point repetitions were carried out. For high pressure-assisted extraction  
163 14 experimental runs with different combinations of three factors were performed along with  
164 the repetition of central point six times.

## 165 **2.6 Biomass analysis by Scanning Electron Microscopy**

166 The *G. gracilis* biomass, before and after the extraction process, were analyzed by scanning  
167 electron microscopy (SEM; Vega3 Tescan, Brno, Czechia, microscope operated at 15 kV.) to  
168 evaluate the effect of the extraction conditions on the solid matrix and correlate it with the

169 extract retention. After extraction, the biomass samples were subjected to sequential dehydration  
170 with ethanol (70, 85, and 100%) followed by incubation in a drying oven (Memmert,  
171 Schwabach, Germany) at 35 °C. Prior to the examination, samples were coated with a  
172 gold/palladium (Au/Pd) thin film, by sputtering, using the sputter coater equipment (Quorum  
173 Technologies). The cellular structure was compared to a pre-treatment lyophilized sample  
174 (control) at a magnification of 600×.

## 175 **2.7 Statistical analysis**

176 The experimental data were analyzed by regression analysis. Analysis of variance (ANOVA)  
177 generated the regression coefficients of linear, quadratic, and the interaction involved in the  
178 model, with a significance level of 95% ( $p \leq 0.05$ ). The adequacy of the models was determined  
179 using the lack-of-fit test and  $R^2$  (coefficient of determination) analysis.

180 Statistical analysis was performed using the software Statistica 10 (StatSoft, Inc., Minneapolis,  
181 USA). Where applicable the results are presented as mean  $\pm$  standard deviation (SD).

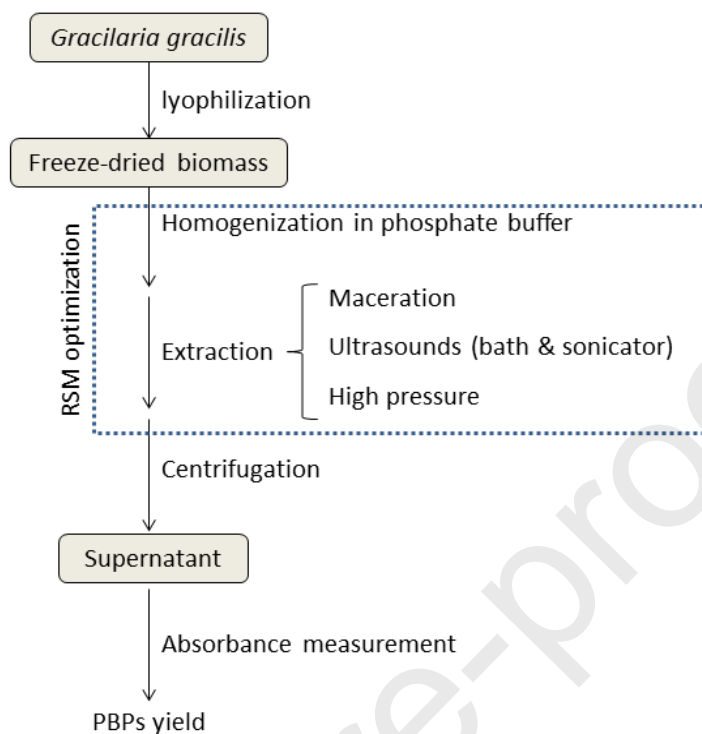
182

## 183 **3 Results and Discussion**

### 184 **3.1. Extraction Results**

185 The procedure followed for the extraction of PBPs from *G. gracilis* is schematized in Figure 1  
186 and a picture of the pinkish supernatant and respective absorption spectrum obtained after  
187 extraction with maceration can be found in Figure S1 (Supplementary material).





188

189 **Figure 1.** Summarizing scheme of the procedure for the extraction of PBPs from *Gracilaria gracilis*.

190

191 Extraction conditions were optimized through RSM applied to several extraction methods as  
 192 described above. The experimental results obtained using the conditions defined by RSM are  
 193 presented in Tables 1 and 2.

194 All the methods successfully extracted PE from freeze-dried *G. gracilis*. The higher PE yields  
 195 were obtained using maceration, with yields ranging from 1.65 to 3.77 mg PE/g biomass (Table  
 196 1). These values are in accordance with the data reported by Francavilla et al. (2013). The  
 197 authors showed the existence of seasonal variations in PBPs concentration with higher contents  
 198 of allophycocyanins (APC, 3.5 mg/g), phycoerythrins (R-PE, 7 mg/g), and phycocyanins (R-  
 199 PC, 3 mg/g) being obtained from samples collected in January when compared with samples  
 200 from October (APC, 1.5 mg/g; PE, 3.6 mg/g; R-PC, 0.7 mg/g). The seasonal differences in  
 201 solar radiation and nutrient concentration in the lagoon could justify the differences in PE  
 202 concentrations. PBPs absorb sunlight in the wavelength range of 470-660 nm, being more active

203 at low light intensities when chlorophyll-*a* becomes inefficient in light absorption, thus allowing  
204 the survival of the species (Beattie et al., 2018). This leads to months with higher sunlight  
205 intensity resulting in lower PBPs contents. Regarding other *Gracilaria* species, previous studies  
206 with mortar maceration of *Gracilaria crassa* yielded 0.50 mg/g of R-PE, 0.28 mg/g of R-PC  
207 and 0.34 mg/g of APC (Sudhakar et al., 2015), while using a table mixer extracted 0.78 mg/g of  
208 R-PE, 0.49 mg/g of R-PC and 0.52 mg/g of APC from *Gracilaria corticata* (Sudhakar,  
209 Saraswathi, & Nair, 2014) and 0.067 mg/g of R-PE and 0.38 mg/g of R-PC from *Gracilaria*  
210 *verrucosa* (Jayasinghe, Pahalawattaarachchi, & Ranaweera, 2016).

211 Compared to conventional maceration process, lower PE yields (1.48-1.99 mg/g, about 55%  
212 less than maceration) were obtained using ultrasound-assisted extraction. The ultrasonic bath,  
213 although having the advantages of being cheap, readily available and allowing the treatment of  
214 many samples simultaneously, also has drawbacks such as low reproducibility and low power  
215 delivery directly to the samples (Chemat et al., 2017). This could have accounted for the low  
216 extraction yield achieved using this extraction method. Previous studies reported the successful  
217 extraction of PBPs using ultrasonic waves from other types of algae, such as *Porphyridium*  
218 *cruentum* and *Heterosiphonia japonica* (Benavides & Rito-Palomares, 2006; Bermejo Román,  
219 Álvarez-Pez, Fernández, & Grima, 2002; Sun et al., 2009). Theoretically, higher concentrations  
220 could be achieved by extending the time in which the samples are subjected to the ultrasonic  
221 bath. (Beattie et al., 2018; Kannaujiya et al., 2017). However, when larger periods of treatment  
222 were used (10-20 min), a degradation of PBPs was observed (decrease in absorbance  
223 maximums), which is in agreement with other studies (Rodrigues, de Castro, Santiago-Aguiar,  
224 & Rocha, 2018).

225 In literature, it is suggested that the ultrasonic probe has advantages over the ultrasonic bath  
226 such as the ultrasonic intensity and the direct delivery of the ultrasounds to the samples with  
227 minimal ultrasonic energy loss (Chemat et al., 2017). Theoretically, the use of an ultrasonic  
228 probe should result in higher extraction yields when compared with an ultrasonic bath, but this  
229 was not verified. However, even lower PE Yields (1.27-1.79 mg/g) were obtained using the  
230 ultrasound probe. Also, the use of an ultrasonic probe led to the simultaneous extraction of  
231 chlorophylls along with PBPs. In nature, the PBPs complement other pigments such as  
232 chlorophylls allowing the transfer of light energy during photosynthesis (Fleurence, 2003).

233 However, in PBPs extraction assays, the simultaneous (and unintentional) extraction of  
234 chlorophylls is considered a contaminant (Laureci, Bresciani, Lami, & Morabito, 2017), which  
235 results in the change of the color of the extracts to a more greenish coloration (as opposed by  
236 the characteristic pinkish color of PEs).

237 For high pressure-assisted extraction, the C (buffer concentration) and t<sub>1</sub> (homogenization time)  
238 variables were fixed at 0.1 M and 2-5 min (the necessary time to prepare the suspension prior  
239 to high-pressure treatment), respectively. The results, presented in Table, show that high  
240 pressure-assisted extraction was the least effective extraction method compared with the other  
241 extraction processes, giving PE yields of 0.25-1.27 mg/g (about 65% less than maceration).  
242 Although high pressure-assisted extraction is widely applied in bacteria and yeast, few studies  
243 have applied this process in algae (even less for the extraction of PBPs). Jubeau et al. (2012)  
244 extracted 3.6 mg of B-PE/g of dry weight biomass applying a two-step high-pressure process in  
245 *Porphyridium cruentum*.

246 Upon extraction optimization with RSM (section 3.2) a model to predict the optimum extraction  
247 conditions was obtained. The predicted optimum extraction conditions were then tested  
248 experimentally in triplicate (Table 1). Optimum predicted extraction conditions for maceration  
249 (t<sub>1</sub> = t<sub>2</sub> = 10 min, C = 0.1 M, and R = 1:50) yielded 3.58 ± 0.03 mg/g of PE. The amounts of R-  
250 phycocyanin were also determined at the optimal conditions (0.62 ± 0.02 mg/g) confirming that  
251 PE is the major PBP found in *G. gracilis*. Regarding the ultrasound-assisted extraction, the  
252 predicted optimum extraction conditions (t<sub>1</sub> = 17.5 min, t<sub>2</sub> = 7.5 min, C = 0.26 M, and R = 1:27)  
253 yielded 1.60 ± 0.12 mg PE/g biomass and 0.37 ± 0.03 mg PC/g biomass. On the other hand, the  
254 ultrasonic probe extracted 1.57±0.10 mg PE/g biomass and 0.44 ± 0.01 mg PC/g biomass using  
255 the predicted optimum extraction conditions (t<sub>1</sub> = t<sub>2</sub> = 10 min, C = 0.26 M, and R = 1:50). In  
256 the three extraction methods, the experimental PE yields were lower than the predicted values,  
257 at optimal conditions.

258 Considering the results obtained with RSM optimization, the following optimal conditions have  
259 been selected for the freeze-thaw extraction: C = 0.1 M, R = 1:50, and t<sub>1</sub> = 10 min. Two freezing  
260 temperatures (-80 °C and -20 °C) and two thawing temperatures (4 °C and RT (approximately  
261 19 °C)) were tested (Figure S2, Supplementary material). The maximum extraction was obtained

262 when freezing at -80 °C and thawing at 4 °C ( $1.51 \pm 0.03$  mg PE/g biomass). In general, the PE  
 263 yields obtained did not present significant differences between them ( $p > 0.05$ ), except for when  
 264 the samples were frozen at -20 °C and thawed at RT, in which case lower yields were obtained.  
 265 Longer thawing times may lead, therefore, to higher yields. In freeze-thaw method, ice crystals  
 266 form during the freezing step (Soni, Kalavadia, Trivedi, & Madamwar, 2006) that upon thawing  
 267 break down the cellular walls and release the intracellular content directly (Hardouin, Bedoux,  
 268 Burlot, Nyvall-Collén, & Bourgougnon, 2014). Therefore, repeated cycles of the freeze-thaw  
 269 are often used to achieve higher yields (Li et al., 2019; Mittal et al., 2017; Senthilkumar, Suresh,  
 270 et al., 2013) although some studies have shown that the increase in PBPs yield is not significant  
 271 (Kannaujiya et al., 2017; Lawrenz, Fedewa, & Richardson, 2011; Thoisen, Hansen, & Nielsen,  
 272 2017).

273

274 **Table 1.** R-phycoerythrin (PE) yields (mg PE/g biomass) for maceration, ultrasonic bath, and ultrasonic  
 275 probe extractions. Experimental PE yields were calculated using Eq. 1 and predicted values were  
 276 calculated by the model.

Run	Variables				PE yield (mg PE/g biomass)					
	R (mL)	C (M)	t1 (min)	t2 (min)	Maceration		Ultrasonic bath		Ultrasonic probe	
					Exp. <sup>a</sup>	Pred. <sup>b</sup>	Exp. <sup>a</sup>	Pred. <sup>b</sup>	Exp. <sup>a</sup>	Pred. <sup>b</sup>
1	1.7	0.3	11.43	2.69	2.52	2.46	1.69	1.67	1.51	1.49
2	1.7	0.7	11.43	2.69	2.65	2.82	1.68	1.68	1.51	1.52
3	1.7	0.3	11.43	7.47	3.44	3.58	1.74	1.77	1.59	1.63
4	1.7	0.3	23.57	7.47	3.41	3.10	1.64	1.79	1.58	1.51
5	1.7	0.3	23.57	2.69	2.54	2.33	1.60	1.63	1.42	1.39
6	1.7	0.7	23.57	2.69	2.48	2.28	1.48	1.64	1.36	1.44
7	1.7	0.7	11.43	7.47	3.78	3.71	1.59	1.62	1.42	1.48
8	1.7	0.7	23.57	7.47	2.67	2.81	1.56	1.63	1.28	1.38
9	3.8	0.3	11.43	2.69	2.54	2.45	1.69	1.72	1.61	1.52
10	3.8	0.3	23.57	2.69	2.52	2.63	1.56	1.58	1.67	1.56
11	3.8	0.3	11.43	7.47	3.26	3.41	1.85	1.83	1.79	1.71
12	3.8	0.3	23.57	7.47	3.25	3.23	1.72	1.74	1.77	1.73
13	3.8	0.7	11.43	2.69	1.65	1.91	1.74	1.72	1.27	1.35
14	3.8	0.7	23.57	2.69	1.65	1.67	1.58	1.57	1.49	1.42
15	3.8	0.7	11.43	7.47	2.37	2.64	1.59	1.66	1.28	1.35
16	3.8	0.7	23.57	7.47	1.92	2.05	1.51	1.58	1.43	1.40
17 (c)	2.8	0.5	17.5	5.08	2.86	2.76	1.99	1.90	1.55	1.53
18	0.5	0.5	23.57	5.08	2.25	2.48	1.73	1.59	1.51	1.42

<b>19</b>	5	0.5	17.5	5.08	2.31	1.98	1.59	1.59	1.47	1.58
<b>20</b>	2.8	0.01	17.5	5.08	3.08	3.25	1.68	1.65	1.47	1.62
<b>21</b>	2.8	1	17.5	5.08	2.41	2.17	1.51	1.44	1.36	1.23
<b>22</b>	2.8	0.5	17.5	0.17	1.95	2.00	1.63	1.61	1.37	1.43
<b>23</b>	2.8	0.5	17.5	10	3.68	3.52	1.85	1.71	1.60	1.56
<b>24</b>	2.8	0.5	5	5.08	3.46	3.17	1.79	1.79	1.54	1.48
<b>25</b>	2.8	0.5	30	5.08	2.32	2.45	1.78	1.65	1.32	1.43
<b>26 (c)</b>	2.8	0.5	17.5	5.08	2.68	2.76	1.94	1.90	1.52	1.53
<b>Optimal<sup>c</sup></b>	10	5	10	0.1	<b>3.58</b>	<b>4.15</b>	-	-	-	-
<b>Optimal<sup>c</sup></b>	17.5	2.8	7.5	0.26	-	-	<b>1.60</b>	<b>1.88</b>	-	-
<b>Optimal<sup>c</sup></b>	10	5	10	0.26	-	-	-	-	<b>1.57</b>	<b>1.89</b>

277 <sup>a</sup> Experimental values of response.

278 <sup>b</sup> Predicted values of response (by RSM proposed model).

279 <sup>c</sup> Optimal conditions (maximum response) obtained by RSM model

280 t1 - homogenization time; t2 - treatment time; R – biomass: buffer ratio; C- buffer concentration; (c) – central  
281 point.

282

283

284

285 **Table 2.** R-phycoerythrin (PE) yields (mg PE/g biomass) for high pressure-assisted extraction.

286 Experimental PE yields were calculated using Eq. 1 and predicted values were calculated by the model.

Run	Variables			PE yield (mg PE/g biomass)	
	t2 (min)	P (MPa)	R (mL)	High pressure Exp. <sup>a</sup>	Pred. <sup>b</sup>
<b>1</b>	10	122	1.41	0.91	0.91
<b>2</b>	25	122	1.41	1.14	1.06
<b>3</b>	10	479	1.41	0.66	0.59
<b>4</b>	25	479	1.41	0.51	0.51
<b>5</b>	10	122	4.09	1.27	1.24
<b>6</b>	25	122	4.09	1.06	1.10
<b>7</b>	10	479	4.09	0.84	0.88
<b>8</b>	25	479	4.09	0.54	0.51
<b>9</b>	5	300	2.75	1.14	1.16
<b>10</b>	30	300	2.75	0.95	0.97
<b>11</b>	17.5	0.1	2.75	1.02	1.04
<b>12</b>	17.5	600	2.75	0.25	0.28
<b>13</b>	17.5	300	0.50	0.65	0.72
<b>14</b>	17.5	300	5.00	1.03	1.00
<b>15 (c)</b>	17.5	300	2.75	1.10	1.05
<b>16 (c)</b>	17.5	300	2.75	1.05	1.05
<b>17 (c)</b>	17.5	300	2.75	1.05	1.05
<b>18 (c)</b>	17.5	300	2.75	1.03	1.05

<b>19 (c)</b>	17.5	300	2.75	1.12	1.05
<b>20 (c)</b>	17.5	300	2.75	0.96	1.05
<b>Optimal<sup>c</sup></b>	5	300	5	-	<b>1.32</b>

287 <sup>a</sup> Experimental values of response.

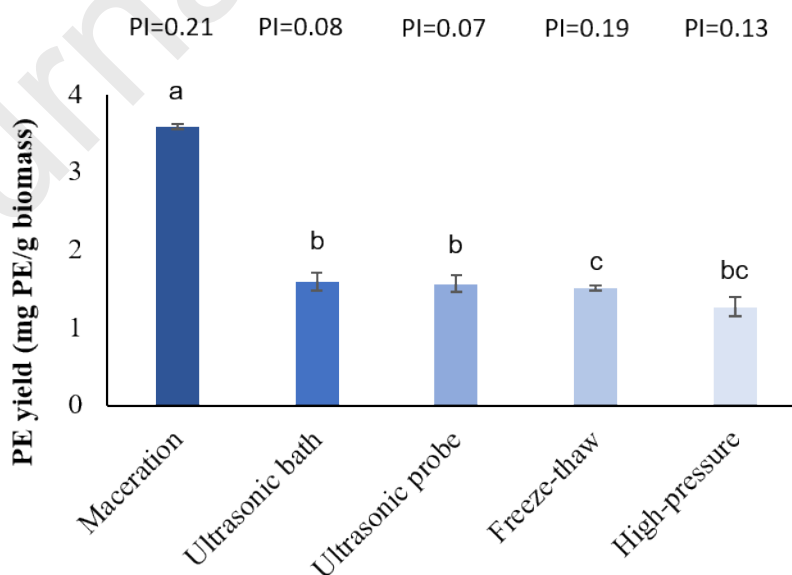
288 <sup>b</sup> Predicted values of response (by RSM proposed model).

289 t<sub>2</sub> - treatment time; P – pressure; R – biomass: buffer ratio; C- buffer concentration; (c) – central point.

290

291 Figure 2 compares the PE yields obtained with the different extraction methods tested. The  
 292 values used for comparison were the PE yields obtained at optimal conditions for maceration  
 293 and ultrasound-assisted extraction (bath and probe) and the best experimental values for freeze-  
 294 thaw and high pressure-assisted extraction. Although all the methods tested succeeded in the  
 295 extraction of pigments from freeze-dried macroalgae, maceration was the most advantageous  
 296 method affording yields of 3.58 mg PE/g biomass, approximately 55-65% more than the other  
 297 methods tested. Maceration also afforded PE with the higher purity index (PI). Phycobiliproteins  
 298 are known to be temperature sensitive, which may account for the higher yields obtained with  
 299 maceration, as the ultrasounds and high pressure induce an increase in the extract temperature  
 300 that can cause pigment denaturation. No statistically significant differences ( $p > 0.05$ ) were  
 301 found between ultrasound (bath and probe) and high pressure-assisted extractions and between  
 302 freeze-thawing and high pressure-assisted extraction.

303



304

305 **Figure 2.** Comparison of PE yields obtained using the different extraction methods. The corresponding  
306 purity indexes (PI), calculated with equation 3, are also presented for each method. PE yields are  
307 expressed as mean  $\pm$  SD ( $n = 3$ ). Values with unlike letters differ significantly ( $p < 0.05$ ).

308

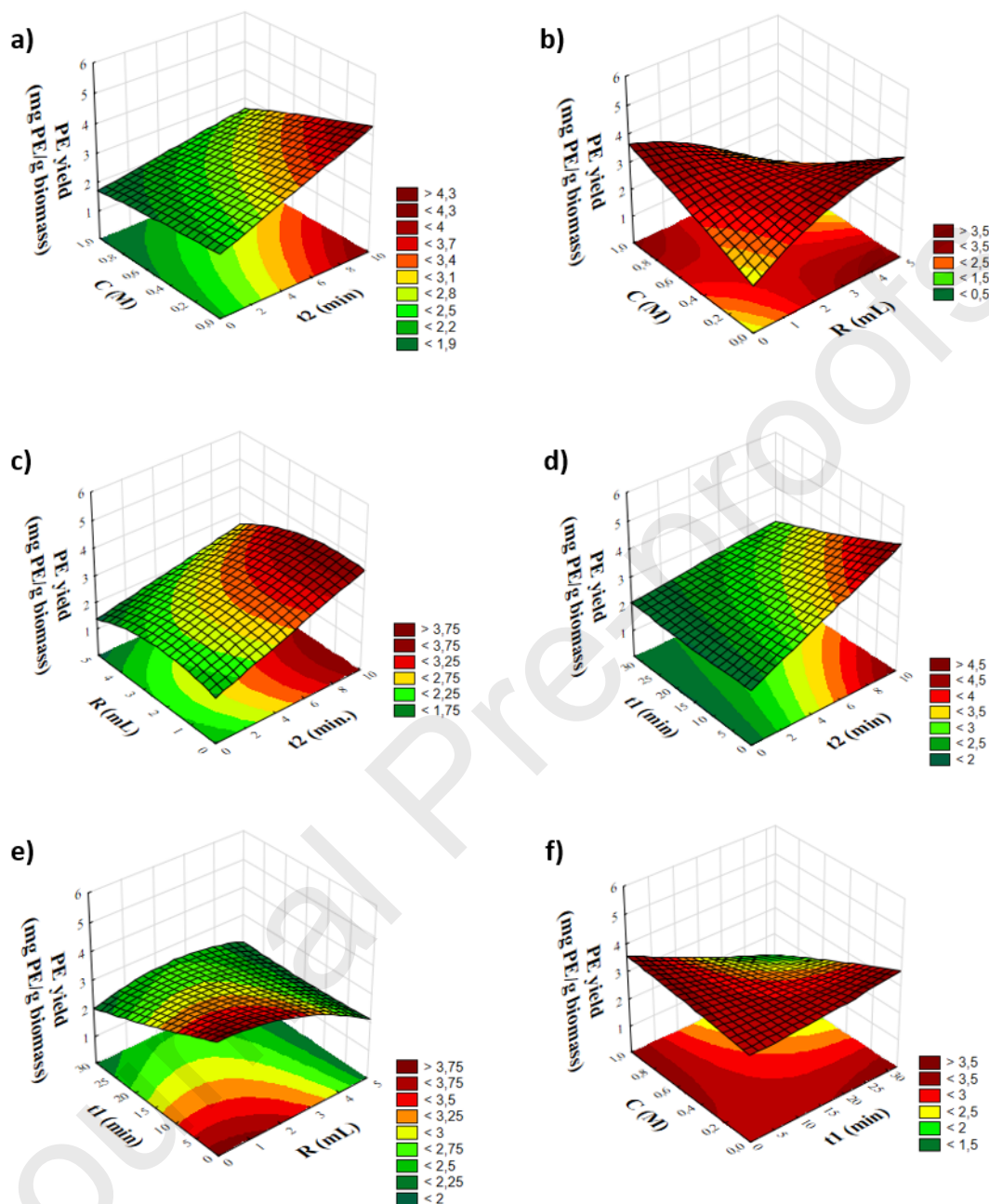
### 309 **3.2 Response surface methodology and statistical analysis**

310 Analysis of the maceration results showed that there were statistically significant differences ( $p$   
311  $< 0.05$ ) in all variables tested, as well as in the interaction between concentration and solid-  
312 liquid ratio, and the more impactful variables in the extraction yield were  $t_2$  and C (Table S3,  
313 Supplementary material). A coefficient of determination ( $R^2$ ) of 0.90 indicated a good  
314 agreement of the model with the experimental results (Figure S3, Supplementary material). The  
315 lack of fit of 0.34 ( $p > 0.05$  non-significant; supplementary material, Table S1) also indicated  
316 that, for the maceration process, the model was well adjusted to the experimental values  
317 representing the actual relationships of parameters well within the selected range (Bezerra et al.,  
318 2008).

319 The influence exerted by the variables on the extraction yield during the maceration process is  
320 displayed in the Pareto chart presented in the Supplementary material (Figure S4). At a 95%  
321 confidence level, the linear effect of  $t_2$  (L) (6.64) was the most significant in PE extraction,  
322 followed by the negative linear effect of C (L) (-3.96), linear effect of R (L) (-3.41), linear effect  
323 of R:C (L) (-3.25), and linear effect of  $t_1$  (L) (-3.21). The positive and linear effect of  $t_2$  indicates  
324 that the extraction yield increases with the increase of this variable while the negative and linear  
325 effect of the other variables suggests that the extraction will be more efficient using lower values  
326 of these conditions. This is shown in the response surface plots presented in Figure 3, which  
327 clearly illustrate the combined effects as well as visually describes these extraction tendencies.

328





329

330 **Figure 3.** Response surface plots for PE yield (mg PE /g biomass) using maceration, with the combined  
 331 effects of a) C (M) and R (mL of buffer); b) C (M) and t<sub>2</sub> (min); c) R (mL of buffer) and t<sub>2</sub> (min); d) t<sub>1</sub>  
 332 (min) and t<sub>2</sub> (min); e) t<sub>1</sub> (min) and R (mL of buffer); and f) C (M) and t<sub>1</sub> (mL of buffer).

333

334



335 The same process was followed for the ultrasound-assisted extractions. The analysis of the  
336 results showed that using the ultrasonic bath there were only statistically significant differences  
337 ( $p < 0.05$ ) in variables R and C with an  $R^2$  of 0.67 and a lack of fit of 0.23 ( $p > 0.05$  non-  
338 significant; supplementary material, Table S2). At a 95% confidence level, the most significant  
339 effect on PE extraction is the negative quadratic effect of C (-3.10), followed by the quadratic  
340 effect of R (-2.66) (Supplementary material, Figure S5). The quadratic and negative effects of  
341 C and R mean that the increase of these variables will increase the extraction of the pigment to  
342 a certain point, from which, even increasing these variables, the extraction decreases. The  
343 response surface plots shown in Figure S6 (Supplementary material) illustrate the combined  
344 effects of the different variables and visually describe the extraction trends.

345 As for the extractions using an ultrasonic probe, the ANOVA showed that there are only  
346 statistically significant differences ( $p < 0.05$ ) in C and, like with the ultrasonic bath, an  $R^2$  of  
347 0.68 and a lack of fit of 0.15 ( $p > 0.05$ ; supplementary material, Table S5). At a 95% confidence  
348 level, the only significant effect on the PE extraction is the negative linear effect of C (-3.40)  
349 (Supplementary material, Figure S7). This negative and linear effect suggests that the extraction  
350 yield decreases with the increase of the C. This effect can be seen in Figure S8 (Supplementary  
351 material), where the surface response plot illustrates the combined effect that the variables exert  
352 in the extraction tendency.

353 Finally, in the analysis of high pressure-assisted extraction, the ANOVA showed that there are  
354 statistically significant differences in all the conditions tested as well as in the interactions  
355 between  $t_2$  and P and between  $t_2$  and R, with an  $R^2$  of 0.97 and lack of fit of 0.34 ( $p > 0.05$  non-  
356 significant) (Supplementary material, Table S6). At a 95% confidence level, all variables were  
357 significant in PE extraction, as shown in Figure S9 (Supplementary material). The Pareto charts  
358 display the effect exerted by the variables on the extraction yield in the maceration process. The  
359 most significant effect on PE extraction is the negative linear (-13.42) and quadratic (-8.39)  
360 effect of P, followed by the positive linear (4.95) and negative quadratic (-4.07) effect of R, the  
361 negative combined effect of R and  $t_2$  (-3.34), negative linear effect of  $t_2$  (-3.23), and negative  
362 combined effect of  $t_2$  and P (-2.68). This suggests that the increase of the variables tested leads  
363 to a decrease of the extraction yield indicating that the extraction could be more efficient using  
364 lower values of these variables. Figure S10 (Supplementary material) represents the surface

365 response plots illustrating the effects that the combinations of variables have on the extraction  
366 yield.

367 Knowing the individual and combined effects that each variable exerts on the extraction of PEs,  
368 a model was constructed to predict the optimum conditions at which higher PE yields can be  
369 extracted. For maceration, the predicted optimum conditions ( $t_1 = t_2 = 10$  min,  $C = 0.1$  M, and  
370  $R = 1:50$ ) gave a PE yield lower than the one foreseen with the RSM (Table 1) but within the  
371 confidence interval. This proved the good prediction accuracy of the model to the optimal  
372 conditions of R-phycoerythrin extraction. Regarding the ultrasound-assisted extraction, the  
373 predicted optimum extraction conditions ( $t_1 = 17.5$  min,  $t_2 = 7.5$  min,  $C = 0.26$  M, and  $R = 1:27$ )  
374 gave a lower PE yield than the one predicted by the model (Table 1), which falls out of the  
375 confidence interval predicted by the model. This discrepancy could be caused by the bad fit of  
376 the model for this method, with a low  $R^2$  that only explains 66.5% of the experimental results.  
377 External factors could have contributed to the unfit adjustment of the model, such as the water  
378 temperature in the ultrasonic bath as well as the ultrasonic wave intensity that throughout the  
379 experiment were not controlled and could somehow have influenced the results. The ultrasonic  
380 probe, similarly to the results for the ultrasonic bath, gave a lower PE yield than the one  
381 predicted by the model (Table 1) at optimal conditions ( $t_1 = t_2 = 10$  min,  $C = 0.26$  M, and  $R =$   
382  $1:50$ ) but unlike the previous process one that fits within the confidence interval. This proves  
383 that the statistical model was reasonably adjusted to the experimental values and that the  
384 discrepancy could be caused by the low  $R^2$ , which only explains 67.9% of the experimental  
385 results. Overall, the response surface methodology resulted in accurate models capable of  
386 predicting the experimental values, proving to be a good procedure to optimize extraction  
387 methods.

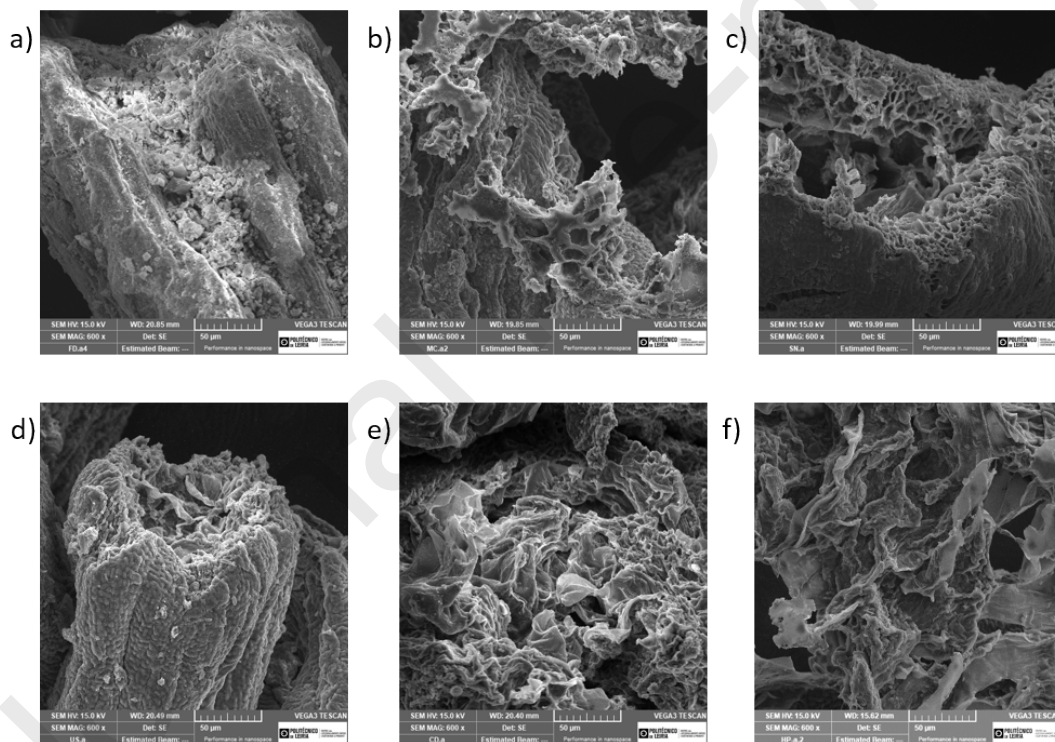
388

### 389 **3.3. Biomass analysis by Scanning Electron Microscopy**

390 To better understand the structural effects that the extraction methods have on the biomass,  
391 Scanning Electron Microscopy images of the biomass were acquired before and after the  
392 extraction processes. Figure 4 shows that there are significant differences in the biomass when  
393 compared with the control (freeze-dried biomass prior to treatment) in the extent to which the

394 cells are ruptured, facilitating the release of PBPs into the extraction buffer. Maceration (Figure  
 395 4, b) appears to promote the cell wall breakage to a higher extent than with the other extraction  
 396 methods (Figure 4, c-f). On the other hand, the use of an ultrasonic probe (Figure 4, c) improves  
 397 the exposure to the solvent, and thus enhances the simultaneous extraction of chlorophyll  
 398 compounds along with the PBPs. Although freeze-thawing and high-pressure seem to promote  
 399 a high extent of cell damage (Figure 4, e and f), it does not break the cell walls completely and  
 400 as efficiently as the maceration, leading to lower releases of PBPs. These observations were  
 401 consistent with the yields obtained during PE extraction optimization and may explain the better  
 402 results achieved with maceration.

403



404

405 **Figure 4.** SEM images of the *Gracilaria gracilis* biomass cells a) before and b)-f) after the extraction  
 406 treatments (b – maceration, c – ultrasonic probe, d - ultrasonic bath, e - freeze-thaw, f - high pressure-  
 407 assisted extraction) at a magnification of 600x.

408

409

410

#### 411 **4 Conclusion**

412 The extraction of PBP pigments from *Gracilaria gracilis* was optimized using different  
413 extraction methods. RSM proved useful in the optimization of PE extraction, providing a model  
414 with a good agreement between the experimental and predicted results. Maceration was the most  
415 efficient extraction method yielding 3.6 mg PE/g biomass at optimal conditions ( $t_1 = t_2 = 10$   
416 min,  $C = 0.1$  M, and  $R = 1:50$ ), which was 55-65% higher than the PE yields obtained with the  
417 other methods tested. The most impactful variable in the extraction process was treatment time  
418 ( $t_2$ ), with higher treatment times yielding higher concentrations of PE, whilst the least  
419 significant variable was homogenization time ( $t_1$ ) variable. SEM analysis showed the effect  
420 caused by the different extraction methods on the biomass, which agreed with PE yields  
421 obtained. *G. gracilis* revealed a good source of PE, that could be used as food colorant.

422

#### 423 **Declaration of Competing Interest**

424 The authors declare that they have no known competing financial interests or personal  
425 relationships that could have appeared to influence the work reported in this paper.

426

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435

436 **Appendix:** Supplementary material

437

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### 588 **Highlights**

- 589 • The extraction of PBP pigments from red algae *G. gracilis* was optimized using RSM
- 590 • Maceration proved to be a suitable process for PE extraction from *G. gracilis*
- 591 • The most impactful variable in the extraction process was extraction time
- 592 • SEM analysis revealed a more efficient cell wall rupture using maceration

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### 595 **CRedit author statement**

596 **Tatiana Pereira:** Investigation, Writing - Original Draft, Visualization; **Sônia Barroso:**  
597 Supervision, Writing - Review & Editing, Visualization; **Susana Mendes:** Formal analysis,  
598 Writing - Review & Editing, Validation; **Renata A. Amaral:** Investigation; **Juliana R. Dias:**  
599 Investigation; **Teresa Baptista:** Resources; **Jorge A. Saraiva:** Resources, Writing - Review

600 & Editing, Validation; **Nuno M. Alves:** Resources, **Maria M. Gil:** Conceptualization,  
 601 Supervision, Funding acquisition, Project administration, Resources, Validation.

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Conceptualization	Ideas; formulation or evolution of overarching research goals and aims
Methodology	Development or design of methodology; creation of models
Software	Programming, software development; designing computer programs; implementation of the computer code and supporting algorithms; testing of existing code components
Validation	Verification, whether as a part of the activity or separate, of the overall replication/ reproducibility of results/experiments and other research outputs
Formal analysis	Application of statistical, mathematical, computational, or other formal techniques to analyze or synthesize study data
Investigation	Conducting a research and investigation process, specifically performing the experiments, or data/evidence collection
Resources	Provision of study materials, reagents, materials, patients, laboratory samples, animals, instrumentation, computing resources, or other analysis tools
Data Curation	Management activities to annotate (produce metadata), scrub data and maintain research data (including software code, where it is necessary for interpreting the data itself) for initial use and later reuse
Writing - Original Draft	Preparation, creation and/or presentation of the published work, specifically writing the initial draft (including substantive translation)
Writing - Review & Editing	Preparation, creation and/or presentation of the published work by those from the original research group, specifically critical review, commentary or revision – including pre-or postpublication stages
Visualization	Preparation, creation and/or presentation of the published work, specifically visualization/ data presentation
Supervision	Oversight and leadership responsibility for the research activity planning and execution, including mentorship external to the core team
Project administration	Management and coordination responsibility for the research activity planning and execution
Funding acquisition	Acquisition of the financial support for the project leading to this publication

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