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Food-grade hydroxypropyl methylcellulose-based formulations for electrohydrodynamic processing: Part I – role of solution parameters on fibre and particle production

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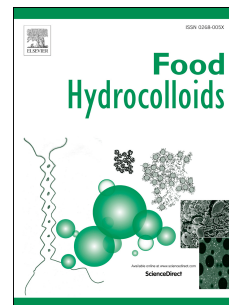
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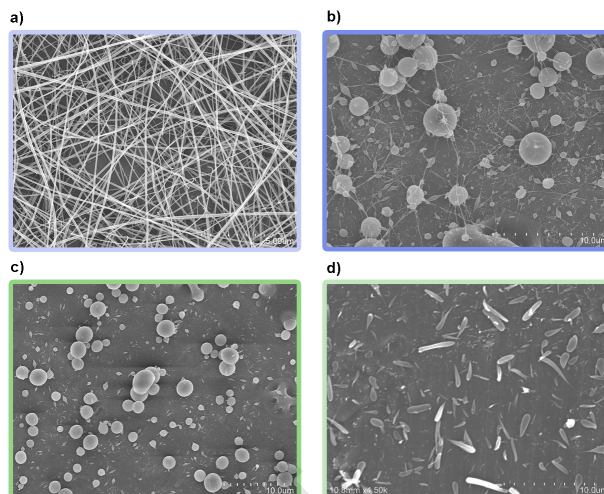
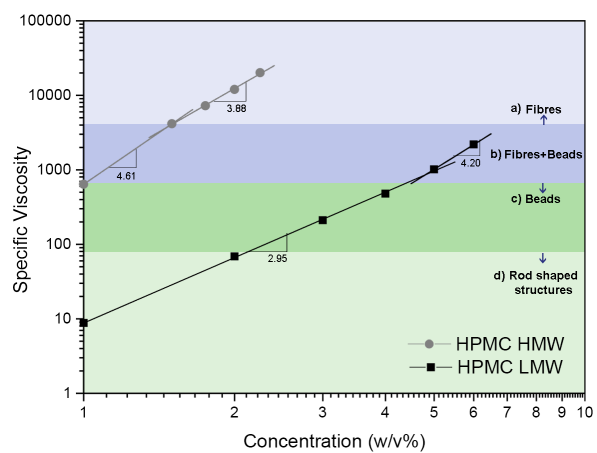
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Author Statement

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1 Short communication

2

3 Food-grade hydroxypropyl methylcellulose-based formulations for electrohydrodynamic  
4 processing: Part I – role of solution parameters on fibre and particle production

5

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16

## 17 **Abstract**

18 Electrohydrodynamic (EHD) processing allows the production of micro and nano  
19 structures with high surface-area-to-volume ratio from biopolymers and environmentally  
20 friendly solvents. Such structures hold a very significant potential for application in the  
21 food area. The aim of this work was to assess the role of solution parameters in the  
22 formation of hydroxypropyl methylcellulose (HPMC)-based micro and nanostructures  
23 through EHD processing, establishing a relationship between variables such as  
24 viscosity and concentration, and processing zones (i.e., combinations of processing  
25 conditions that move the system towards electrospinning – fibres are formed – or  
26 electro spraying – particles are formed).

27 Micro and nano structures were produced through electrospinning and electro spraying  
28 using HPMC with low (HPMC LMW) and high (HPMC HMW) molecular weight.  
29 Solutions were characterized regarding surface tension, conductivity, viscosity, zero-  
30 shear rate and specific viscosity. Plotting specific viscosity *versus* concentration

31 allowed determining the electro spraying and electro spinning zones, which were  
32 confirmed through scanning electron microscopy analysis. HPMC LMW led to the  
33 formation of particles. For concentrations between 1 and 2 % (w/v) rod like particles  
34 were formed, and round particles were obtained for concentrations ranging from 3 to 6  
35 % (w/v). The mean particle diameter varied between 833 and 1188 nm, while the  
36 aspect ratio ranged from 1.3 to 3.7. Nanofibres were generated using HPMC HMW,  
37 being beaded fibres produced at a concentration of 1 % (w/v) and smooth fibres  
38 produced for concentrations between 1.5 and 2.25 % (w/v). The developed nanofibres  
39 displayed a mean diameter ranging between 79 and 161 nm.

40 Electro spraying and electro spinning zones were successfully determined for HPMC  
41 LMW and HMW. Nevertheless, near transition zones variability regarding the obtained  
42 morphology was observed once other processing parameters (e.g., flow rate) can  
43 influence the morphology of fibers and particles.

44

45 **Keywords:** Electrohydrodynamic Processing; Electro spinning zone; Electro spraying  
46 zone; Aspect Ratio; Specific Viscosity; Nanotechnology.

47

## 48 1. Introduction

49 Over the last decades, the interest in micro and nano structures has been increasing in  
50 different areas, such as food and biomedicine. Given the need for properties such as  
51 biocompatibility, low toxicity and low cost, biopolymers have been presented as one of  
52 the materials of great interest for the development of these structures (Abuzar et al.,  
53 2018; Bourbon, Barbosa-Pereira, Vicente, Cerqueira, & Pastrana, 2020; Nunes et al.,  
54 2020; Zhang et al., 2018). The use of biopolymers in the design of micro and nano  
55 structures allows the development of structures that possess high surface-area-to-  
56 volume ratios, and a tunable and versatile morphology (Costa et al., 2019; Lasprilla-  
57 Botero, Álvarez-Láinez, & Lagaron, 2018; Limongi et al., 2017; Senthil Muthu Kumar et  
58 al., 2019).

59 One of the biopolymers that has been increasingly used in the food and biomedical  
60 industries is the polysaccharide hydroxypropyl methylcellulose (HPMC). This increase  
61 is explained by its biocompatibility, low toxicity, solubility in different solvents, and  
62 approval for use in a wide range of applications. HPMC is a cellulose ether with  
63 substituted hydroxyl groups, allowing for control of properties, such as solubility and  
64 viscosity (Burdock, 2007; Kaur et al., 2018; Pal, Paulson, & Rousseau, 2013; Sun,

65 Liang, Tan, & Wang, 2018). It is currently widely used as a direct or indirect food  
66 additive in the food industry (Chowhan, 1980; Stephen, Phillips, & Williams, 2016;  
67 Tanti, Barbut, & Marangoni, 2016).

68 These industries have widely used the encapsulation of bioactive compounds or drugs  
69 through methodologies such as spray-drying, complex coacervation, emulsification and  
70 salting-out (Cerqueira et al., 2014; Karim et al., 2016; Katona, Sovilj, Petrović, &  
71 Milanović, 2010; Romita, Cheng, & Diosady, 2011; Silva et al., 2019). Currently used  
72 techniques have disadvantages such as making use of temperature, pressure, or  
73 leading to low encapsulation efficiencies, which can be a problem depending on the  
74 encapsulated compound and the field of application (Costa et al., 2019; García-  
75 Moreno, Mendes, Jacobsen, & Chronakis, 2018; Marques et al., 2019; Rodrigues et al.,  
76 2020). Electrohydrodynamic (EHD) processing arises as an up-and-coming  
77 encapsulation technology, presenting a high encapsulation efficiency, low cost,  
78 allowing room or ambient working conditions, as well as controllable temperature and  
79 humidity, if needed. EHDs allows a versatile production of micro and nano structures  
80 with high surface-area-to-volume ratio, combined with a narrow size distribution, simply  
81 by fine tuning its processing parameters. These characteristics and properties are of  
82 extreme interest for the production of micro and nano structures for the food industry,  
83 as the recent increase in publications and applications in this area shows (Costa et al.,  
84 2019; Deng, Kang, Liu, Feng, & Zhang, 2018; García-Moreno et al., 2018; Liao, Loh,  
85 Tian, Wang, & Fane, 2018; Rodrigues et al., 2020; Senthil Muthu Kumar et al., 2019).  
86 Parameters that influence structure morphology include voltage, tip-to-collector  
87 distance, flow rate, the selected solvent and polymer, its concentration and the  
88 viscosity of the solution obtained with it (Costa et al., 2019; García-Moreno et al., 2018;  
89 Marques et al., 2019; Senthil Muthu Kumar et al., 2019; Wang, Jansen, & Yang, 2019).

90 EHD processing has been used to produce particles and fibres using different  
91 polysaccharides. However, despite HPMC being frequently used in the food and  
92 biomedical industries, its stand-alone use in EHD processing for the development of  
93 food grade micro and nano structures is unexplored. Existing reports typically make  
94 use of non-aqueous and non-GRAS solvents, limiting the applicability of the developed  
95 structures based on HPMC in the food industry. In EHD processing, HPMC is most  
96 often used blended with other polymers or used to produce solid amorphous  
97 dispersions that lack a defined and reproducible morphology (Aydogdu, Sumnu, &  
98 Sahin, 2019; Mahesh, Kathyayani, Nanjundaswamy, Channe Gowda, & Sridhar, 2019;  
99 Smeets, Clasen, & Van den Mooter, 2017; Smeets, Koekoekx, Clasen, & Van den  
100 Mooter, 2018; Zhou et al., 2019). Therefore, the need exists for exploring the use of

101 food-grade biomaterials, such as HPMC, in EHD processing technologies, with food  
102 grade and generally recognized as safe solvents, for the development of micro and  
103 nano structures with well-defined and reproducible morphology. Viscosity and surface  
104 tension are essential parameters that need to be studied in order to predict the  
105 produced structures (particles or fibres, thus defining electrospinning and  
106 electro spraying zones, respectively) and to control their morphology through EHD  
107 processing. To this point, such work has not yet been developed while using HPMC  
108 (Faramarzi, Barzin, & Mobedi, 2016; Huang et al., 2019; Lee et al., 2018). In this  
109 sense, an analysis of the relationship between concentration, viscosity, surface  
110 tension, concentration regimes and chain entanglements is important to define the  
111 electrospinning and electro spraying zones. This kind of study has been previously used  
112 with other polymers, such as polyimide, zein, poly(lactic-co-glycolic acid), among  
113 others, but has not yet been used for HPMC (Bhushani, Kurrey, &  
114 Anandharamakrishnan, 2017; Lasprilla-Botero et al., 2018; Tiwari & Venkatraman,  
115 2012).

116 In this work, high and low molecular weight HPMC were used to produce food-grade  
117 fibres and particles by an EHD process (electrospinning and electro spraying,  
118 respectively), using an ethanol-water mixture (75%) as solvent. A relationship between  
119 the viscosity of the formulations and the morphology of electro spun fibres or particles  
120 was established, and potential electrospinning and electro spraying zones were  
121 proposed. Polymer solutions were then combined with electrohydrodynamic working  
122 conditions to produce micro and nano structures from HPMC. The developed micro  
123 and nano structures were then characterised regarding their morphology, and  
124 electrospinning and electro spraying zones were determined.

## 125 **2. Materials and Methods**

### 126 2.1. Materials

127 Hydroxypropyl methylcellulose (HPMC 45847) (methoxyl 28-30 %, hydroxypropyl 7-12  
128 %, viscosity 2 % aqueous solution with a viscosity range of 7500-14000 mPa.s, at 20  
129 °C, 746 kDa) and hydroxypropyl methylcellulose (HPMC 44779) (methoxyl 28-30 %,  
130 hydroxypropyl 7-12 %, viscosity 2 % aqueous solution with a viscosity range of 40-60  
131 mPa.s at 20 °C, 90 kDa) were purchased from Alfa Aesar GmbH & Co KG (Germany),  
132 absolute ethanol EPR PH.EUR. (>99.5 %) was purchased from LabKem (Spain).

### 133 2.2. Preparation of polymer solutions for electrohydrodynamic processing

134 HPMC (1, 2, 3, 4, 5 and 6 % of HPMC 44779, and 1, 1.5, 1.75, 2 and 2.5 % of HPMC  
135 45847) was slowly added to a solvent consisting of a mixture of pure ethanol (75 % v/v)

136 and distilled water (25 % v/v) in a closed plastic container and left to stir magnetically  
137 overnight at room temperature ( $\approx 20$  °C). The polymer solutions obtained were then  
138 filtered through a mesh to remove any solid impurities and were ready to be used after  
139 standing for a few hours to ensure removal of air bubbles. Ethanol at 75 % (v/v) was  
140 selected as solvent due to the partial solubility of HPMC in both ethanol and water.  
141 These conditions will allow a higher versatility for the produced structures, which will be  
142 then able to incorporate both lipophilic and hydrophilic compounds.

### 143 2.3. Characterisation of polymer solutions

#### 144 2.3.1. Rheological analysis

145 A Discovery Hybrid Rheometer (DHR) (TA Instruments, New Castle, USA) was used to  
146 determine the zero-shear rate and the specific viscosity of the solutions. TA  
147 Instruments Trios v.4.1.133073 software was used to collect the data. Up-down-up flow  
148 sweeps between  $0.01\text{ s}^{-1}$  and  $300\text{ s}^{-1}$  were conducted, using a 60 mm, 2.006°, cone  
149 geometry, at room temperature ( $\approx 25$  °C).

150

#### 151 2.3.2. Surface Tension

152 Surface tension was determined using a Force Tensiometer- K20 (Kruss, Hamburg,  
153 Germany) using the Du Noüy ring method. 15 mL of the sample were placed in a  
154 vessel placed on the tensiometer platform, then a Du Noüy ring was suspended from  
155 the pendulum and placed inside the vessel to be analysed. The Du Noüy ring was  
156 carefully cleaned, with abundance of water, between measurements. Samples were  
157 analysed at room temperature ( $\approx 23$  °C).

158

#### 159 2.3.3. Electrical conductivity

160 Solution conductivity was measured using a HI2003-02 Edge conductivity meter  
161 (Hanna, Rhode Island, USA). 5 mL of solution were transferred to a Falcon tube and  
162 the probe was submerged until the sensors were covered and stabilised. All  
163 measurements were made at room temperature ( $\approx 23$  °C).

164

### 165 2.4. Electrohydrodynamic processing conditions

166 The EHD processing equipment was a Spinbox Systems® from Bioinicia S.L.  
167 (Valencia, Spain) and was equipped with a variable high voltage power supply (0-30  
168 kV). 10 mL plastic syringes were used to host the polymer solutions and were  
169 electrospun and electrosprayed under a steady flow rate using a blunt stainless-steel  
170 needle with a diameter of 0.601 mm (20 G). The needle was connected to the syringe  
171 through a Polytetrafluoroethylene (PTFE) tube and was horizontal to the collector. The



172 syringe was coupled to a digitally controlled syringe pump. Electrohydrodynamic testing  
 173 conditions are presented in Table 1. The relative humidity ranged between 31 % and  
 174 51 % for all experiments.

175

## 176 2.5. Characterisation of structures

### 177 2.5.1. Morphology

178 Produced micro and nano structures were analysed regarding their morphology using a  
 179 scanning electron microscope (Hitachi S-4800, Tokyo, Japan) after being coated with a  
 180 gold–palladium mixture under vacuum for 3 min (SC7640, Polaron, Kent, UK). SEM  
 181 analyses were carried out with 1–2 mg of sample at 10 kV. Between 100 and 200 fibres  
 182 or particles were measured using ImageJ software (v1.52a).

183 Samples were analysed regarding diameter, diameter distribution, aspect ratio and  
 184 aspect ratio distribution for particles and diameter and diameter distribution for fibres.  
 185 At least 200 fibres or particles were measured. The particle diameter is represented as  
 186 the average height and length of particles.

187 Particle diameter distribution measures the homogeneity of the produced  
 188 microstructures (Equation 1), while the particle aspect ratio (Equation 2) assesses  
 189 structure morphology, which is required to be spherical. Particle aspect ratio  
 190 distribution (Equation 3) assesses how homogeneous the shape of the produced  
 191 particles is across the diameter range of the produced particles.

192

$$193 \text{ Particle diameter distribution} = \left( \frac{\text{Particle diameter standard deviation}}{\text{Particle Diameter}} \right)^2 \quad \text{Equation 1}$$

$$194 \text{ Particle aspect ratio} = \frac{\text{Particle Height}}{\text{Particle Length}} \quad \text{Equation 2}$$

$$195 \text{ Particle aspect ratio distribution} = \left( \frac{\text{Particle aspect ratio standard deviation}}{\text{Particle Aspect Ratio}} \right)^2 \quad \text{Equation 3}$$

195

196 Fibre diameter distribution (Equation 4) measures the homogeneity of the produced  
 197 nanostructures which is optimal when at its lowest.

198

$$199 \text{ Fibre diameter distribution} = \left( \frac{\text{Fibre Diameter standard deviation}}{\text{Fibre Diameter}^2} \right)^2 \quad \text{Equation 4}$$

## 200 2.6. Statistical analyses

201 Statistical analyses were performed using analysis of variance, Tukey's mean  
202 comparison test ( $p < 0.05$ ) and results were reported as an average and standard  
203 deviation, using Origin 9.0 software (OriginLab Corporation, 2012) and GraphPad  
204 Prism 8.4.3 (GraphPad Software, LLC, 2020). A minimum of 3 replicates were  
205 performed.

206

## 207 3. Results and discussion

### 208 3.1. Solution properties

209 The selection of a solvent is intertwined with the conductivity and surface tension, as  
210 these two properties can vary significantly from solvent to solvent. In EHD processing,  
211 a higher conductivity is usually associated with smoother and smaller micro and nano  
212 structures, as it allows an easier formation of the Taylor cone, needed for the correct  
213 formation of the fibres and particles. Surface tension is another critical parameter in the  
214 formation of the Taylor cone: a lower surface tension results in easier EHD processing.  
215 The applied voltage must overcome the solvents' surface tension in order to develop a  
216 Taylor cone. In this case, the use of an ethanol/water mixture (75 % v/v) leads to a  
217 decrease of water surface tension, from 57.17 mN/m for water to around 25 mN/m for  
218 the ethanol/water mixture. The same behaviour was observed for polymer solutions.  
219 The conductivity, on the other hand, increased from 0.37  $\mu\text{S}/\text{cm}$  for distilled water to  
220 0.9  $\mu\text{S}/\text{cm}$  for the ethanol/water mixture, as shown in Table 2. The biopolymer also  
221 affects the conductivity, where higher concentrations and MW lead to higher  
222 conductivity values. Results showed that HPMC solutions with the same polymer  
223 concentration (1 and 2 % w/w from both HP) but different MW (low and high), had  
224 different conductivity results, with solutions prepared from HPMC with higher MW  
225 displaying higher values of conductivity.

226 Results also show that the polymer concentration and MW influence viscosity.  
227 Typically, higher MWs and polymer concentrations result in higher viscosity values for  
228 the polymer solutions, which then affect the production of micro and nano structures.  
229 This influence is explained by the increase in chain entanglements that occurs for  
230 higher MW polymers and at higher concentrations. Chain entanglements represent the  
231 physical interlocking of polymer chains, and for polymer solutions the solution  
232 entanglement number ( $ne_{(soln)}$ ) is also affected by the polymer concentration. Higher  
233 chain entanglements help stabilising the electrospinning jet, allowing for solvent  
234 evaporation and fibre formation (McKee, Wilkes, Colby, & Long, 2004; Shenoy, Bates,  
235 Frisch, & Wnek, 2005)

236 The magnitude of  $n_{e(soln)}$  values obtained will depend on the regime of the solution.  
 237 These regimes are divided in: i) “dilute regime”, typically more appropriate for  
 238 electrospinning ( $n_{e(soln)} < 2$ ); ii) “semi-dilute unentangled regime” for  $n_{e(soln)}$  values between  
 239 2 and 3.5, where the likelihood of electrospinning of both fibres and beads increases,  
 240 and iii) “semi-dilute entangled regime” obtained for  $n_{e(soln)}$  values higher than 3.5, where  
 241 electrospinning of smooth fibres is more likely to happen (Bock, Dargaville, & Woodruff,  
 242 2012; Lee et al., 2018; McKee et al., 2004; Shenoy et al., 2005).

243 Thus, the viscosity and concentration of polymer solutions and MW of the polymer are  
 244 extremely important in the prediction of the type of structure that can be obtained.  
 245 Supplier information indicates that HPMC 44779 is of low viscosity (40-60 mPa·s in a 2  
 246 % aqueous solution at 20 °C), which can be adequate for electrospinning, while HPMC  
 247 45847 has a higher viscosity (7500-14000 mPa·s in a 2 % aqueous solution at 20 °C),  
 248 and thus could be used to produce nanofibers (Lasprilla-Botero et al., 2018; Tiwari &  
 249 Venkatraman, 2012).

250 Figure 1 presents the rheological profile of the formulations. The polymer solutions  
 251 displayed a non-Newtonian behaviour, within the concentration range tested. The  
 252 viscosity decreased for higher shear rate, being this trend more noticeable in the  
 253 HPMC HMW samples. Figure 1 shows the dependence of viscosity on concentration,  
 254 with higher concentrations leading to higher viscosity values. For a proper comparison  
 255 between samples, the zero-shear rate viscosity ( $\eta_0$ ) of each sample was determined  
 256 through data fitting by Cross’s model (Stephen et al., 2016), and is presented in Table  
 257 2. Results show that only at its higher concentrations (> 4 %) the HPMC LMW present  
 258 values close to the HPMC HMW values at the lowest concentration (1 %).

259 Table 2 shows that the zero-shear rate viscosity increases from 15.71 mPa·s to  
 260 3509.49 mPa·s for the HPMC LMW, as concentration increases from 1 to 6 % (w/v),  
 261 while for the HPMC HMW viscosity increases from 1030.73 mPa·s to 33035.88 mPa·s  
 262 when the concentration increases from 1 to 2.25 % (w/v). The influence of the polymer  
 263 on the  $\eta_0$  was evaluated by determining each solution’s specific viscosity ( $\eta_{sp}$ ), through  
 264 Equation 5, in which  $\eta_s$  is the solvent viscosity.

$$\eta_{sp} = \frac{\eta_0 - \eta_s}{\eta_s} \quad \text{Equation 5}$$

265 Results presented in Table 2 show the same trend as seen in the zero-shear rate  
 266 viscosity measurements. The values increase for higher polymer concentrations and  
 267 reach higher values for HPMC HMW when compared to HPMC LMW. Results also  
 268 show that at the highest concentrations of HPMC LMW (6 %) the values are similar to  
 269 those found for the lowest concentration of the HPMC HMW (1 %). This indicates that  
 270 at the highest concentrations of HPMC LMW the EHD processing could result in a

271 structure of particles with fibres (or fibres with particles), something that was confirmed  
 272 in the SEM analysis presented below.

273 In the dilute regime ( $C \ll C_e$ ), the specific viscosity ( $\eta_{sp}$ ) increases exponentially with  
 274 concentration, presenting a slope of 1.0 ( $C^{1.0}$ ), while in the semi-dilute unentangled  
 275 regime ( $C < C_e$ ) the exponential increase presents a slope value of 1.25 ( $C^{1.25}$ ). In these  
 276 regimes, the formation of particles and beaded fibres is favoured, but as concentration  
 277 increases, chain overlapping initiates, viscosity changes abruptly, and a point, that can  
 278 be defined as the entanglement concentration ( $C = C_e$ ),  $C_e$  is reached. A semi-diluted  
 279 entangled regime is entered ( $C > C_e$ ) and  $\eta_{sp}$  reflects the abrupt change in viscosity by  
 280 scaling with concentration to the power of 4.8 ( $C^{4.8}$ ). A concentrated regime ( $C^{**}$ ) is  
 281 entered as concentration and viscosity further increase and  $\eta_{sp}$  scales at the power of  
 282 3.6 ( $C^{3.6}$ ). To determine the solution type of regime, as well as to estimate  $C_e$  and  $C^{**}$ ,  
 283 specific viscosity and concentration were plotted in a log-log plot. These plots are  
 284 presented in Figure 2. The abrupt changes in the slope mark the transition between  
 285 different regimes.  $C_e$  marks the beginning of the semi diluted entangled regime, and  
 286  $C^{**}$  marks the beginning of the concentrated regime, both of which are regions more  
 287 prone to produce fibres, with the concentrated regime typically producing smoother  
 288 fibres with lower diameters (Bock et al., 2012; Lee et al., 2018; McKee et al., 2004;  
 289 Shenoy et al., 2005).

290 For the HPMC HMW, the first slope change occurs when the concentration moves from  
 291 1 to 1.5 %, marking the transition from the semi dilute unentangled regime to the semi  
 292 dilute entangled regime, in which the  $C_e$  is determined to be 1.5 %. The second slope  
 293 change (as concentration increases from 1.5 % to 2 %) marks the concentrated regime  
 294 ( $C^{**} = 2$  %). Slope changes displayed in Figure 2 show that the semi-dilute entangled  
 295 regime,  $\eta_{sp} \sim C^{4.61}$ , and the concentrated regime,  $\eta_{sp} \sim C^{3.88}$ , are in good agreement with  
 296 the theoretically predicted scaling law exponents' values of 4.8 and 3.8. The dilute and  
 297 semi-dilute unentangled regimes were not determined as rheological analysis was not  
 298 conducted below 1 %. Results would indicate that an electrospinning zone can be  
 299 found for concentrations above 1.5 %, namely around 2 % where the  $C^{**}$  was found.

300 Regarding the HPMC LMW, the first slope change occurs when the concentration  
 301 increases from 1 % to 5 %, with an  $\eta_{sp} \sim C^{2.77}$ , while the second slope change occurs  
 302 between 5 % and 6 %, with an  $\eta_{sp} \sim C^{4.20}$ . It marks the transition between the semi-  
 303 diluted unentangled regime and the semi-diluted entangled regime, in which  $C_e = 6$  %,   
 304 shifting from a zone in which the formation of particles is expected to a zone in which  
 305 fibres would be the obtained structure. Results show that for the semi-diluted  
 306 unentangled regime the obtained values ( $\eta_{sp} \sim C^{2.95}$ ) do not present a good fit with the

307 theoretical values ( $\eta_{sp} \sim C^{1.25}$ ), however for the semi dilute entangled regime, the obtained  
308 values  $\eta_{sp} \sim C^{4.8}$ , fit well with the theoretical value ( $\eta_{sp} \sim C^{4.20}$ ).

309 This crossover point is usually identified as ideal to produce particles, as there is  
310 enough entanglement of molecular chains in this transition to produce particles in a  
311 stable and reproducible form, without producing fibres. Nevertheless, transition zones  
312 can be a fertile ground for the production of mixed structures (with both particles and  
313 fibres) as slight changes in the EHD parameters (e.g., voltage, flow rate, working  
314 distance) will influence the final outcome (Bock et al., 2012; Faramarzi et al., 2016; Lee  
315 et al., 2018; Shenoy et al., 2005). After the determination of theoretical electrospinning  
316 and electrospinning zones, the structures obtained from the polymer solutions  
317 processed by EHD were evaluated regarding their morphology.

318

### 319 3.2. Micro and nano structure analysis

320 The electrospinning and electrospinning zones that were previously determined, were  
321 confirmed by submitting the polymer solutions to EHD processing. Needle diameter,  
322 solution flow rate, voltage and distance values were kept constant, except for one  
323 formulation of HPMC HMW in which voltage varied and was adjusted to obtain a visible  
324 Taylor cone at the tip of the spinneret and without visible droplets in the collector.  
325 Typically, for higher concentrations, due to higher sample viscosity, higher voltage and  
326 distance combinations were needed to produce a stable Taylor cone. The resulting  
327 structures were evaluated by SEM and are presented in Figure 3. It is possible to see  
328 that for all tested concentrations some type of structure was produced. At low  
329 concentrations, namely 1 and 2 % (w/v), rod-shaped structures were formed, but by  
330 increasing the concentration (up to 5 %) rounder particles were produced and at the  
331 highest tested concentration (6 %) larger beads connected with fibres, 'beads-on-a-  
332 string', were obtained. This was more noticeable at higher flow rates than lower flow  
333 rates.

334 Based on the results, low concentrations of HPMC LMW (1-2 %) were not considered  
335 as appropriate for electrospinning, as round particles were not obtained, while the  
336 highest concentration (6 %) was also not considered appropriate due to the  
337 simultaneous production of round particles and fibres. These results agree with the  
338 results obtained in the specific viscosity *versus* concentration plot analysis, where an  
339 abrupt increase in viscosity is seen at 6 % (w/v) solutions, indicating the presence of  
340 both beads and fibres. Thus, based on these results, polymer concentrations between  
341 3 and 5 % (w/v) seem more appropriate to produce particles.

342 Figure 4 presents SEM images of the structures obtained using HPMC HMW. Results  
343 show that HPMC HMW was appropriate to produce fibres as all tested formulations

344 resulted in fibres, although in some of the formulations used (namely at the lower  
345 concentrations of 1 and 1.5 %) beaded fibres were obtained. It was also observed that  
346 some samples presented droplets among the fibres, indicating that higher voltages  
347 might be needed for appropriate processing, namely, to allow a proper solvent  
348 evaporation. Less beading of the fibres was observed at higher polymer concentrations  
349 (from 1.75 to 2.25 % w/v) which seem to be more appropriate to obtain fibres. As  
350 observed for the particle production, the electrospinning zones predicted through the  
351 specific viscosity *versus* concentration plot analyses matched the results observed by  
352 SEM, given that samples above 1.5 % seemed to produce more adequate fibres, with  
353 less beading.

354 The structures observed in Figure 3 and Figure 4 show the adequacy of the previously  
355 predicted electrospaying and electrospinning zones for both HPMC tested (LMW and  
356 HMW), validating the use of this methodology for HPMC. In Figure 5 it is also possible  
357 to see the influence of other parameters of EHD processing, especially near transition  
358 zones, on the structural morphology (in this case, the influence of flow rate). In one of  
359 those regime's transition zones, at a concentration of 6 %, an increase of the amount of  
360 fibres in the 'beads-on-string' structure can be obtained by changing the flow rate of the  
361 EHD process from 500 to 1000  $\mu\text{L}/\text{h}$ .

362 Figure 5 shows that despite being extremely important variables, polymer  
363 concentration and viscosity are not be-all's and end-all's when it comes to determining  
364 and tuning the structure morphology, and a more comprehensive study of the  
365 parameters that influence structure morphology, and how they influence it, is  
366 necessary. As such, further research on the influence of processing and solution  
367 parameters or properties should be conducted.

368 Sample morphology was analysed, and structures produced from HPMC LMW  
369 displayed rod-like and spherical morphology, and in some formulations produce both  
370 particles and fibres. HPMC HMW produced mostly fibrous structures, at times  
371 accompanied by particles. HPMC LMW structures were characterised regarding their  
372 particle diameter and sphericity, while HPMC HMW were characterised regarding their  
373 fibre diameter. These properties are presented in Table 3 and showed that  
374 microparticles size ranged between 800 and 1200 nm. When low concentrations are  
375 used (1 and 2 %) produced structures displayed a rod like morphology, while when  
376 higher concentrations are used (between 3 and 6 %) the process produced more  
377 spherical particles. For microparticles produced using 3 and 4 % of HPMC the aspect  
378 ratio (the closer the aspect ratio is to one the more spherical the particles are) is closer  
379 to one than that the microparticles produced at 5 and 6 %, formulations in which fibres  
380 were also produced. Formulations with 3 and 4 % of HPMC also lead to good aspect

381 ratio uniformity, diameter uniformity and span values. Particle diameters obtained here  
382 agree well with the results reported by Huang et al (2019), in which a modified coaxial  
383 electro spray was performed, using HPMC with the same type of substitution (type E,  
384 methoxyl 28-30%, hydroxypropyl 7-12%), a lower viscosity (5 mPa·s) and using a  
385 mixture of ethanol and dichloromethane (1:1) as solvent. The process was carried out  
386 at lower flow rates, which has been reported to decrease size distribution, but also has  
387 the drawback of decreasing the productivity (Faramarzi et al., 2016; Lee et al., 2018).  
388 The produced nanofibres displayed mean diameters ranging from 80 to 160 nm, with  
389 mostly low diameter uniformity and span values. The lowest diameter uniformity and  
390 span values were obtained at a concentration of 2.25 %, respectively with values of  
391 0.121 and 0.805. The highest values of diameter uniformity and span were obtained at  
392 a concentration of 1 %, respectively 1.93 and 1.59. This is probably because in this  
393 formulation beaded fibres were produced, causing a lower uniformity of the produced  
394 structures. An overarching trend regarding the influence of concentration on fibre  
395 diameter does not seem to exist, possibly due to the presence of beaded fibres in  
396 some of the samples, which artificially increase their mean diameter. For samples  
397 without beaded fibres (concentration at 2 % and 2.25 %) an increase in concentration  
398 leads to higher fibre diameter. In another work, aiming to produce nanofibres of similar  
399 diameters (around 120 nm) higher concentrations of HPMC and higher voltages were  
400 needed. This might be due to the use of slightly different processing parameters,  
401 namely the use of a different ratio (1:1) of water-ethanol, which resulted in lower  
402 viscosities and higher surface tensions (Frenot, Henriksson, & Walkenström, 2007).

403

#### 404 **4. Conclusions**

405 The use of EHD processing allowed to produce micro and nano structures using low  
406 and high viscosity HPMC. Round and spherical particles were produced using the  
407 HPMC LMW, at concentrations ranging between 3 and 5 % (w/v). All tested  
408 formulations of HPMC HMW were able to produce fibres, while the use of lower  
409 concentrations of HPMC HMW led to the production of beaded fibres (between 1 and  
410 1.5 %), while higher concentrations (1.75 to 2.25 %) led to the production of less  
411 beaded and smoother fibres. SEM morphology results confirmed the information  
412 obtained from the specific viscosity *versus* concentration plots for electro spraying and  
413 electro spinning zones. An electro spraying zone was found between 1 % and 5 % of  
414 HPMC LMW, while at 6 % particles of larger diameters and a mix of particles and fibres  
415 started to form, indicating a transition to an electro spinning zone. Particle diameter  
416 varied between 800 and 1200 nm, while aspect ratio varied between 1.316 and 3.732

417 (spherical particles and rod-shaped structures, respectively). Regarding HPMC HMW,  
418 fibres were formed at all tested concentrations, but at lower concentrations (below 1.5  
419 %) beaded fibres were produced. An electrospinning zone was thus defined between  
420 1.5 % and 2.25 %, with higher concentrations producing smoother fibres. The mean  
421 fibre diameter ranged from 80 to 160 nm. Additionally, it was also possible to  
422 demonstrate that for systems operating near transition zones, other parameters such  
423 as the flow rate, can have a great influence on the structure morphology. Therefore,  
424 future work should focus on the assessment of the influence of the remaining  
425 parameters on particle and fibre morphology, especially doing so at higher flow rates to  
426 increase productivity as this is one of the main drawbacks of the use of EHD  
427 processing. This assessment would ideally be conducted with a Design of Experiments  
428 methodology to understand better the relationship and influence between the different  
429 process or solution parameters and the morphological outcome of the produced  
430 structures.

431

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- 595  
596  
597

598 **Table 1** Electrohydrodynamic processing testing conditions

Biopolymer	Solvent	Needle	Tip-to-collector distance (cm)	Voltage (kV)	Concentration (w/v %)	Flow rate (mL/h)
Hydroxypropyl methylcellulose LMW	Ethanol 75% (v/v)	20G (0.601 mm)	15	10	1 to 6	0.5 to 1
Hydroxypropyl methylcellulose HMW			20	12 to 18	1 to 2.25	1

599

600

601 **Table 2** Surface tension, conductivity, zero shear rate viscosity and specific viscosity of the polymer and  
602 solvent solutions. Different letters, for the same HPMC, in the same column indicate statistically significant  
603 differences ( $p < 0.05$ )

Sample	Concentration (w/v)	Surface tension (mN/m)	Conductivity ( $\mu\text{S/cm}$ )	Zero shear rate viscosity (mPa·s)	Specific viscosity
Water	-	57.2 $\pm$ 0.8	0.37 $\pm$ 0.12	N.D.	N.D.
Ethanol	75% (v/v)	25.1 $\pm$ 0.1	0.90 $\pm$ 0.00	N.D.	N.D.
HPMC LMW	1	25.0 $\pm$ 0.1 <sup>a</sup>	5.13 $\pm$ 0.06 <sup>a</sup>	15.71 $\pm$ 12.40 <sup>a</sup>	8.76 $\pm$ 7.71 <sup>a</sup>
	2	25.0 $\pm$ 0.1 <sup>a</sup>	9.50 $\pm$ 0.20 <sup>b</sup>	111.93 $\pm$ 51.65 <sup>a</sup>	68.57 $\pm$ 32.11 <sup>a</sup>
	3	25.3 $\pm$ 0.1 <sup>b</sup>	13.00 $\pm$ 0.10 <sup>c</sup>	340.29 $\pm$ 25.04 <sup>a</sup>	210.51 $\pm$ 15.56 <sup>a</sup>
	4	25.1 $\pm$ 0.1 <sup>ab</sup>	16.73 $\pm$ 0.25 <sup>d</sup>	769.20 $\pm$ 64.06 <sup>b</sup>	477.11 $\pm$ 39.82 <sup>b</sup>
	5	25.1 $\pm$ 0.1 <sup>ab</sup>	19.40 $\pm$ 0.40 <sup>e</sup>	1633.86 $\pm$ 93.96 <sup>c</sup>	1014.54 $\pm$ 58.40 <sup>c</sup>
	6	25.1 $\pm$ 0.1 <sup>ab</sup>	22.33 $\pm$ 0.12 <sup>f</sup>	3509.49 $\pm$ 382.28 <sup>d</sup>	2180.36 $\pm$ 194.01 <sup>d</sup>
HPMC HMW	1	24.9 $\pm$ 0.1 <sup>a</sup>	8.33 $\pm$ 0.06 <sup>a</sup>	1030.73 $\pm$ 95.35 <sup>a</sup>	639.66 $\pm$ 59.26 <sup>a</sup>
	1.5	25.1 $\pm$ 0.1 <sup>ab</sup>	12.30 $\pm$ 0.27 <sup>b</sup>	6687.30 $\pm$ 774.62 <sup>b</sup>	4155.56 $\pm$ 481.47 <sup>b</sup>
	1.75	25.3 $\pm$ 0.1 <sup>b</sup>	13.87 $\pm$ 0.06 <sup>c</sup>	11656.11 $\pm$ 2420.33 <sup>c</sup>	7243.97 $\pm$ 1504.38 <sup>c</sup>
	2	25.7 $\pm$ 0.1 <sup>c</sup>	15.97 $\pm$ 0.15 <sup>d</sup>	19312.61 $\pm$ 3181.63 <sup>d</sup>	12002.95 $\pm$ 1440.03 <sup>d</sup>
	2.5	26.1 $\pm$ 0.1 <sup>d</sup>	17.23 $\pm$ 0.23 <sup>e</sup>	33035.88 $\pm$ 1012.30 <sup>e</sup>	20090.98 $\pm$ 924.10 <sup>e</sup>

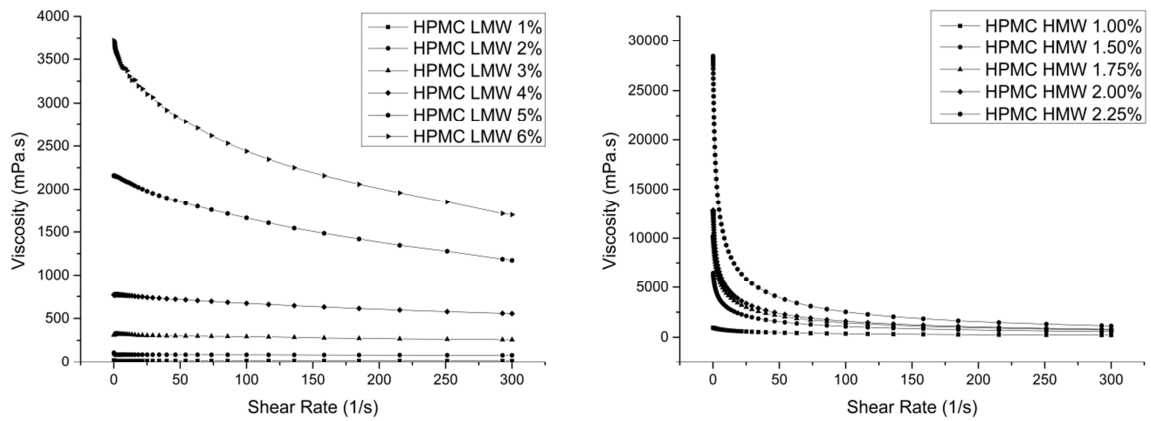
604

605 **Table 3** Aspect Ratio, aspect ratio uniformity, diameter, diameter uniformity and span of LMW and HMW  
606 HPMC micro and nanostructures.  
607

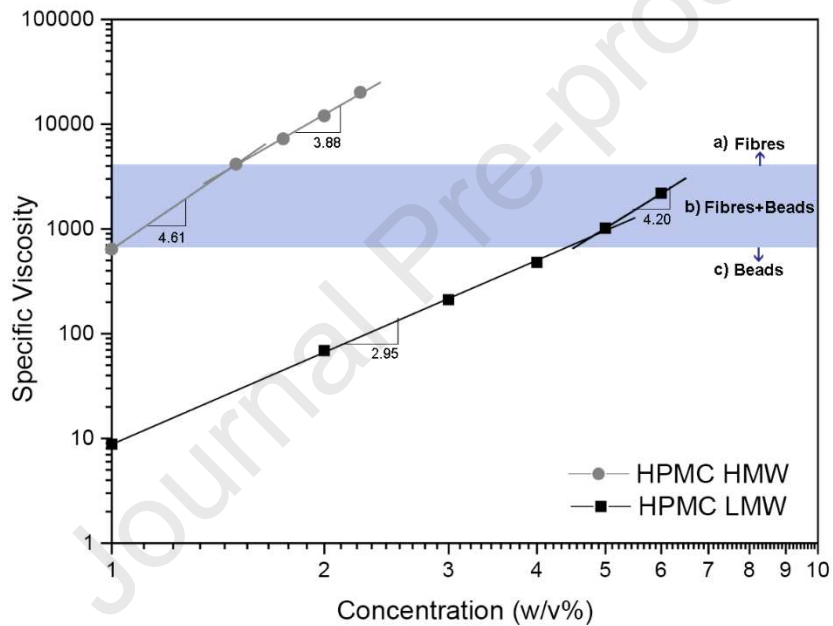
Sample	Aspect Ratio	Aspect Ratio Uniformity	Diameter (nm)	Diameter Uniformity	Span
LMW HPMC 1%	3.7	0.15	973	0.52	2.38
LMW HPMC 2%	2.1	0.27	994	0.25	1.31
LMW HPMC 3%	1.3	0.23	833	0.20	1.18
LMW HPMC 4%	1.3	0.10	1188	0.28	1.65
LMW HPMC 5%	2.0	0.48	906	0.32	1.74
LMW HPMC 6%	1.7	0.54	931	0.43	1.79
HMW HPMC 1%	-	-	151	1.93	1.59
HMW HPMC 1.5%	-	-	142	0.15	0.90
HMW HPMC 1.75%	-	-	161	0.34	0.88
HMW HPMC 2%	-	-	79	0.14	0.82
HMW HPMC 2.25%	-	-	107	0.12	0.81

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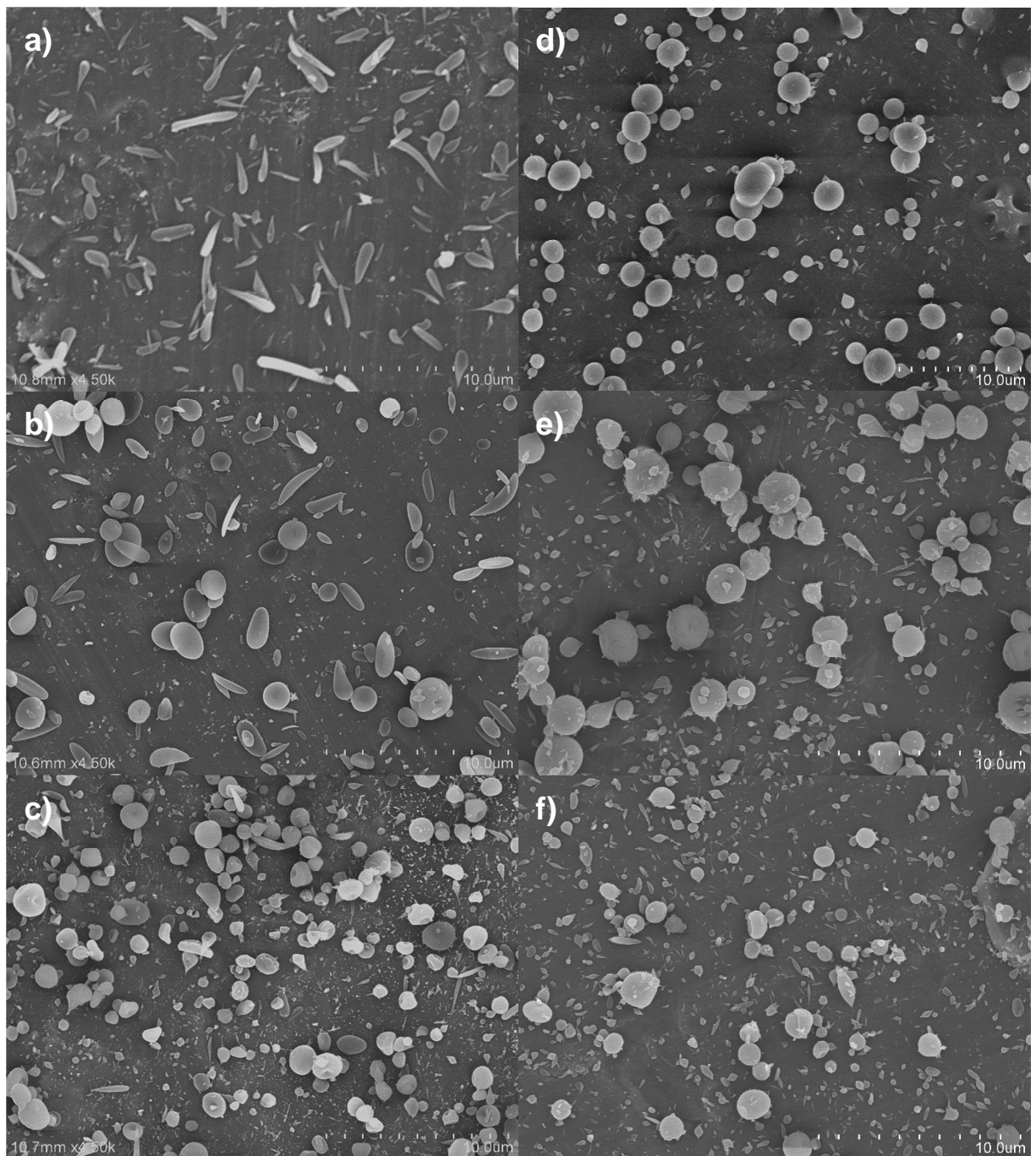
611 **Figure 1** – Viscosity profile of polymer solutions over a range of shear rates (0.01 to 300 s<sup>-1</sup>).

612

613 **Figure 2** Specific viscosity for different concentrations of HPMC LMW (Mw=90 kDa) and HPMC HMW  
614 (Mw=746 kDa). The blue zone represents the conditions where fibre+beads are obtained.

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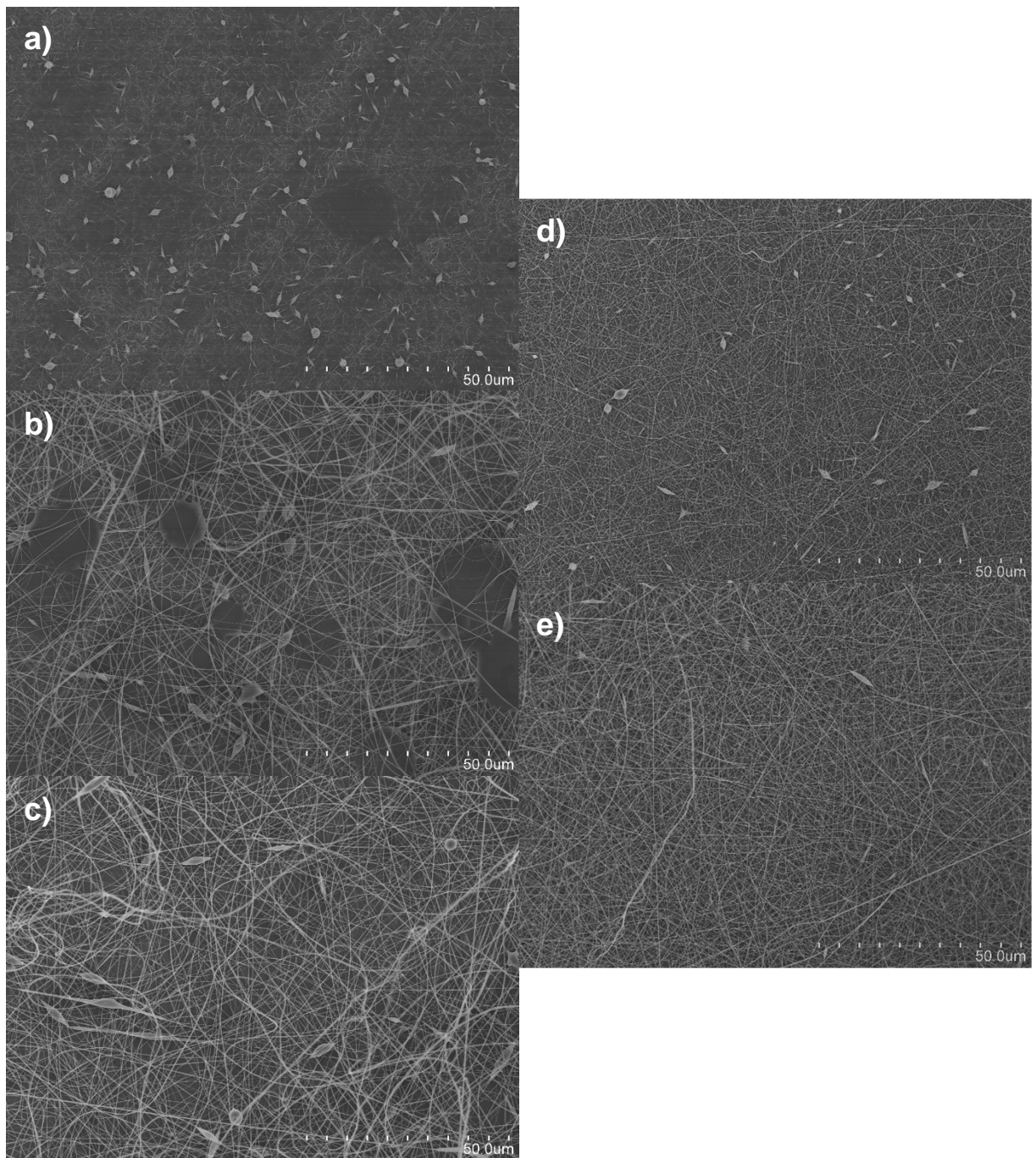


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618 **Figure 3** SEM imaging for the low viscosity samples. a) 1 %, b) 2 %, c) 3 %, d) 4 %, e) 5 %, f) 6 %.

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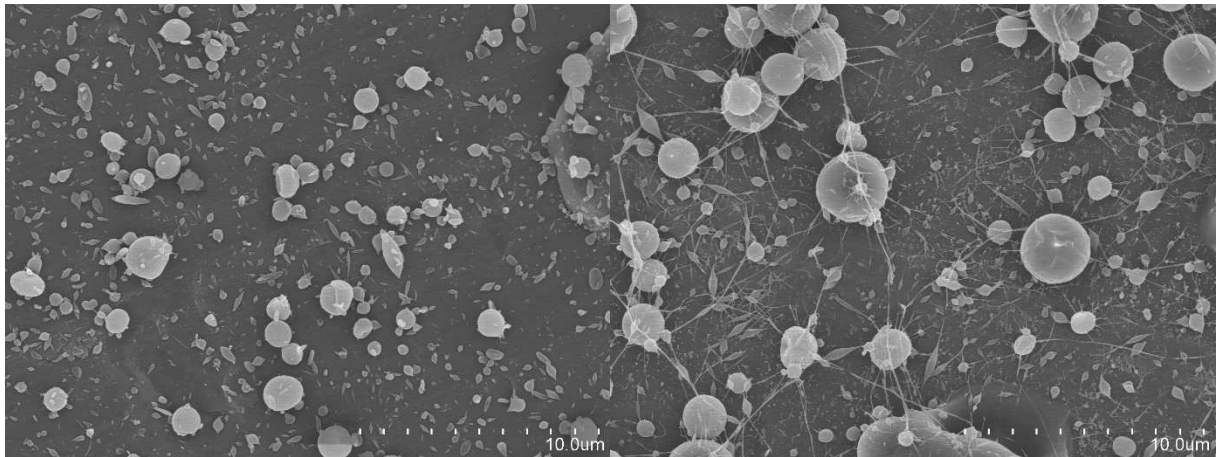




620

621 **Figure 4** SEM imaging for the high viscosity samples. a) 1 %, b) 1.5 %, c) 1.75 %, d) 2 %, e) 2.25 %.

622



623

624 **Figure 5** Comparison between microstructures produced at different flow rates. 500  $\mu\text{L/h}$  (left), 1000  $\mu\text{L/h}$   
625 (right). Remaining parameters were the same. Polymer concentration of 6 % (w/v) of HPMC LMW, voltage  
626 10 kV, distance 15 cm.

627

628

## Highlights

- Electrospinning and electro spraying zones were estimated through viscosity analysis and confirmed through SEM analysis
- Low molecular weight HPMC led to the formation of rod-like and round particles
- High molecular weight HPMC led to the formation of beaded and bead-free fibres
- Food-grade HPMC microparticles and nanofibres were produced from stand-alone HPMC
- Assessment of the influence of other process parameters (e.g. flow rate, voltage) on particle and fibre morphology should be conducted in future works

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**Declaration of interests**

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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