1	All-Aqueous Freeform Fabrication of Perfusable Self-Standing Soft Compartments
2	
3	Raquel C. Gonçalves, Sara Vilabril, Catarina M. S. S. Neves, Mara G. Freire, João A. P.
4	Coutinho, Mariana B. Oliveira*, João F. Mano*
5	
6	R.C. Gonçalves, S. Vilabril, C.M.S.S. Neves, M.G. Freire, J.A.P. Coutinho, M.B. Oliveira,
7	J.F. Mano
8	Department of Chemistry, CICECO – Aveiro Institute of Materials. University of Aveiro.
9	3810-193 Aveiro, Portugal
10	E-mail: mboliveira@ua.pt, jmano@ua.pt
11	
12	Keywords: all-aqueous fabrication, tubular/hollow materials, aqueous two-phase systems,
13	interfacial complexation, cell encapsulation
14	
15	Abstract. Compartmentalized structures obtained in all-aqueous settings have shown
16	promising properties as cell encapsulation devices, as well as reactors for trans-membrane
17	chemical reactions. While most approaches focus on the preparation of spherical devices,
18	advances on the production of complex architectures have been enabled by the interfacial
19	stability conferred by emulsion systems, namely mild aqueous two-phase systems (ATPS), or
20	non-equilibrated analogues. However, the application of non-spherical structures has mostly
21	been reported while keeping the fabricated materials at a stable interface, limiting the free-
22	standing character, mobility, and transposition of the obtained structures to different setups.
23	Here, we show the fabrication of self-standing, malleable and perfusable tubular systems
24	through all-aqueous interfacial assembly, culminating in the preparation of independent objects
25	with stability and homogeneity after disruption of the polymer-based aqueous separating system.
26	Those hollow structures could be fabricated with a variety of widths, and rapidly printed as long
27	structures at flow rates of 15 mm s ⁻¹ . The materials were used as compartments for cell culture,
28	showcasing high cytocompatibility, and could be tailored to promote cell adhesion. Such
29	structures may find application in fields that benefit from freeform tubular structures, including
30	the biomedical field with e.g., cell encapsulation, and benchtop preparation of microfluidic
31	devices.
32	

- 33
- 34

35 **1. Introduction**

36 Strategies with high relevance in the biotechnology and bioengineering fields, including drug/protein delivery and enzyme immobilization, have relied on compartmentalization 37 approaches compatible with mild processing.^[1] Such encapsulation methods have been adapted 38 and extended to withstand cell encapsulation, relevant for tissue engineering and regenerative 39 40 medicine, and to recent technological developments on disease modelling.^[2] Most emphasis has 41 been given to spherical-shaped cell encapsulation systems due to ease of processing, as well as 42 to the architecture-enabled achievement of controlled molecular release profiles. More recently, 43 though, fibrillar and tubular geometries have gained momentum, mainly owing to their ability to mimic complex and hierarchical architectures of naturally occurring fiber-shaped and tubular 44 tissues including, for example, vasculature.^[2,3] Also, flexible fiber-shaped materials may be 45 deposited with high three-dimensional (3D) freedom, enabling the bottom-up fabrication of 46 complex geometries, much needed in tissue regeneration based on defect-filling strategies.^[4,5] 47 Other biomedical-related applications may reside in their integration on fluidics models^[6] or as 48 platforms for the generation of organoid models.^[7,8] 49

The direct fabrication of perfusable tubular materials with free-form distributions may 50 51 arise from techniques such as co-axial extrusion 3D printing. Those often require the use of one phase that gives rise to sacrificial templates that need subsequential removal with, for example, 52 53 ion chelating agents.^[9-13] On the other hand, all-liquid template-free strategies are most commonly based on the assembly of a variety of active materials such as surfactants^[14] or 54 nanoparticles^[15] at oil-aqueous interfaces.^[16] However, traces of oil or organic solvents may be 55 56 either difficult to wash and/or pose toxicity constrains. Aqueous two-phase systems (ATPS) 57 have emerged as interesting platforms to fabricate emulsion-based structures in all-aqueous environments. The aqueous environment provided by these systems has led to their application 58 59 in the processing of products for the tissue engineering and biomedical field.^[17] ATPS are 60 formed when two aqueous solutions containing incompatible polymers, salts or other agents, separate into two immiscible phases above certain critical concentrations.^[18] Dispersing 61 62 oppositely charged polyelectrolytes (PEs) in the different phases of the ATPS or their analogues has been explored as a way to produce biomaterials through a single-step interfacial 63 64 complexation. This method has been mainly used for the generation of PE spherical-shaped capsules and particles with potential applications in cell encapsulation, controlled release of 65 active agents^[19–23] and, more recently, for the fabrication of disease models.^[24] The processing 66 of such structures in tubular form through PE complexation is poorly explored^[25]. The few 67 68 studies reporting the fabrication of complex-shaped materials at the interface of all-aqueous

interfaces have proven their applicability as supports for intermembranous reactions^[25] and cell 69 70 encapsulation^[4] while kept at the stabilized ATPS, or "prototypical" ATPS interfaces based on non-equilibrium analogues^[25]. The effect of either using ATPS in equilibrium – as well as in 71 72 different equilibrium points -, or prototypical systems based on precursory aqueous polymer 73 solutions before equilibration, has been overlooked. Importantly, the ability of all-aqueous 74 systems to assist on the fabrication of materials with architectural complexity, homogeneity, 75 and ability to be handled after disruption of the interface remains unexplored. This has limited 76 the technique for the production of materials amenable to be independently handled and 77 positioned in more complex systems.

Here, we report the direct and rapid fabrication of perfusable fiber-shaped materials supported by the well-characterized ATPS composed of poly(ethylene glycol) (PEG) and dextran. By adjusting physical and chemical processing parameters, namely by exploring nonequilibrium and different equilibrium points of the ATPS, we prove the feasibility of processing self-standing, easy to handle and cytocompatible materials with membrane-bounded tubular shape.

84

85

2. Results and discussion

86 The interfacial complexation of two oppositely charged natural PEs – alginate (ALG) and 87 ϵ -poly-L-lysine (EPL) –, at physiological pH (7.2-7.4), was promoted at the interface of 88 different aqueous systems. In an initial experiment, a system based on an ATPS precursor 89 composed of aqueous PEG and dextran solutions was thoroughly characterized. For that, ALG 90 was dissolved in a 15 wt% dextran solution (phase I – inner phase) and immersed in a larger 91 volume solution made of EPL dissolved in a 17 wt% PEG solution (phase II – outer phase) 92 (Figure 1a). The formation of tubular structures was induced by dispensing a discrete phase 93 (phase I) into a continuous bath (phase II) by applying controlled continuous displacement.

94 The interaction between oppositely charged PEs was crucial for the development of stable 95 structures: when a PE-free phase I was immersed in a PE-free phase II, long threads were 96 formed upon the application of movement. However, the thread broke up into smaller droplets within less than 1 minute (Table S1, Supporting Information).^[17] When oppositely-charged PEs 97 98 were dissolved in the solutions, a condensed membrane was formed, which can probably be 99 ascribed to the electrostatic interaction between the charged groups of the polymers, as well as 100 the entropy gain upon the release of counter ions and solvating molecules in solution, in a phenomenon called PE complexation.^[26,27] Previous studies using PE complexation in ATPS 101 102 to produce biomaterials demonstrated that the phase in which the PEs are initially positioned

may influence the formed structure, as well as the ability to fabricate continuous materials with high stability while kept at the ATPS precursor interface.^[25,28] In an initial approach, we empirically investigated the effect of inversing the dissolution of both PEs in the phases. Macroscopic observations showed the formation of continuous and surface-homogeneous fibers when alginate was mixed in the inner phase (dextran), and EPL in the outer one (PEG). On the other hand, disintegrated structures were obtained when alginate and EPL were in the outer and inner phases, respectively (Figure S1, Supporting Information).

110 By using the optimized phase positioning and initially studied concentrations of 0.75 wt% 111 EPL and 2 wt% ALG, the formation of a detectable membrane at the interface around the 112 immersed phase took around 30 seconds (Figure 1b). Due to the aqueous nature of the system, 113 the dissolved PEs are hypothesized to slowly diffuse towards the interface of the ATPS 114 precursor. Overtime, polyions are expected to continuously interact, which correlates with the 115 gradually increasingly darkening of the membrane, and the consequent formation of more 116 robust fiber-shaped structures (Figure 1b,c). Interestingly, in the absence of the precursor ATPS, 117 the reaction between EPL and ALG (dissolved in PBS) led to the formation of structures with 118 poor malleability (Videos S1 and S2, Supporting Information), which were darker at 2 min of 119 complexation than any of the structures prepared using the ATPS precursor, regardless of 120 complexation time. Additionally, the gradual increase in the darkness observed for the materials 121 prepared in the non-equilibrium ATPS was not detectable in the non-equilibrium ATPS-free 122 setup, suggesting that the use of a non-equilibrated ATPS enable establishing time of 123 complexation as a parameter to easily induce morphological versatility in the prepared 124 membranes/tubes (Figure 1c). Since the membrane was formed at the interface of the aqueous 125 system, ones would expect that, by cutting off the ends of the materials, the produced fibers 126 would be hollow upon releasing their liquid content, producing tubular structures. Scanning 127 electron microscopy (SEM) micrographs of cross-sectioned and dehydrated fibers with 128 different complexation times allowed confirming the tubular/hollow feature of the fabricated 129 structures (Figure 1d).

130 Upon the disruption of the interface of the ATPS precursor, fiber-shaped solid structures 131 were retrieved to a saline medium without visible collapse (Figure 1e). Interestingly, the free-132 standing structures showed robustness and could be easily handled with tweezers both in a 133 water-based solution, as well as while in contact with air (Figure 1f,g). The microscopic 134 analysis of the membranes right after production and cross-sectioning allowed estimating a 135 thickness c.a. 7-12 μ m, with a slight increase on walls' thickness with increasing complexation 136 time (Figure S2a, Supporting Information).

137 A volumetric expansion of the fibers was observed upon washing in PBS, which was 138 hypothesized to be triggered by the disruption of the interfacial tension barrier from the ATPS 139 after complete removal of phase II during the washing. The disturbance of the aqueous interface 140 may had established osmotic gradients that induced the movement of water molecules towards the interior of the fibers, culminating in swelling.^[23] The expansion process was monitored over 141 142 time by registering the changes in fibers' diameter (Figure S2b, Supporting Information). The 143 average swelling ratio increased with time, and eventually reached equilibrium after 40 min for 144 all conditions. Moreover, fibers washed after a reduced time of complexation (2 and 5 min) 145 expanded in a higher extent than fibers with 10 and 15 min of complexation. As mechanical 146 analysis corroborates, lower complexation times led to the formation of softer fibers; therefore, 147 their membrane may more easily deform, and fibers expand more upon the entrance of water, 148 while stiffer fibers resist more to expansion resulting in lower swelling ratios. A tendency for 149 increasing elastic modulus with the increase in the complexation time was observed. 150 Statistically significant difference of almost two-fold was detected between 5 min (15 ± 0.7 151 kPa) and 15 min (27 ± 1.9 kPa), with fibers with increasing stiffness produced with increased 152 complexation times (Figure S2c, Supporting Information). The PE complexation has been 153 described to be mostly entropically driven, with a two-phase sequence firstly involving 154 formation of soluble complexes, and a second step involving coacervation (comprising water 155 expulsion), driving the formation of insoluble organized complexes.^[29] We speculated the 156 stiffening of the membranes formed at the interface of the system may be related with the 157 decreased hydration of the membranes as complexation time increases, as well as a putative 158 progressive organization of the coacervates. Therefore, softer fibers may have been obtained 159 from lower times of complexation due to their ability to retain and absorb higher amounts of 160 water. Using this system, the mechanical performance of fibers could be easily tuned by the 161 complexation time, presenting a range of stiffnesses resembling some native soft tissues such as cardiac and skeletal muscle^[30], providing them with potential for cell support and tissue 162 163 integration. The diameter of the fibers could easily be tuned by changing the needle used to 164 deposit phase I into phase II. Due to their water-swelling properties, the diameter significantly 165 increased for all the tested needle sizes after the washing process (Figure S2d, Supporting 166 Information). This approach allowed stablishing a range of low-dispersion external diameters 167 comprising macrometer $(1.50 \pm 0.19 \text{ mm})$ to micrometer scales $(0.25 \pm 0.03 \text{ mm})$, opening the 168 range of applications for the system.

169 Despite the tubular shape and handelability obtained for the studied times of 170 complexation using 0.75 wt% EPL and 2 wt% ALG in the ATPS precursor, the microscopic

171 observation of the obtained tubes after washing revealed uncontinuities in the membranes 172 (Figure 2a,b), especially for the ones produced using higher complexation times. Therefore, a more thorough study of processing conditions comprising different polymer concentrations, 173 174 times of complexation, and the pH of the solutions was performed. The yield of fibers that kept 175 a continuous character, without microscopically detectable opening or collapsing after washing 176 with PBS, followed by incubation at 37°C overnight, was calculated. Fibers were prepared using 177 a syringe pump system, which allowed controlling the flow rate of phase I, and achieve 178 increased reproducibility when compared to manual dispensing of solutions. Figure 2c 179 summarizes the stability yield obtained for all tested conditions, with solutions prepared at pH 180 ~7. A tendency for decreasing stability with increasing complexation times seems to occur, 181 regardless of PE concentrations. Beyond the attractive electrostatic interactions, the entropy 182 gain from the release of water is considered to be one of the driving forces for the formation of PE complexes or coacervates.^[26] In fact, it has been previously described that the presence of 183 184 highly hydrophilic polymers in solutions with oppositely charged PEs, enhance the dehydration of the PE constituents and favors entropically the formation of the coacervation condensate.^[31] 185 186 We therefore hypothesized that, with increasing time, the increasing PE interactions and consequent dehydration of the PE molecules and possible local accumulation of elastic stress^[32] 187 188 may have caused the tightening of the membrane mesh, inducing the opening of 189 thermodynamically instable areas of the fiber. The fact that an ATPS precursor, in a non-190 equilibrium state, was used to prepare the fibers may explain the formation of localized sites 191 with accumulated elastic stress in the forming fibers. The time for the first breakage of the PE-192 free precursor ATPS was assessed, with the first breakage being detected in less than 1 minute 193 after the filament extrusion (Table S1, Supporting Information).

194 Both alginate and EPL are weak polyelectrolytes, with a degree of ionization in solution 195 dependent on a dissociation constant, pKa.^[33] This property enables polymers to acquire fractional charges, which can be tuned by changing the solution's pH.^[34] Taking this aspect in 196 197 consideration, we evaluated the role of pH on the formation and stability of fiber-shaped 198 materials. More robust fibers were formed when the pH of the global system decreased to 5, 199 while increasing the pH to 9 prevented the formation of fibers (Figure 2d). This result was 200 deemed to be mainly influenced by the degree of protonation and conformation of EPL, since the charge density of alginate $(pKa \sim 3.2-3.6)^{[35]}$ was previously shown not to be significantly 201 influenced by solutions' pH above 5.^[36] At acidic pH, the repulsion of protonated amine groups 202 of EPL might promote an electrostatically expanded conformation^[37] which favors the 203 204 interaction with the carboxylic groups from alginate, thereby increasing the speed of

complexation (Figure 2d). Theoretically, EPL isoelectric point is assumed to be close to 9^[38]; 205 206 consequently, interfacial electrostatic interactions between the PEs at pH 9 is expected to be 207 mostly absent, which here may had prevented the formation of complexed membranes. This 208 was corroborated by the higher transparency of the formed fibers at pH 9 (Figure 2d). 209 Considering these findings, the yield of structures capable of preserving their tubular features 210 after washing and overnight incubation was calculated for fibers obtained using phases at 211 different pH values (Figure 2e). As expected, a generalized decrease in stability with increasing 212 pH of phase II, where EPL was dissolved, was observed. When the EPL-containing phase was 213 kept at pH 5, the interfacial membrane formed more quickly yielding highly stable structures. 214 However, even with the EPL-containing phase at pH 5, an increase in phase I (alginate-215 containing phase) to 9 led to the formation of less stable membranes. In fact, the assembly of 216 PEs in an ATPS depends not only on the electrostatic interaction between the PE's charged 217 groups, but it is also critically influenced by the affinity and partitioning-induced distribution of the PEs in the distinct polymer phases.^[39] Based on the theory purposed by Ma *et al.* which 218 219 states that an increase in pH may enhance hydrogen bonds between polyelectrolytes and the hydroxyl groups of dextran^[39], we hypothesize that higher pH values in our solutions could 220 221 have increased the affinity of alginate towards the dissolving phase. Consequently, its 222 availability at the interface would be decreased, culminating in the reduced stability of the 223 produced fibers. In summary, it was possible to control the formation and stability of the fiber-224 shaped structures, mostly by charge- and time-dependent mechanisms (Figure 2f), and possibly 225 by ATPS-PEs, by tuning the pH of the system.

226 Moreover, the stability of washed fibers, produced in 2 minutes of complexation, when 227 immersed in solutions at different pH, was evaluated (Figure S3, Supporting Information). Low 228 pH values, including 1 and 4, induced the stiffening of the fibers, while alkaline pH values in 229 the range of 10 and 13 led to the loss of integrity of the fibers. A very speedy effect observed 230 for pH 13, with the complete disintegration of the fibers within a few seconds. The structural 231 loss of the fibers at pH 13 may be ascribed to the loss of charge from amines in EPL, as well as 232 possible acquisition of negative charge (owing to carboxyl groups), culminating in increased 233 repulsion between EPL and ALG.

An overall analysis of processing conditions allowed stablishing ALG and EPL concentrations of 2 wt% and 0.75 wt%, with 2 min of complexation and pH~7, as the most robust condition for further functional characterization. The processing conditions comprising close-to-physiological pH, the use of an isotonic solution to dissolve the polymers, as well as the short time of complexation, also made these structures appealing as devices for the mild

encapsulation processes. Therefore, the selected condition was explored on its permeability andadequacy to withstand cell culture.

241 The possibility to develop compartmentalized tubular systems with adequate permeability 242 is crucial to ensure long-term survival of encapsulated biological compounds, and to possibly 243 improve the system's ability to serve as a permselective releasing and uptaking container. The 244 permeability of fibers was assessed using FITC-dextran molecules with different molecular 245 weights (40 and 150 kDa), as well as FITC-albumin (~67 kDa) as a representative protein model. 246 The fluorescent molecules were dissolved in the inner phase (DEX+ALG), and fibers were 247 produced and washed. Fluorescence intensity inside the material was monitored for a 24h period. 248 All molecules could diffuse through the membrane over time, with a high decrease of 249 fluorescence intensity after 60 min (Figure 2g). This release profile suggests that most 250 molecular content was probably released through a burst release, indicating their free diffusion 251 through the membrane. Negligible fluorescence was observed after 60 min for albumin and 252 small sized dextran molecules (Figure S4a, Supporting Information), indicating the 253 permeability of the membrane material to small molecules and proteins, suggesting its 254 effectiveness in exchanging nutrients, oxygen and metabolites essential for cell function and 255 survival. In opposition, fibers prepared in the absence of the ATPS precursor (PEs dissolved in PBS) showed low permeability to molecules as small as 10 kDa for four hours (Figure S4b, 256 257 Supporting Information), indicating that a further release may have been set by an increase on 258 membranes' permeability by, for example, swelling mechanisms or occurrence of localized 259 defects due to osmotic pressure.

260 To demonstrate the versatility of the developed system, the ability of the developed tubes 261 to be perfused with aqueous solutions was examined by injecting a blue dye solution using a 262 syringe. Perfusing liquids directly through bioengineered constructs is considered a key requirement for the generation of functional tubular tissues.^[12] The entire length of the materials 263 could be perfused with flows ranging from $2 \mu l \min^{-1}$ to $2 m l \min^{-1}$ - in ranges frequently used 264 in microfluidics for biomaterials processing, cell mechanical stimulation, and cell sorting 265 applications^[40,41]; Video S3) -, and continuously up to 1 hour (Video S4), while keeping their 266 267 structural integrity (Figure 2h). Moreover, the absence of a pre-formed solid template enabled 268 the easy development of free-form configurations using an extrusion 3D bioprinter (Figure 2i; 269 Video S5, Supporting Information). The deposition of phase I into phase II was achieved in 270 multiple directions, giving this method the potential to be used in the fabrication of fit-to-shape 271 materials to fill pre-determined shapes, such as tissue defects.^[5] Bioprinting of such tubule

fibers offers easy control not only over the geometry and distribution, but also the length,enabling the generation of structures with virtually unlimited length (Figure 2i).

274 Regardless of the concentrations of PE used for the formation of fibers, the fabrication of 275 non-leaky structures at the interface of the non-equilibrated ATPS was dependent on the control 276 over PE complexation time, with best yields obtained for 2 minutes. We hypothesized that the 277 formation of leaky regions at the coacervated membranes could be ascribed to increasing 278 tensions formed at tendentially breaking points of the filament, which occurred at times lower 279 than 1 minute for PE-free solutions. The use of equilibrated ATPS (Figure 3a) was 280 hypothesized to render more stable interfaces. Additionally, the variation of different 281 equilibrium points – corresponding to different tie lines in the phase separation diagram of the ATPS (Figure 3b) - enables selecting working points with varying interfacial tensions.^[42] 282 Considering such versatility, the effect of using ATPS points corresponding to tie lines (TL) 283 284 with increasing distance to the binodal curve was assessed. Since the PEG/dextran system has been well characterized in the literature, data reported by Liu et al.^[42] were used to 285 286 approximately characterize the binodal curve, and further select tie lines. Filaments of dextran 287 or dextran-rich (equilibrated) phases were dispensed in PEG or PEG-rich (equilibrated) baths 288 using a 3D bioprinter (Table S1, Supporting Information). The time after initiating extrusion (i.e., with the system at rest after full filament deposition) until the first breakage was registered. 289 290 Conditions prepared in equilibrated phases showed the first breakage at later times when compared to the non-equilibrated phases. The tendency for breakage was attenuated and 291 292 delayed for TLs associated with lower interfacial tension (i.e., time for breakage of TL1 > TL2 293 > TL3), with values for TL1 c.a. 5 minutes until the first breakage.

294 To further characterize the overall system, we calculated the partition coefficients for 295 the three different ATPS compositions (Figure 3c). Overall, ALG showed a stronger affinity 296 for the dextran-rich phases, while EPL also partitioned preferentially towards the same phase, 297 with affinity for dextran in the following order: TL3 > TL2 > TL1. Since the flow of ALG 298 towards the PEG-rich phases seems to be close to neglectable, the migration of EPL from the 299 PEG phase towards dextran is probably one of the most important factors contributing to the 300 formation of the interface-complexed fibers. This fact may also explain the observed growth of 301 the fibers' walls inwards, which is corroborated by the maintenance of their outer diameter 302 overtime (Figure S5a, Supporting Information), as well as the gradual increase of the thickness 303 of the membrane wall, until full closure of the lumen observed at 60 minutes (Figure S5b, 304 Supporting Information).

305 The production yield of continuous and non-leaky fibers obtained using 2 and 15 306 minutes of complexation was assessed. While for non-equilibrated phases, the achievement of 307 high yields of non-leaky fibers depended on the restriction of the complexation time to 2 308 minutes, the use of equilibrated phases led to a significant improvement of the yield of 309 continuous fibers obtained with 15 minutes complexation (Figure 3d). Moreover, this trend is 310 in agreement with the use of systems closer to the binodal curve (i.e., TL1 and TL2). The 311 thickness of fibers obtained in different TLs was also assessed and compared with samples 312 fabricated in the non-equilibrium system, with different partition coefficients resulting in 313 neglectable changes in the membranes' thickness, both for 2 and 15 minutes complexation 314 (Figure 3e). Overall, the use of equilibrated ATPS improved the production of continuous non-315 leaky fibers, showcasing thicknesses similar to fibers prepared in non-equilibrated phases, and 316 with increasing production yields for tie lines associated with lower interfacial tensions.

317 The potential of using the developed tubes as substrates for cell culture was assessed by 318 resuspending mesenchymal stem cells derived from human adipose tissue (hASCs) in phase I 319 (ATPS precursor), and producing the fiber-shaped materials using a syringe-needle manual 320 method under sterile conditions. Mesenchymal stem cells have been considered promising 321 therapeutic cells for the regeneration of damaged tissues. This potential is mainly associated to 322 their differentiation potential into many specific cell types, as well as to paracrine effects 323 characterized by the release of a variety of trophic factors that have been related to their capacity 324 to modulate the immune system, promote cell survival and proliferation, and enhance angiogenesis.^[43] Although we previously reported the encapsulation of mesenchymal stem cells 325 326 derived from the umbilical cord with low cytotoxicity in EPL/alginate spherical millimetric and 327 micrometric capsules^[44], we here relied on a higher concentration of the positively charged EPL 328 and continuous ejection forces to prepare membrane-bounded fibers. Despite its positive charge, 329 associated with its antimicrobial potential and often correlated with a cytotoxic potential for 330 several molecules, EPL is considered to have a relatively low toxicity against mammalian 331 cells.^[45] A preliminary cytotoxicity assessment for different complexation times showed that 332 times of complexation up to 5 min were compatible with high cell viability (Figure S6, 333 Supporting Information). To potentiate cell adhesion, alginate functionalized with the RGD 334 sequence was used for the assembly of the fibers. This peptide sequence is present in several 335 extracellular matrix proteins, and is responsible for mediating cell adhesion through integrinbinding.^[46] The purpose of including alginate-RGD was to further promote cell adhesion 336 337 throughout the structure at the membrane-level while maintaining the processing requirements 338 for the generation of the material, enabling ALG complexation with EPL molecules. By using

this strategy, we avoided the need for incorporation of external microparticles in the system a commonly used approach to provide cell anchorage support in cell-laden liquid-core
membrane bounded materials -, or the formation of multicellular aggregates.^[44,47]

- 342 The ability of encapsulating adherent cells in the developed biomaterial fibers was 343 assessed using hASCs (Figure 4a). The viability of encapsulated cells was monitored by 344 fluorescence microscopy using live/dead staining, and cellular metabolic activity was assessed 345 for 14 days of cell culture (Figure 4b,c). hASCs adhered and showcased a spread morphology 346 in fibers' walls on day 7, and a similar behavior was observed for 14 days of culture, with the 347 formation of an increasing number of interconnected networks with neighboring cells (Figure 348 4b). Although a statistical decrease in cell metabolic activity was observed after 4 days of 349 culture, cellular activity recovered after 14 days (Figure 3c), indicating the cytocompatibility 350 of the method. The location of cells upon the formation of the coacervate fibers was assessed 351 by imaging techniques. SEM images, as well as optical and fluorescence micrographs, showed 352 that a fraction of cells was incorporated in the polymeric membrane (Figure S7, Supporting 353 Information). In general, cells seemed to be present only in one side of the membrane (the inside 354 part), which did not affect the ability of continuous and stable fibers to be formed. Additionally, 355 the importance of the aqueous separating system as a key element in the formation of intact 356 devices for cell encapsulation procedures was also assessed. While maintaining the same 357 processing conditions, but in the absence of the ATPS precursors, collapsed structures with 358 non-uniform thickness and tendency to undergo localized rupture were obtained. Nonetheless, 359 cell viability was not negatively affected in this setup, although it seems to have driven cell 360 aggregation (Figure S8, Supporting Information). This result reinforces the importance of 361 building structures at the interface of ATPS to achieve high homogeneity and easy of handling.
- 362 363

3. Conclusion

364 In summary, a straightforward method was established to directly fabricate fiber-shaped 365 materials stable in all-aqueous physiological-relevant conditions, through the interfacial 366 complexation of oppositely charged natural polyelectrolytes. Size-versatile fibers and tubes 367 could be obtained from highly accessible, affordable and off-the-shelf materials, avoiding the 368 use of specifically designed materials.^[32,48,49] Our system enables the single-step generation of 369 robust, free- and self-standing flexible materials with arbitrary spatial organization, and features 370 of tubular structures after trimming, enabling the perfusion of liquid fluids. The diameter of the 371 structures could vary from millimeter to micrometer sizes depending on the size of the needle 372 used to extrude the dispersive phase, and mechanical and swelling properties could be easily

373 tuned by adjusting time of complexation. Optimized polyelectrolyte concentrations, 374 complexation time, pH, and equilibrium status in completely aqueous conditions led to the 375 production of devices with adequate permeability, and with potential to encapsulate delicate 376 cargos and maintain their bioactivity. Mesenchymal stem cells could be easily encapsulated 377 within fiber walls comprising cell adhesive peptide domains, where they adhered and spread 378 for 14 days, indicating that functional features of the developed material can also be controlled. 379 For the first time, non-spherical materials assembled at the interface of non-equilibrated 380 aqueous phases and ATPS at different equilibrium points are fabricated as self-standing entities,

381 with the ability to be used and handled outside the equilibrated two-phase system. The tube-

382 shape and cytocompatible features of the reported materials enable to foresee potential

383 applications in the biomedical field, enabling its integration into three-dimensional matrices, as

384 well as to be connected to perfusion sources, integrating *in vitro* multichannel fluidics devices.



385

Figure 1. Characteristics of tubule fibers produced in all-aqueous environments. (a) Schematic 386 387 representation of fiber formation using polyelectrolyte complexation between alginate and ε -388 poly-L-lysine (EPL) at the interface of an aqueous two-phase system composed of PEG and 389 dextran. (b) Microscopic images showing the darkening of the membrane over time, compared 390 to the control consisting of dextran phase immersed in PEG phase without the polyelectrolytes. 391 Scale bar: 500 µm. (c) Mean gray value over time of fibers produced in the presence and absence 392 of the ATPS precursor (n = 3 replicate fibers). (d) SEM micrographs of cross-sectioned fibers 393 with different complexation times demonstrating hollow features after dehydration. Arrows

- indicate upper and lower layers of collapsed structures with 2 and 5 min of complexation. (e)
- 395 Free-standing fiber material remained intact after 3x washing with PBS. (f,g) The structure was
- able to be handled with tweezers both in PBS (f) and in air (g).
- 397





Figure 2. Stability optimization, pH dependency, and system permeability and versatility. Representative images retrieved in a microscope (a) and stereomicroscope (b) of fiber leaking spots after washing steps with PBS. Concentrations of 0.75 wt% and 2 wt% for EPL and ALG, respectively, and 10 min of complexation are shown. (c) Yield calculation of fibers' stability based on their ability to remain intact without leakage after 3x PBS washing, and an overnight incubation period at 37°C (n = 10 replicate fibers). (d) Mean gray value determined for microscopic images of different fibers produced in a system with a global pH of 5, 7 and 9

406 (means that both phase I and II were adjusted to the related pH) (n = 5 replicate fibers). (e) 407 Analysis of the yield-related stability and structural integrity of fibers formed in systems with 408 varying phase I and II pH values (n=10 fibers per condition). (f) Graphical scheme representing 409 the increase of complexation time and pH leads to the formation of more unstable fibers related 410 to non-continuities derived from membrane rupture and opening. (g) Normalized fluorescence 411 intensity over time inside the fibers, which were produced in 2 min of complexation and further 412 washed and transferred to a PBS bath solution (n = 20 replicate fibers, excluding leaky fibers). 413 Data indicated as mean \pm standard deviation. (h) Time-lapse images from a video, showing the 414 perfusion of a blue dyed liquid solution throughout the structure. (i) Free-form deformability and ability to generate long length fibers with different shapes using an extrusion-based 3D 415 416 bioprinter. The structures could remain intact after washing with PBS. After printing the fibers 417 are blue due to the addition of a blue dye to visualize the printing procedure.



419

Figure 3. Study of the effect of ATPS equilibrium on the fabrication of coacervate fibers. (a) 420 421 Schematic representation of the phase separation obtained after mixing PEG and dextran at 422 different mixing points, obtained from (b) tie lines selected from a phase diagram of the ATPS. (c) Partition coefficients calculated for three different tie lines of the system. (d) Yield of 423 424 fabrication of continuous non-leaky fibers obtained after washing for non-equilibrated 425 precursory ATPS condition (NE), and for the three different equilibrium points (TL1, TL2, and

426 TL3) (n>24 fibers). (e) Thickness measured for fibers prepared on NE or different ATPS
427 equilibria (n=6).

428





430 Figure 4. Encapsulation of human adipose-derived stem cells. (a) Schematic representation of 431 the cell encapsulation procedure where hASCs are mixed in phase I also containing alginate 432 functionalized with the RGD domain. Fibers are produced and washed with DPBS after 2 min 433 of complexation, placed on well-plates with appropriate cell culture medium. Cells start to adhere through the fiber material after several days of culture. (b) Live/Dead micrographs of 434 435 fibers with hASCs after 1, 4, 7 and 14 days of culture. Green: calcein-AM (live), red: PI (dead). 436 (c) Cell metabolic activity measured by the fluorescence intensity using AlamarBlue assay. 437 Samples with size of approximately 0.5 cm long were used (n = 2 independent experiments; 4 replicate fibers/experiment). The values of fluorescence in cell-laden fibers (Fl measured) were 438

439 normalized with the fluorescence of non-cell fibers (Fl control). *** and ** indicates statistical 440 significance with p < 0.0001 and p < 0.01, respectively.

- 441
- 442

443 Experimental Section

444

445 *Materials:* Poly(ethylene glycol) (average MW 8000 Da), dextran (from Leuconostoc spp., 446 MW 450,000 – 650,000 Da), sodium alginate from brown algae (MW 120,000-190,000 g moL⁻ 447 ¹), and phosphate buffered saline (PBS) pellets were purchased from Sigma-Aldrich. ε -Poly-L-448 lysine (Epolyly®, MW ~ 4700 g mol⁻¹) derived from fermentation of Streptomyces albulus PD-449 1 was purchased from Handary S.A. (Brussels, Belgium). For cell assays, was used sodium 450 alginate NOVATACHTM MVG GRGDSP (GRGDSP-coupled high MW alginate) which was 451 purchased from NovaMatrix (Sandvika, Norway).

452

453 Formation of fibers using ATPS: For experiments using the non-equilibrated ATPS precursor, 454 solutions of 17 wt% poly(ethylene glycol) (PEG) and 15 wt% dextran (DEX) were prepared in PBS.^[44] Sodium alginate (ALG) and ε-poly-L-lysine (EPL) were dissolved separately in the 455 456 DEX 15 wt% and PEG 17 wt% solutions, respectively. In equilibrium conditions, mixtures of 457 dextran and PEG were prepared accordingly to mixture points of the tie lines selected from Liu 458 et al.^[42] by dissolving the polymers in PBS. The solutions were left sitting and further 459 centrifugation at 5000 rpm for 15 min to obtain a well separated two-phase system. ALG was dissolved in the DEX-rich inner phase to be extruded, and EPL in the PEG-rich outer/bath phase. 460 461 Considering that phase volume ratios vary along the same tie line^[50], the polymer mixture in each TL was chosen considering the preparation of fibers where a much higher quantity of bath 462 463 phase (PEG-rich) is needed compared to an extruded filament of inner (DEX-rich) phase. The 464 following initial compositions were used: PEG 7.5 wt% + DEX 3 wt%; PEG 12 wt% + DEX 3 465 wt%; and PEG 15 wt% + DEX 3 wt% for TL1, TL2 and TL3, respectively.

Fibers could be prepared using a simple manual injection method, where a solution composed of dextran and alginate (phase I) is dispersed through a syringe in a bath solution composed of PEG and EPL (phase II), by moving the syringe in thread-like configurations. To improve the control over the injection flow rate and shape of the structures, a syringe pump (Harvard Apparatus) with assembled syringes with 25 gauge needle was used. A microfluidic fluorinated ethylene-propylene tubing with 0.5 mm of inner diameter (Dolomite) was placed in front of the needles so that the phase was extruded perpendicular to the petri dish containing the bath

solution, using a flow rate of 0.2 mL min⁻¹. The ends of the fibers could be further removed still 473 474 within the complexation bath by cutting with a spatula, in order to remove irregularities derived 475 from the processing method and produce straight structures with a specific length if required. 476 Since polyelectrolytes were still able to interact inside the complexation bath, the ends 477 spontaneously closed after cutting. After formation, fibers were kept in agitation in an orbital 478 shaker at 30 rpm during a pre-determined complexation time, to prevent the structures from 479 sinking to the bottom of the petri dish due to higher density of phase I compared to the 480 continuous phase II, allowing PE complexation to occur uniformly throughout the entire 481 segment. To test the ability of fibers to be perfused, complexation was interrupted at pre-482 determined times by removing the bath phase and then washing the fibers with PBS (Sigma-483 Aldrich). Afterwards, the closed ends were removed using a spatula to leave the fibers with 484 open ends and allow the liquid-core solution to enter/exit. A diluted blue dye solution was 485 injected through one end using a syringe and a small 34 gauge needle.

486

487 Scanning electron microscopy: Scanning electron microscopy (SEM) analysis was performed 488 to analyze the morphology and the presence of a hollow lumen in the formed structures. Fibers 489 were produced using the syringe pump method with different complexation times, and were 490 dehydrated with ethanol solutions following a concentration gradient of: 30% (v/v), 50% (v/v), 491 70% (v/v), 80% (v/v), 90% (v/v), 96% (v/v) and 100% (v/v), by immersing them in these 492 solutions for 15 minutes. To visualize the lumen, transversal cross sections were made using a 493 scalpel blade prior to dehydration. In order to make them conductive, samples underwent gold 494 sputtering for 3 minutes. Samples were then imaged using an Ultra-high Resolution Analytical 495 Scanning Electron Microscope HR-FESEM Hitachi SU-70 (Hitachi, Tokyo, Japan).

496

497 Stability optimization: To analyze the stability of the fibers according to the concentration of 498 PE, complexation time and system's pH, the ability of the fibers to resist specific conditions 499 after processing was assessed. Different ALG concentrations (1.5 wt%, 2 wt% and 2.5 wt%) 500 and EPL concentrations (0.5 wt%, 0.75% and 1 wt%) were tested as well as different 501 complexation times, namely 2, 5, 10 or 15 min. The continuous phase was immediately 502 removed after complexation, and PBS was added. This washing step was repeated two 503 additional times until complete removal of the continuous phase. With this procedure, a yield 504 was determined for the fibers that could remain stable without opening or collapsing after the 505 washing steps plus an overnight incubation period at 37°C (Equation 1). Two independent 506 experiments were performed with a total representative number of 10 fibers used for each

507 condition, using fibers with approximately 1.5 cm long. The formation and structural 508 integrity/stability of the PE fibers were also analyzed for different system pH, namely, 5, 7 and 509 9, and imagens of the fibers were acquired in a microscope (Primostar, Zeiss), all in the same 510 light conditions. To assess the darkening of the membranes, associated with higher extents of 511 complexation, the mean gray value was determined using ImageJ.

512

$$Yield (\%) = \frac{Number of stable fibers after 37^{\circ}C overnigth incubation}{Total of produced fibers} \times 100$$
(1)

514

Membrane thickness: Tubular fibers were prepared as described using the syringe pump method
and washed after pre-established complexation times. Fiber ends were removed using a spatula.
The samples were tilted using tweezers, and observed using optical microscopy (Primostar,
Zeiss). Membrane thickness while hydrated was measured using ImageJ.

519

520 Permeability characterization: Fluorescein isothiocyanate-dextran (Dextran-FITC, Sigma-521 Aldrich) with different average molecular weights - 40 and 150 kDa - and albumin-fluorescein 522 isothiocyanate conjugate (albumin-FITC, ~66 kDa), were mixed in phase I (1 mg mL⁻¹). Fibers 523 were prepared using the previously described syringe manual method with 25G needles to 524 mimic the further described cell encapsulation scenario. To determine the release profile of the 525 fluorescently labeled molecules that might diffuse through the fiber membrane, the bath 526 solution was removed after 2 min of complexation, and 10 mL of PBS was added, following 527 PBS washes (30 mL) (x2). 5 fibers with 0.5 cm long were made, in quadruplicates, for each 528 fluorescent molecule. Images were acquired at 0 min (immediately after the first washing step), 529 10 min, 30 min, 60 min, 120 min and 24 hours in a fluorescence microscope (Axio Imager M2, 530 Carl Zeiss, Germany). Fibers that opened during the process were not considered. The 531 fluorescence intensity was quantified using ImageJ software. For each fiber, the fluorescence 532 intensity was normalized with the fluorescence intensity after the first wash (since it was 533 hypothesized to trigger the higher release of molecules).

534

Free-form 3D printing: To explore the versatility of the system to produce free-form and long structures, an extrusion 3D bioprinter (Inkredible+, Cellink) was used. A colored food dye was added into aqueous solution of phase I to make the printing procedure visible. The different shapes were fabricated using computer aided design models created in SolidWorks 2020, sliced and converted into a print file using Cellink HeartWare Software which was also used to control the bioprinter. A 22G nozzle was used to extrude the dyed solution under 80 kPa pressure at a

541 speed of 10-15 mm s⁻¹. The structures were produced after immersing the printing nozzle in a 542 petri dish containing the aqueous solution of PEG and EPL (10 mL).

543

544 Determination of the partitioning coefficients of polyelectrolytes. The partitioning coefficient is defined as the ratio between the concentration of a compound in the two immiscible phases 545 546 at equilibrium.^[51,52] Based on previously reported methodologies^[28,39], to determine the 547 partition coefficients of ALG and EPL in the different studied ATPS compositions, 548 spectrophotometric methods were used. For EPL, different known concentrations were 549 prepared from a stock solution of EPL 1 wt% in PBS, and the absorbance at 230 nm (where EPL shows a distinctive absorbance signal^[53]) was measured using a microplate 550 spectrophotometer to obtain a calibration curve. For the experimental systems, a known 551 552 concentration of EPL in PBS was added to a mixture of PEG and dextran and, after dissolution 553 of the system, the mixture was left sitting overnight, and then centrifugated at 5000 rpm during 554 15 min to obtain a fully separated system. A separated system prepared with the same polymer 555 composition without the presence of polyelectrolyte was used as blank for samples. The 556 concentration of EPL in both polymer-rich phases was determined using the previously 557 obtained calibration curve, and the partitioning coefficient was calculated as follows (Equation 558 2):

559

$$K = \frac{[PE]_{top}}{[PE]_{bottom}} \tag{2}$$

560 Where $[PE]_{top}$ and $[PE]_{bottom}$ is the concentration of the polyelectrolyte in the top and bottom 561 phase, respectively.

562 A similar procedure was applied to determine the partitioning coefficient of ALG. A method 563 based on the complexation of ALG with a cationic blue dye (1,9-dimethyl methylene blue (DMMB, Sigma-Aldrich) (adapted from^[54,55]) was applied. Briefly, solutions for the calibration 564 565 curve and experimental phase-separated systems (samples and blank) were incubated with a 1 566 mM DMMB solution (in water) (1:25) for 45 min. The absorbance was measured at 520 and 567 650 nm to determine the 520/650 nm absorbance ratio. ALG concentrations were determined, 568 and the partition coefficient calculated using equation 2. The initial compositions of PEG and 569 dextran for the separation in PEG-rich and dextran-rich phases in conditions TL1, TL2 and TL3 were chosen from the phase diagram previously reported by Liu et al.^[42], considering an equal 570 phase volume ratio (at the center of the TL). The following compositions were used: PEG 5.1 571 572 wt% + DEX 8 wt%: PEG 7 wt% + DEX 12 wt%; and PEG 8.6 wt% + DEX 15 wt% for the 573 samples TL1, TL2 and TL3, respectively.

574

575 *Cell culture and encapsulation:* The cytocompatibility of PE fibers was evaluated using human 576 adipose-derived mesenchymal stem cells (hASCs) (purchased from LGC Standards, ATCC) 577 and were cultured in α -MEM, supplemented with 10% (v/v) fetal bovine serum (FBS, 578 ThermoScientific) and 1% antibiotic/antimycotic (ThermoScientific). Cells were used in 579 passages between 6 to 8. Cell suspensions were prepared after trypsinization and were 580 encapsulated in the phase to be dispersed containing the ALG 2 wt%. To promote cell adhesion, 581 alginate functionalized with the cell adhesion peptide arginine-glycine-aspartate (ALG-RGD) 582 was used at a concentration of 0.5 wt%. Both solutions containing the phase-forming polymers and PEs were sterilized. For that, ATPS phases containing the dissolved polymers were filtered 583 584 using sterile 0.2 µm pore-sized filters, alginate and EPL reagents were exposed to UV light during 40 min and ALG-RGD during 20 min. The sterile polyelectrolytes were added to the 585 586 filtered solutions to dissolution using autoclaved stirring magnets. A syringe containing the phase with cells $(10 \times 10^6 \text{ cells/mL})$ was manually injected in the phase containing PEG and 587 588 EPL to facilitate the processing method. After 2 min of complexation, DPBS was added (x3), 589 and fibers were transferred to a DPBS solution (30 mL) and then to the appropriate cell culture 590 medium. Cell encapsulated fibers were maintained in incubators with controlled temperature 591 (37°C) and 5% CO2. For the comparison of structures being formed with and without the 592 presence of the ATPS, the fibers were produced as previously described in sterile conditions, and the same cell density of 10×10^6 cells/mL was used in both conditions, but in this case, 593 594 MC3T3 cell lineage cultured also in α -MEM medium with the appropriate supplementation, 595 was used.

596

597 *Cell viability assays:* The cell viability of cell-laden fibers was analyzed by live/dead assay 598 (Invitrogen, USA) and Alamar Blue® Cell Viability assay at different time points. Both assays 599 were performed in accordance with manufacturer instructions. To analyze live and dead cells 600 at pre-determined timepoints, fibers were incubated in cell culture medium with propidium 601 iodide (PI) (Thermo Fisher Scientific) and Calcein-AM solution (Thermo Fisher Scientific) at concentration of 1 µL mL⁻¹ and 2 µL mL⁻¹, respectively, during 10 min at 37°C. Fibers were 602 603 washed with culture medium and examined in an upright widefield fluorescence microscope 604 (Axio Imager M2, Carl Zeiss, Germany). The AlamarBlue® assay (Thermo Fisher Scientific) 605 was used to access metabolic activity of encapsulated cells. Cell encapsulated fibers with approximately 0.5 cm long were placed in a 48 well-plate with 1.2 cm of diameter per well. 606 AlamarBlueTM reagent was added to the cell culture medium (1:10), with an incubation period 607

of 8.5 hours. Fluorescent measurements (λ excitation: 540 nm, λ emission: 600 nm) were performed in a Synergy HTX microplate reader using a 96-well black-clear bottom plate. A representative number of four fibers per independent experience were used for each assay at the different timepoints.

For cell nuclei identification in the membranes, cell-laden fibers were fixed with cold methanol for 10 min at -20°C. Afterwards, the structures were washed with PBS and ruptured with up and down movements using a micropipette. Fiber fragments were incubated with 4',6-Diamidine-2'-phenylindole dihydrochloride (DAPI, ThermoScientific, 1 μ g/mL) at room temperature, and cell nuclei visualized in a fluorescence microscope.

617

618 *Statistical analysis:* GraphPad Prism 8 was applied for data statistical analysis, and results are 619 presented as mean \pm standard deviation. Statistical significance between the groups was 620 determined by multiple t tests using one-way and two-way analysis of variance (ANOVA), 621 considering a statistically significant difference if p < 0.05.

622

623 Supporting Information

- 624 Supporting Information is available from the Wiley Online Library or from the author.
- 625

626 Acknowledgements

627 This work was financially supported by the European Research Council grant agreement ERC-628 2014-ADG-669858 (project ATLAS), by the Programa Operacional Competitividade e 629 Internacionalização, in the component FEDER, and by national funds (OE) through 630 FCT/MCTES, in the scope of the projects 'TranSphera' (PTDC/BTM-ORG/30770/2017) and "CellFi" (PTDC/BTM-ORG/3215/2020). This work was developed within the scope of the 631 632 project CICECO-Aveiro Institute of Materials, UIDB/50011/2020, UIDP/50011/2020 & 633 LA/P/0006/2020, financed by national funds through the FCT/MEC (PIDDAC). M. B. Oliveira 634 acknowledges the individual contract CEECIND/03605/2017. FCT also financially supported 635 this work through individual doctoral grant 2021.07435.BD of Raquel C. Gonçalves.

636

637 **Conflict of interest**

638 The authors declare no conflict of interest.

639

640 Data Availability Statement

641 The raw data required to reproduce these findings are available from the authors upon request.

642		
643		Received: ((will be filled in by the editorial staff))
644		Revised: ((will be filled in by the editorial staff))
645		Published online: ((will be filled in by the editorial staff))
646		
647	Refe	rences
648	[1]	Z. J. Meng, W. Wang, R. Xie, X. J. Ju, Z. Liu, L. Y. Chu, Lab on a Chip 2016, 16, 2673.
649	[2]	C. R. Correia, R. L. Reis, J. F. Mano, Advanced Healthcare Materials 2018, 7, 1701444.
650	[3]	C. R. Correia, S. Nadine, J. F. Mano, Advanced Functional Materials 2020, 30, 1908061.
651 652	[4]	G. Luo, Y. Yu, Y. Yuan, X. Chen, Z. Liu, T. Kong, Advanced Materials 2019, 31, 1904631
653 654	[5]	A. R. Sousa, C. Martins-Cruz, M. B. Oliveira, J. F. Mano, <i>Advanced Materials</i> 2020 , <i>32</i> , DOI 10.1002/adma.201906305.
655	[6]	K. A. DiVito, M. A. Daniele, S. A. Roberts, F. S. Ligler, A. A. Adams, Biomaterials
656		2017 , <i>138</i> , 142.
657	[7]	H. Wang, H. Liu, X. Zhang, Y. Wang, M. Zhao, W. Chen, J. Qin, ACS Applied Materials
658		and Interfaces 2021 , 13, 3199.
659	[8]	Y. Zhu, L. Wang, F. Yin, Y. Yu, Y. Wang, H. Liu, H. Wang, N. Sun, H. Liu, J. Qin,
660		Integrative Biology 2017, 9, 774.
661	[9]	H. Savoji, L. Davenport Huyer, M. H. Mohammadi, B. F. Lun Lai, N. Rafatian, D.
662		Bannerman, M. Shoaib, E. R. Bobicki, A. Ramachandran, M. Radisic, ACS Biomaterials
663		<i>Science & Engineering</i> 2020 , <i>6</i> , 1333.
664	[10]	Q. Gao, Y. He, J. zhong Fu, A. Liu, L. Ma, <i>Biomaterials</i> 2015, 61, 203.
665	[11]	W. Jia, P. S. Gungor-Ozkerim, Y. S. Zhang, K. Yue, K. Zhu, W. Liu, Q. Pi, B. Byambaa,
666		M. R. Dokmeci, S. R. Shin, A. Khademhosseini, <i>Biomaterials</i> 2016, 106, 58.
667	[12]	Q. Pi, S. Maharjan, X. Yan, X. Liu, B. Singh, A. M. van Genderen, F. Robledo-Padilla,
668		R. Parra-Saldivar, N. Hu, W. Jia, C. Xu, J. Kang, S. Hassan, H. Cheng, X. Hou, A.
669		Khademhosseini, Y. S. Zhang, Advanced Materials 2018, 30, 1706913.
670	[13]	C. Li, X. Han, Z. Ma, T. Jie, J. Wang, L. Deng, W. Cui, Advanced Healthcare Materials
671		2021 , 2101836.
672	[14]	W. Feng, Y. Chai, J. Forth, P. D. Ashby, T. P. Russell, B. A. Helms, Nature
673		Communications 2019, 10, 1095.
674	[15]	S. Shi, T. P. Russell, Advanced Materials 2018, 30, 1800714.

- 675 [16] J. Forth, P. Y. Kim, G. Xie, X. Liu, B. A. Helms, T. P. Russell, *Advanced Materials* 2019,
 676 *31*, 1806370.
- 677 [17] Y. Chao, H. C. Shum, *Chemical Society Reviews* 2020, 49, 114.
- 678 [18] A. G. Teixeira, R. Agarwal, K. R. Ko, J. Grant-Burt, B. M. Leung, J. P. Frampton,
 679 *Advanced Healthcare Materials* 2018, 7, 1701036.
- [19] L. Zhang, L. H. Cai, P. S. Lienemann, T. Rossow, I. Polenz, Q. Vallmajo-Martin, M.
 Ehrbar, H. Na, D. J. Mooney, D. A. Weitz, *Angewandte Chemie International Edition*2016, 55, 13470.
- 683 [20] M. Kim, S. J. Yeo, C. B. Highley, J. A. Burdick, P. J. Yoo, J. Doh, D. Lee, ACS Nano
 684 2015, 9, 8269.
- 685 [21] S. D. Hann, T. H. R. Niepa, K. J. Stebe, D. Lee, *ACS Applied Materials and Interfaces*686 2016, 8, 25603.
- 687 [22] S. D. Hann, D. Lee, K. J. Stebe, *Physical Chemistry Chemical Physics* 2017, 19, 23825.
- [23] Y. Zou, J. Song, X. You, J. Yao, S. Xie, M. Jin, X. Wang, Z. Yan, G. Zhou, L. Shui, ACS *Applied Materials and Interfaces* 2019, *11*, 21227.
- 690 [24] H. Liu, Y. Wang, H. Wang, M. Zhao, T. Tao, X. Zhang, J. Qin, *Advanced Science* 2020,
 691 7, 1903739.
- 692 [25] G. Xie, J. Forth, Y. Chai, P. D. Ashby, B. A. Helms, T. P. Russell, *Chem* 2019, *5*, 2678.
- 693 [26] J. Fu, J. B. Schlenoff, J Am Chem Soc 2016, 138, 980.
- 694 [27] R. H. Tromp, R. Tuinier, M. Vis, *Physical Chemistry Chemical Physics* 2016, 18, 30931.
- 695 [28] Q. Ma, Y. Song, J. W. Kim, H. S. Choi, H. C. Shum, ACS Macro Letters 2016, 5, 666.
- 696 [29] A. B. Kayitmazer, Advances in Colloid and Interface Science 2017, 239, 169.
- 697 [30] T. R. Cox, J. T. Erler, Disease Models and Mechanisms 2011, 4, 165.
- 698 [31] S. Park, R. Barnes, Y. Lin, B. jin Jeon, S. Najafi, K. T. Delaney, G. H. Fredrickson, J. E.
 699 Shea, D. S. Hwang, S. Han, *Communications Chemistry* 2020, *3*, 83.
- 700 [32] K. E. Inostroza-Brito, E. Collin, O. Siton-Mendelson, K. H. Smith, A. Monge-Marcet,
- D. S. Ferreira, R. P. Rodríguez, M. Alonso, J. C. Rodríguez-Cabello, R. L. Reis, F.
 Sagués, L. Botto, R. Bitton, H. S. Azevedo, A. Mata, *Nature Chemistry* 2015, 7, 897.
- 703 [33] A. M. Díez-Pascual, P. S. Shuttleworth, *Materials* 2014, 7, 7472.
- 704 [34] A. M. Díez-Pascual, P. S. Shuttleworth, *Materials* 2014, 7, 7472.
- 705 [35] F. Loosli, L. Vitorazi, J. F. Berret, S. Stoll, *Water Research* 2015, 80, 139.
- 706 [36] M. G. Carneiro-Da-Cunha, M. A. Cerqueira, B. W. S. Souza, J. A. Teixeira, A. A.
 707 Vicente, *Carbohydrate Polymers* 2011, 85, 522.

- [37] S. C. Shukla, A. Singh, A. K. Pandey, A. Mishra, *Biochemical Engineering Journal* 2012,
 65, 70.
- 710 [38] T. Yoshida, T. Nagasawa, *Applied Microbiology and Biotechnology* **2003**, *62*, 21.
- 711 [39] Q. Ma, H. Yuan, Y. Song, Y. Chao, S. Y. Mak, H. C. Shum, *Soft Matter* **2018**, *14*, 1552.
- 712 [40] K. Raj M, S. Chakraborty, *Journal of Applied Polymer Science* **2020**, *137*, 48958.
- [41] C. L. Thompson, S. Fu, M. M. Knight, S. D. Thorpe, *Frontiers in Bioengineering and Biotechnology* 2020, 8, 602646.
- 715 [42] Y. Liu, R. Lipowsky, R. Dimova, *Langmuir* **2012**, *28*, 3831.
- [43] Y. Fu, L. Karbaat, L. Wu, J. Leijten, S. K. Both, M. Karperien, *Tissue Engineering Part B: Reviews* 2017, 23, 515.
- [44] S. Vilabril, S. Nadine, C. M. S. S. Neves, C. R. Correia, M. G. Freire, J. A. P. Coutinho,
 M. B. Oliveira, J. F. Mano, *Advanced Healthcare Materials* 2021, 2100266.
- [45] M. Hyldgaard, T. Mygind, B. S. Vad, M. Stenvang, D. E. Otzen, R. L. Meyer, *Applied and Environmental Microbiology* 2014, 80, 7758.
- 722 [46] S. L. Bellis, *Biomaterials* **2011**, *32*, 4205.
- [47] C. R. Correia, R. P. Pirraco, M. T. Cerqueira, A. P. Marques, R. L. Reis, J. F. Mano, *Scientific Reports* 2016, 6, 21883.
- Y. Wu, B. O. Okesola, J. Xu, I. Korotkin, A. Berardo, I. Corridori, F. L. P. di Brocchetti,
 J. Kanczler, J. Feng, W. Li, Y. Shi, V. Farafonov, Y. Wang, R. F. Thompson, M. M.
- Titirici, D. Nerukh, S. Karabasov, R. O. C. Oreffo, J. Carlos Rodriguez-Cabello, G.
 Vozzi, H. S. Azevedo, N. M. Pugno, W. Wang, A. Mata, *Nature Communications* 2020, *11*, 1182.
- Y. Wu, G. M. Fortunato, B. O. Okesola, F. L. P. Di Brocchetti, R. Suntornnond, J.
 Connelly, C. De Maria, J. C. Rodriguez-Cabello, G. Vozzi, W. Wang, A. Mata, *Biofabrication* 2021, *13*, 035027.
- 733 [50] J. F. B. Pereira, J. A. P. Coutinho, *Liquid-Phase Extraction* **2020**, 157.
- 734 [51] A. L. Grilo, M. R. Aires-Barros, A. M. Azevedo, *Separation and Purification Reviews*735 **2016**, *45*, 68.
- M. Iqbal, Y. Tao, S. Xie, Y. Zhu, D. Chen, X. Wang, L. Huang, D. Peng, A. Sattar, M.
 A. B. Shabbir, H. I. Hussain, S. Ahmed, Z. Yuan, *Biological Procedures Online* 2016, 18, 18.
- 739 [53] Y. Meng, Q. Xue, J. Chen, Y. Li, Z. Shao, Journal of Dairy Science 2022, 105, 3746.
- 740 [54] J. P. Halle, D. Landry, A. Fournier, M. Beaudry, F. A. Leblond, *Cell Transplantation*741 **1993**, *2*, 429.

742 [55] J. C. Richardson, P. W. Dettmar, F. C. Hampson, C. D. Melia, *European Journal of*743 *Pharmaceutics and Biopharmaceutics* 2004, *57*, 299.

744