

1       **The influence of zwitterions on the partition of biomolecules in**  
2                                   **aqueous biphasic systems**

3  
4       Anusha Basaiahgari,<sup>1</sup> Helena Passos,<sup>2</sup> João A. P. Coutinho,<sup>2\*</sup> Ramesh L. Gardas<sup>1\*</sup>

5  
6       <sup>1</sup>*Department of Chemistry, Indian Institute of Technology Madras, Chennai - 600 036, India;*

7       <sup>2</sup>*CICECO - Aveiro Institute of Materials, Department of Chemistry, University of Aveiro, 3810-*  
8                                   *193 Aveiro, Portugal.*

9 -----  
10  
11                                   \**Corresponding authors. E-mail address:*

12                                   *jcoutinho@ua.pt (J.A.P. Coutinho);*

13                                   *gardas@iitm.ac.in (R.L. Gardas)*

1 **Abstract**

2 The use of hydrophilic zwitterionic compounds (ZI) to act as phase forming components of  
3 aqueous biphasic systems (ABS) has been attracting increased interest. Although previous works  
4 studied the phase behavior of ZI, there is still a lack of knowledge on the partition behavior of  
5 compounds in ZI-based ABS. This work reports a study on the influence of ZI structure for the  
6 extraction of 7 different biomolecules selected as molecular probes – 2 alkaloids (nicotine and  
7 caffeine), 2 phenolic compounds (gallic acid and vanillic acid) and 3 amino acids (*L*-tryptophan,  
8 *L*-tyrosine and *L*-phenylalanine). The partition and extraction efficiencies of these biomolecules  
9 were evaluated in ternary systems composed of hydrophilic ZI constituted by ammonium,  
10 imidazolium, pyridinium and piperidinium cationic and SO<sub>3</sub><sup>-</sup> anionic groups, K<sub>2</sub>CO<sub>3</sub> and water.  
11 The obtained results show that all the biomolecules preferentially partition to the ZI-rich phase,  
12 and the extent of their partition was closely related with the octanol-water partition coefficients of  
13 both biomolecules and ZI. It was demonstrated that the partition of biomolecules in ZI-based ABS  
14 is firstly ruled by hydrophobic/hydrophilic effects and only in some particular cases specific  
15 interactions between the biomolecule and the ZI affect their partition. Furthermore, despite the  
16 similarity between ZI and ionic liquids behavior as phase forming compounds of ABS for the  
17 extraction of biomolecules, ZI-based ABS presented a better performance in the extraction of  
18 phenolic compounds in alkaline environment.

19

20

21 **Keywords:** Aqueous biphasic systems; zwitterionic compounds; alkaloids; phenolic compounds;  
22 amino acids; partition coefficient; hydrophobic/hydrophilic effects.

23

## 1 **1. Introduction**

2 The study and development of new aqueous biphasic systems (ABS) has triggered a renewed  
3 interest among the research community for the use of liquid-liquid extraction (LLE) techniques in  
4 the separation and purification of value-added compounds.[1] As a part of research for the  
5 extraction of value-added chemicals from biomass residues, in the framework of biorefinery  
6 processes, it is of importance to develop cost-effective extraction and separation systems.[2]  
7 Among multiple factors that contribute to the success of the extraction and purification  
8 technologies, the proper choice of solvents is of high relevance since they have impact on the rate  
9 of mass transfer, on the stability of the target compounds, and in the economic and environmental  
10 feasibility of the whole process.[3] Thus, there is a challenge in the formulation of sustainable  
11 systems with appropriate solvents.

12 ABS are constituted by water in major proportions. These systems are nowadays considered as  
13 suitable alternatives to the conventionally used LLE systems since they fulfill the green chemistry  
14 principles by avoiding the use of conventional volatile organic solvents thereby minimizing their  
15 environmental impact. Conventional ABS are composed of either two polymers, a polymer and a  
16 salt or two salts resulting in two aqueous-rich phases in equilibrium.[4] Despite the “greener”  
17 character of these systems induced by their aqueous nature, conventional polymer-based systems  
18 present some issues, namely restricted polarity, high viscosity and consequent low phase  
19 separation rates.[5]

20 Over the years, researchers have tried to develop novel ABS by using a variety of phase forming  
21 components that allow overcoming of drawbacks associated to the most conventional systems. In  
22 this context, ionic liquids (IL) were identified as a suitable alternative. Following the first work  
23 reported by Rogers and co-workers,[6] several studies on the use of IL as phase forming  
24 components of ABS have been published in past decades.[5] IL are defined as salts constituted by  
25 asymmetrical cations and anions that present low melting points. Along with interesting properties,  
26 such as high chemical and thermal stability, tunability of their chemical structures and negligible  
27 vapor pressure, IL exhibit a wide solubility for compounds of variable polarities. These unique  
28 properties enabled them to be efficient phase forming components of ABS when combined with  
29 salts, polymers, amino acids, carbohydrates, inorganic acids among others.[5,7–9] Furthermore,  
30 IL-based ABS have shown an amazing potential for application in the extraction and separation of

1 several varieties of compounds including amino acids, alkaloids, proteins, phenolic compounds,  
2 terpenoids, acids, metals etc .[5,10–14]

3 Hydrophilic zwitterionic compounds (ZI), were recently proposed as phase forming compounds  
4 of ABS.[15,16] They are similar in behavior to IL, but are not composed of separated ions, rather  
5 they are constituted by covalently bonded cations and anions.[17] This type of chemical structure  
6 confers particular characteristics to ZIs; for example, despite their electric neutrality, these  
7 molecules present very high polarity induced by the coexistence of both opposite charges. These  
8 compounds are also well-known by their self-association ability and strong hydration, which allied  
9 with their non-toxicity and biodegradability, allowed their application in several fields, namely  
10 cosmetics, personal care and detergent industries.[18,19] Furthermore, their properties can be  
11 tuned by changes in their structures (modification of the cationic and anionic groups, the size of  
12 the spacer, addition or size change of hydrocarbons chains, etc.) allowing a large number of  
13 possibilities.[19]

14 ZI use in the formation of ABS when mixed with salts and polymers conferred special properties  
15 to the systems that make them suitable alternatives for the development of novel extraction and  
16 separation processes. Ferreira et al.[16] showed that it is possible to tune the thermal behavior of  
17 ABS between upper critical solution temperature (UCST) and lower critical solution temperature  
18 (LCST) behavior by only changing the size of the alkyl chains that compose sulfobetaine-based  
19 ZI. These ABS allowed the separation of aromatic and aliphatic amino acids mixtures and opened  
20 the possibility to design more dynamic systems. The same authors[15] also demonstrated the  
21 potential application of ZI-polymer-based ABS as an integrated process in enzymatic catalysis,  
22 allowing both the recovery of the product and the reuse of the enzyme. Induced by these new  
23 findings, we synthesized novel hydrophilic ZI based on ammonium, imidazolium, piperidium and  
24 pyrrolidinium cations.[20] This previous work was focused on evaluating ZI phase behavior in  
25 combination with potassium-based salts and systems ability to partition caffeine, which was  
26 selected as a model alkaloid.[20] However, despite the increased interest in the application of ZI  
27 as phase forming compounds, the works reported up to now are not enough to provide broad  
28 knowledge on the influence of ZI nature on compounds partition in ZI-based ABS and how their  
29 ability is comparable to well-known IL-based ABS.

30 Aiming to explore the applicability of novel ZI-based ABS for the extraction and separation of a  
31 large range of compounds, it is here presented a study on the ability of ABS composed of

1 hydrophilic ZI, potassium carbonate salt ( $K_2CO_3$ ) and water to extract different types of  
2 biomolecules, namely 2 alkaloids (nicotine and caffeine), 2 phenolic compounds (gallic acid and  
3 vanillic acid) and three amino acids (*L*-tryptophan, *L*-tyrosine and *L*-phenylalanine). These  
4 compounds were selected as molecular probes, similarly to what was previously done in works  
5 about IL- and deep-eutectic-solvents-based ABS, since they serve as model compounds for a wide  
6 variety of value added compounds of interest present in biomass [21,22]. These biomolecules  
7 present different structures and polarities, which allow the evaluation of possible specific and non-  
8 specific interactions that may occur between biomolecules and phase-forming compounds.  
9

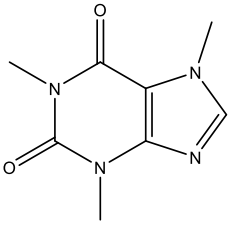
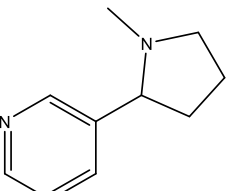
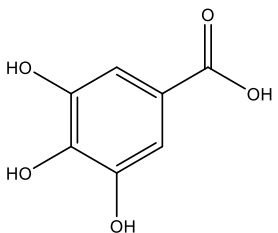
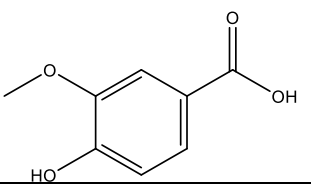
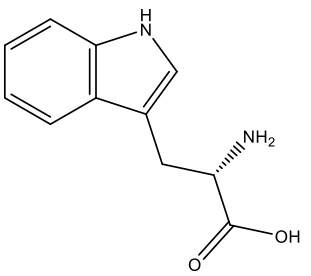
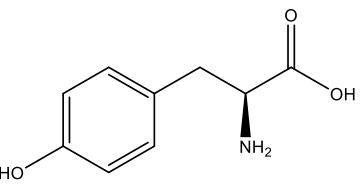
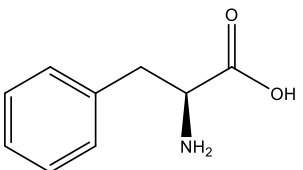
## 10 **2. Materials and methods**

### 11 *2.1. Materials*

12 The chemical structures and properties, including octanol-water partition coefficient ( $K_{OW}$ ) and  
13 water solubility, of the biomolecules here studied are reported in **Table 1**. In **Table 2** are listed the  
14 ZI studied in this work along with their acronyms, structures and properties. The synthesis  
15 procedure for these ZI was previously described by us.[20] The reagents used in the ZI preparation  
16 were triethylamine (99.5 wt % pure), *N*-methylimidazole (99 wt % pure), *N*-vinylimidazole (99 wt  
17 % pure), *N*-methyl pyrrolidine (98 wt % pure), *N*-ethylpiperidine (98 wt % pure) and 1,4-  
18 butanesultone (99 wt % pure) all supplied by Sigma-Aldrich. Acetonitrile (99.5 wt % pure) and  
19 diethylether (98 wt % pure) from Sigma-Aldrich were used during synthesis procedure.  $^1H$  and  
20  $^{13}C$  nuclear magnetic resonance (NMR) analysis was used to confirm ZI structure and purity. The  
21 water content of the ZI was determined by Karl Fischer titration, and these values were considered  
22 in the preparation of the ABS. The purity and water content determined for each ZI are presented  
23 in the **Table S1**.

24 Ternary systems studied in this work were prepared by mixing each ZI with dipotassium carbonate  
25 salt ( $K_2CO_3$  of 99 wt % purity) supplied by Merck. Caffeine (98 wt % pure) from SRL, nicotine  
26 (99 wt % pure) from Fluka, gallic acid (99.5 wt %) from Merck, vanillic acid (97 wt % pure) from  
27 Sigma-Aldrich, and *L*-tryptophan (99 wt % pure), *L*-tyrosine (99 wt % pure) and *L*-phenylalanine  
28 (99 wt % pure) all supplied by Spectrochem, were used as biomolecules (**Table 1**).

1 **Table 1.** Chemical structure and properties of the studied biomolecules.[23,24]

	Biomolecule	Structure	log ( <i>K</i> <sub>ow</sub> )	log ( <i>K</i> <sub>ow</sub> ) at pH 12	<i>S</i> <sub>water</sub> (g·L <sup>-1</sup> ) <sup>a</sup>
ALKALOIDS	Caffeine (Caf)		-0.55	-0.55	21.6
	Nicotine (Nic)		1.16	1.16	miscible
PHENOLIC COMPOUNDS	Gallic acid (GA)		0.72	-6.66	11.9
	Vanillic acid (VA)		1.17	-3.93	1.5
AMINO ACIDS	<i>L</i> -Tryptophan (Tryp)		-1.09	-2.35	13.4
	<i>L</i> -Tyrosine (Tyr)		-1.49	-4.33	0.48
	<i>L</i> -Phenylalanine (Phe)		-1.18	-2.45	25.9

1 <sup>a</sup> at 298.15 K.[24]

2

3 **Table 2.** Name, acronym, structure and octanol-water partition coefficient ( $K_{OW}$ ) of the ZI studied  
4 in this work.

Name	Acronym	Structure	log ( $K_{ow}$ ) [23]
4-(triethylammonio)butane-1-sulfonate	N <sub>222</sub> C4S		-1.28
4-(1-methylimidazolium-3-yl)butane-1-sulfonate	C <sub>1</sub> ImC4S		-5.05
4-(1-vinylimidazolium-3-yl)butane-1-sulfonate	ViImC4S		-4.54
4-(1-methylpyrrolidinium-1-yl)butane-1-sulfonate	C <sub>1</sub> PyrC4S		-1.95
4-(1-ethylpiperidinium-1-yl)butane-1-sulfonate	C <sub>2</sub> PipC4S		-1.14

5

## 6 2.2. Methods

### 7 2.2.1. Determination of tie-lines and tie-line length data

8 The binodal curves of ABS composed of ZI + K<sub>2</sub>CO<sub>3</sub> + H<sub>2</sub>O studied in this work were previously  
9 reported by us.[20] In order to select an appropriate mixture composition for biomolecules  
10 partition experiments, one tie-line (TL) was determined for each system. Moreover, to reduce the  
11 possible influence which could arise from the different compositions of the phases, the partition  
12 studies were performed in mixture points leading to similar tie-line length (TLL), ranging from 65  
13 to 70. However, in the ABS composed of ViImC4S and C<sub>2</sub>PipC4S it was not possible to prepare  
14 TLs with a length higher than 50 and 61, respectively, due to ZI solubility limitations. Thus, the  
15 mixture points selected for biomolecules partition experiments and TLs determination were 25 wt

1 % of ZI + 25 wt % of  $K_2CO_3$  + 50 wt % of  $H_2O$  for  $N_{222}C_4S$ ,  $C_1ImC_4S$  and  $C_1PyrC_4S$  ZI and 22  
2 wt % of ZI + 25 wt % of  $K_2CO_3$  + 53 wt % of  $H_2O$  for  $C_2PipC_4S$  and  $ViImC_4S$  ZI. The TLs were  
3 determined at  $(298.15 \pm 1)$  K by a gravimetric method originally described by Merchuck et al.[25]  
4 and previously reported by us.[20]

5 The pH of both top and bottom phases that compose each ZI-based ABS studied in this work were  
6 determined at  $(298 \pm 1)$  K using a SevenExcellence™ pH/conductivity meter (Mettler Toledo  
7 (USA)).

8

### 9 *2.2.2. Biomolecules partition in ZI-based ABS*

10 An aqueous solution of each biomolecule was prepared at the following concentrations:  $5.15 \times 10^{-3}$   
11  $mol \cdot L^{-1}$  of caffeine,  $6.17 \times 10^{-3} mol \cdot L^{-1}$  of nicotine,  $4.90 \times 10^{-3} mol \cdot L^{-1}$  of *L*-tryptophan,  $0.55 \times 10^{-3}$   
12  $mol \cdot L^{-1}$  of *L*-tyrosine,  $1.82 \times 10^{-3} mol \cdot L^{-1}$  of *L*-phenylalanine,  $2.94 \times 10^{-3} mol \cdot L^{-1}$  of gallic acid and  
13  $2.97 \times 10^{-3} mol \cdot L^{-1}$  of vanillic acid. The ternary mixtures previously referred were gravimetrically  
14 prepared ( $\pm 10^{-4}$  g) at  $(298 \pm 1)$  K and atmospheric pressure. All phase forming components were  
15 weighed, vigorously stirred and then centrifuged for 30 min at 3500 rpm to ensure the complete  
16 phases separation and biomolecules partition. After the careful separation of both ZI- and salt-rich  
17 phases, the concentration of each biomolecule in each individual phase was determined through  
18 UV-Visible spectroscopy using a BioTeck Synergy HT microplate reader, at the following  
19 wavelengths: 273 nm for caffeine, 260 nm for nicotine, 279 nm for *L*-tryptophan, 275 nm for *L*-  
20 tyrosine, 258 nm for *L*-phenylalanine, 262 nm for gallic acid and 259 nm for vanillic acid.  
21 Biomolecules concentration was calculated using calibration curves previously established. In  
22 order to avoid possible interferences from the ZI and salt present in ABS phases, blank samples  
23 were prepared in the same mixture compositions by using pure water instead of aqueous solution  
24 of biomolecule.

25 Due to the high interferences derived from the  $ViImC_4S$  ZI in the quantification of gallic acid and  
26 *L*-phenylalanine by UV-Visible spectroscopy, the concentration of these biomolecules in the  
27 phases of  $ViImC_4S$ -based ABS were determined by using high performance liquid  
28 chromatography (HPLC) with diode array detector (DAD). A HPLC-DAD apparatus (Shimadzu,  
29 model PROMINENCE) with an analytical C18 reversed-phase column ( $250 \times 4.60$  mm), Kinetex  
30  $5 \mu m$  C18 100 Å, from Phenomenex, was used. The mobile phase consisted of ultrapure  $H_2O$  (+  
31 0.05 % trifluoroacetic acid (TFA)) as solvent A and methanol (+ 0.05 % TFA) as solvent B, with



1 the following gradient elution program: 0 min 15% B; 12 min 40% B; 14 min 74% B; 16 min 15%  
2 B; 25 min 15% B. This methodology was developed based on [26]. The flow rate used was 0.8  
3 mL/min, with an injection volume of 20  $\mu$ L. DAD was set at 258 and 262 nm for the quantification  
4 of *L*-phenylalanine and gallic acid, respectively. *L*-phenylalanine and gallic acid presented  
5 retention times of 7.8 and 4.8 minutes, respectively. Each sample was analyzed at least in duplicate.  
6 The column oven and the autosampler operated at 30 °C. Calibration curves were prepared using  
7 pure gallic acid and *L*-phenylalanine aqueous solutions.

8 All the experiments were performed in triplicate to determine the average partition coefficient (*K*),  
9 extraction efficiency percentage (*EE* %) and the corresponding standard deviations ( $\sigma$ ).  
10 Biomolecules partition coefficients ( $K_{Mol}$ ) and extraction efficiency percentage ( $EE_{Mol}$ %) were  
11 calculated according to the following equations:

$$12 \quad K_{Mol} = \frac{[Mol]_{ZI}}{[Mol]_{salt}}$$

13 (6)

$$14 \quad EE_{Mol}\% = \frac{m_{Mol}^{ZI}}{m_{Mol}^{ZI} + m_{Mol}^{salt}} \times 100$$

15 (7)

16 where  $[Mol]_{ZI}$  and  $[Mol]_{salt}$  are biomolecule concentration in ZI- and salt-rich phase, respectively,  
17 and  $m_{Mol}^{ZI}$  and  $m_{Mol}^{salt}$  are the biomolecule weight (g) determined in the ZI- and salt-rich phase,  
18 respectively. The biomolecules weight in each phase was determined as the product of the  
19 biomolecule concentration and phase volume

### 1 3. Results and discussion

2 The demixing of two-aqueous phases, and consequent formation of an ABS, occurs due to the  
3 competition of two species for the formation of hydration complexes.[5] Despite the strong ability  
4 of ZI to interact with water,[27,28] it was previously demonstrated that in ternary systems  
5 composed of ZI and salts, salts are capable of stronger hydration and are responsible for the salting-  
6 out effect and phase separation.[16,20] The liquid-liquid equilibrium of the ternary systems  
7 composed of C<sub>1</sub>ImC4S, ViImC4S, C<sub>1</sub>PyrC4S, N<sub>222</sub>C4S and C<sub>2</sub>PipC4S ZI + K<sub>2</sub>CO<sub>3</sub> + H<sub>2</sub>O were  
8 already reported.[20] The representation of the ternary phase diagrams can be found in the **Figure**  
9 **S1**. In this previous study it was proposed that water solubility of ZI is related with their ability to  
10 induce phase separation, with ZI of higher water solubility being less capable to form ABS, and  
11 the following trend was found when ZI were mixed with K<sub>2</sub>CO<sub>3</sub>: C<sub>1</sub>ImC4S < ViImC4S <  
12 C<sub>1</sub>PyrC4S < N<sub>222</sub>C4S ~ C<sub>2</sub>PipC4S.[20]

13 Since the goal of the present work is to understand how biomolecules partition occurs in ZI-salt-  
14 based ABS, K<sub>2</sub>CO<sub>3</sub> was selected as a moderate salting-out agent. Salts such as K<sub>3</sub>PO<sub>4</sub>, present a  
15 strong effect on the molecules partition due to their high charge density. This results in a strong  
16 ability to salt-out the compounds to the ZI-rich phases regardless the nature of ZI and,  
17 consequently, masking ZI influence on biomolecules partition.

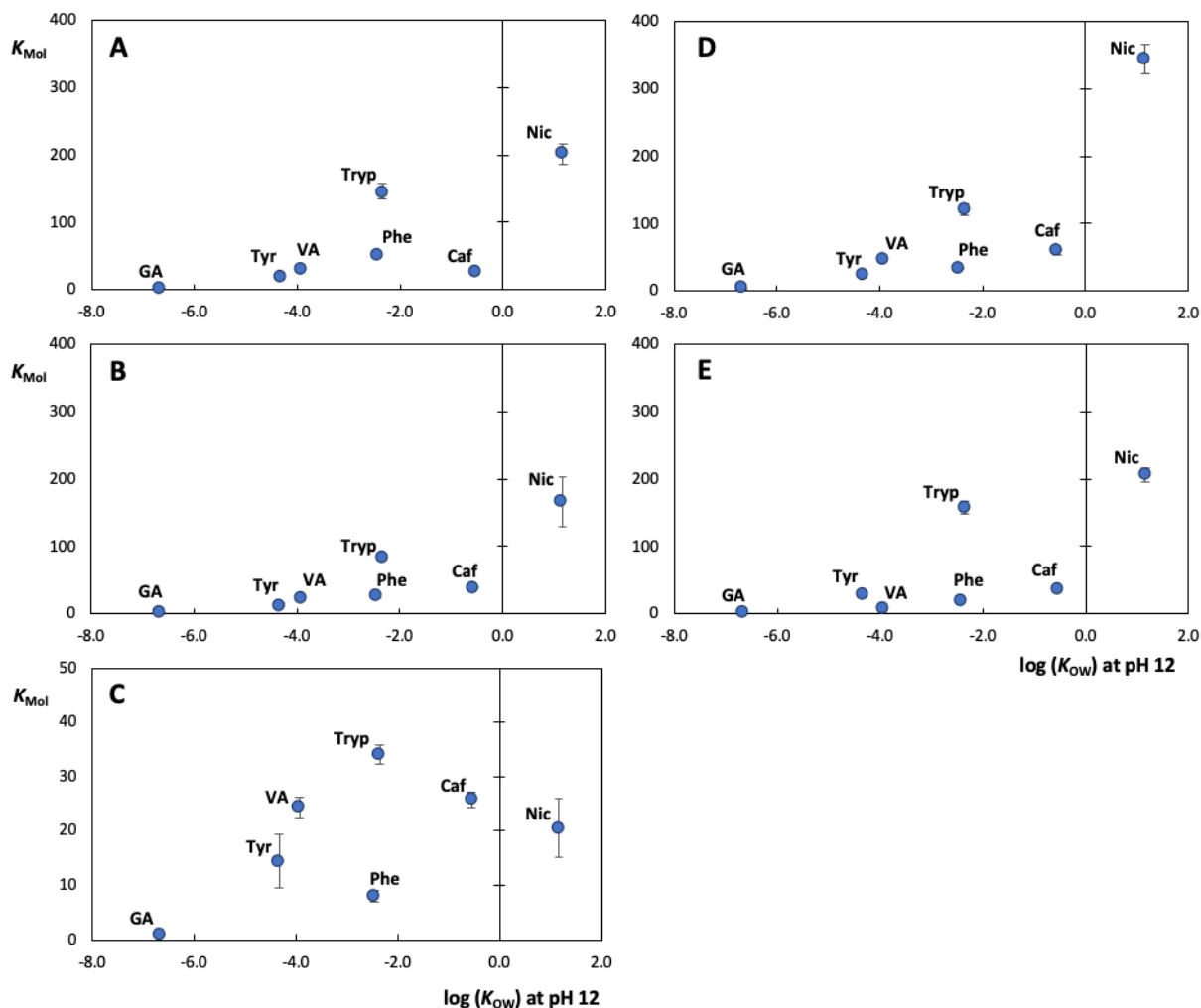
18 Considering the phase diagrams previously reported,[20] new TLs were determined for ZI +  
19 K<sub>2</sub>CO<sub>3</sub> + H<sub>2</sub>O ternary systems. To reduce the number of variables that may influence the partition  
20 of biomolecules, TLs of similar length were considered. The graphical representation of phase  
21 diagrams with selected mixture points as well as corresponding tie lines is presented in **Figure S2**.  
22 The obtained results for the ZI- and salt-rich phases, along with the composition of mixtures points  
23 and TLL of the coexisting phases are presented in **Table 3**. As expected, for all studied systems it  
24 was observed the formation of a top phase rich in ZI while the bottom phase is rich in salt. The pH  
25 values of the phases of these systems are in the alkaline region (~12).

26

1 **Table 3.** Experimental data for TLs, TLLs and phases pH for ABS composed of ZI + K<sub>2</sub>CO<sub>3</sub> +  
 2 H<sub>2</sub>O, determined at (298.15 ± 1) K and atmospheric pressure.

ZI	Weight fraction percentage (wt %)								TLL
	[salt] <sub>M</sub>	[ZI] <sub>M</sub>	[salt] <sub>salt</sub>	[ZI] <sub>salt</sub>	pH <sub>salt</sub>	[salt] <sub>ZI</sub>	[ZI] <sub>ZI</sub>	pH <sub>ZI</sub>	
N <sub>222</sub> C4S	25.01	25.00	48.48	0.05	11.8	3.86	47.48	12.4	65.12
C <sub>1</sub> ImC4S	24.98	25.02	38.73	2.17	12.0	2.62	62.18	12.4	70.03
ViImC4S	21.99	22.01	31.00	6.91	11.8	5.19	50.17	12.1	50.37
C <sub>1</sub> PyrC4S	24.95	25.00	39.93	2.11	12.0	1.52	60.80	12.6	70.15
C <sub>2</sub> PipC4S	22.01	21.99	34.68	2.21	11.8	1.50	54.01	12.1	61.52

3  
 4 The effect of the ZI nature in the partition of biomolecules was here evaluated by measuring the  
 5 partition coefficients of caffeine, nicotine, gallic acid, vanillic acid, *L*-tryptophan, *L*-tyrosine and  
 6 *L*-phenylalanine in the biphasic systems reported in **Table 3**. The obtained results are presented in  
 7 **Figures 1** to **4**. Details on biomolecules partition coefficients and extraction efficiencies  
 8 experimental data and respective standard deviations are given in **Tables S2** and **S3**.  
 9



1  
 2 **Figure 1.** Partition coefficient,  $K_{Mol}$ , of caffeine (Caf), nicotine (Nic), gallic acid (GA), vanillic  
 3 acid (VA), *L*-tryptophan (Tryp), *L*-tyrosine (Tyr) and *L*-phenylalanine (Phe) as a function of their  
 4 octanol-water partition coefficients,  $\log(K_{Ow})$ , at pH 12[23] in ABS composed of  $K_2CO_3$  and the  
 5 following ZI: (A)  $N_{222}C_{4S}$ , (B)  $C_1ImC_{4S}$ , (C)  $ViImC_{4S}$ , (D)  $C_1PyrC_{4S}$  and (E)  $C_2PipC_{4S}$ .

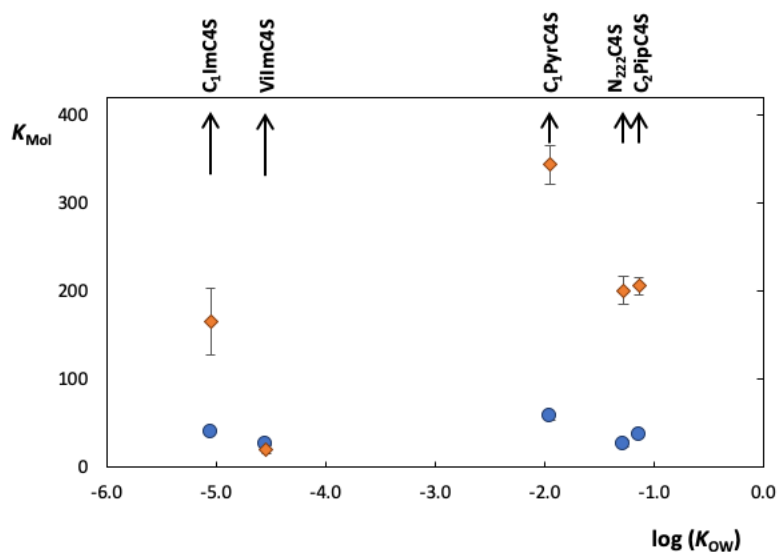
6  
 7 In **Figure 1**, biomolecules partition coefficients are represented as function of their octanol-water  
 8 partition coefficients ( $\log$ ) at pH 12 for each ABS. Since most of the studied biomolecules suffers  
 9 speciation at the pH of the systems (pH 12),  $K_{Ow}$  at this pH were estimated and used, instead of  
 10 the usual octanol-water partition coefficients of neutral molecules. All  $K_{Mol}$  values are higher than  
 11 1, meaning that all biomolecules, independently of the type of ZI that compose the system, have a  
 12 preferential partition to the ZI-rich phase. In what concerns extraction efficiencies (*cf.* **Table S2**),  
 13 most of the biomolecules presented high  $EE_{Mol}$  % values ( $> 80$  %), while gallic acid showed a  
 14 lower capability to be extracted to the ZI-rich phase ( $EE_{Mol}$  % ranges between 39 to 85 %). From

1 **Figure 1**, it is also possible to observe a trend valid for most systems: the higher is the octanol-  
2 water partition coefficient of the solute (at pH 12), the higher its partition for the ZI-rich phase.  
3 Gallic acid ( $K_{OW}$  (pH 12) = -6.66) is the biomolecule which presents the lower partition  
4 coefficients in all systems, while nicotine ( $K_{OW}$  (pH 12) = 1.16) is the compound with the higher  
5 capacity to partition to the ZI-rich phase, with the sole exception of the system composed of  
6 ViImC4S, in which *L*-tryptophan ( $K_{OW}$  (pH 12) = -2.35) presents the highest value of  $K_{Mol}$ . These  
7 results are in good agreement with data previously reported for other types of ABS, including ZI-  
8 and IL-based ABS.[20–22,29] In fact, despite specific interactions that may occur, it has been  
9 observed that the hydrophilic/hydrophobic nature of the solutes controls their preferential partition.  
10 In this work, the impact of the hydrophilic/hydrophobic nature of each solute is patent in the trends  
11 observed in **Figure 1**, with all possible interferences which could arise from the different  
12 compositions of the phases being taken into account, since all ternary mixtures were prepared for  
13 TLs with similar TLLs. Nevertheless, it is possible to observe some deviations to these trends,  
14 namely in the behavior of some biomolecules and in the ZI influence on biomolecules partition.  
15 These deviations will be discussed in detail below.

16 The lowest values of  $K_{Mol}$  were observed in the system composed of ViImC4S +  $K_2CO_3$  +  $H_2O$ .  
17 While in the remaining systems the  $K_{Mol}$  reach values  $> 150$ , when the system is composed by the  
18 ZI ViImC4S, the partition coefficient values range only between 1.15 and 34. Furthermore, as  
19 shown by the data presented in **Figure 1C**, this is the only system in which it is not possible to  
20 clearly distinguish a tendency between the  $K_{Mol}$  and  $\log(K_{OW})$  of the molecules as described above.  
21 Due to ZI solubility limitations this system is the one which has the smallest TLL – *cf.* **Table 3**.  
22 This may justify the lower partition of these biomolecules. It is well known that a lower TLL  
23 means a higher similarity between the phases that compose the system and a harder separation of  
24 the biomolecules between the phases.[5,21] This seems to have a higher impact on the partition of  
25 biomolecules with higher octanol-water partition coefficient, such as nicotine – *cf.* **Figure 1C**.

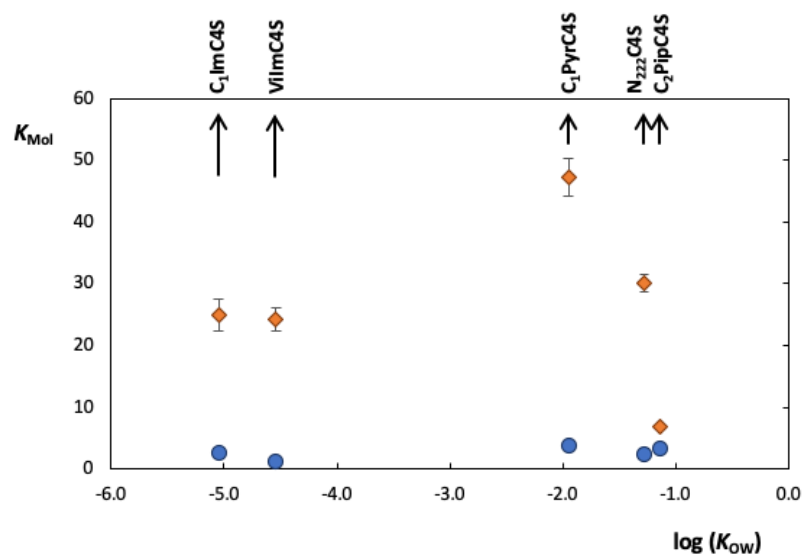
26 To facilitate the interpretation and discussion of the behavior of each biomolecule, in **Figures 2** to  
27 **4** are presented the  $K_{Mol}$  values obtained for each family of biomolecules – alkaloids, phenolic  
28 compounds and amino acids – as a function of ZI  $\log(K_{OW})$ . In **Figure 2** are presented the results  
29 obtained for the alkaloids nicotine and caffeine. Nicotine exhibited very high  $K_{Mol}$  values (higher  
30 than 100 in most systems), while caffeine presents relatively low partition to ZI-rich phase and  
31 with smaller variations with the type of ZI that compose the system ( $K_{Mol}$  range from 26 to 58). As

1 previously referred, the differences observed between the two alkaloids can be explained based on  
2 their higher or lower affinity for the most hydrophobic phase. However, through the data presented  
3 in **Figure 2**, it seems clear that the ZI hydrophobicity/hydrophilicity is not the only variable  
4 influencing the partition of the alkaloids to the ZI-rich phase. Considering nicotine, its favorable  
5 partition to ZI-rich phase follows the order: ViImC4S < C<sub>1</sub>ImC4S < N<sub>222</sub>C4S ~ C<sub>2</sub>PipC4S <  
6 C<sub>1</sub>PyrC4S, while caffeine presents the following trend: ViImC4S ~ N<sub>222</sub> < C<sub>2</sub>PipC4S ~ C<sub>1</sub>ImC4S  
7 < C<sub>1</sub>PyrC4S. Despite the differences, it is possible to conclude that the ZI influence, in general, it  
8 is similar for both alkaloids. With the exception of ViImC4S-based ABS in which the low TLL may  
9 have a high impact on alkaloids partition, resulting in lower  $K_{Mol}$  values, C<sub>1</sub>PyrC4S is the only ZI  
10 that is out of the expected trend. Nicotine has *N*-methylpyrrolidine ring linked to a pyridine group.  
11 The structural similarity between nicotine and the C<sub>1</sub>PyrC4S ZI could result in specific interactions  
12 and justify the high ability of this system to extract nicotine. Furthermore, caffeine partition in  
13 systems composed of the same ZI and K<sub>3</sub>PO<sub>4</sub> (a stronger salting-out agent than K<sub>2</sub>CO<sub>3</sub>) was  
14 previously evaluated by us.[20] In this previous work the system composed of C<sub>1</sub>PyrC4S also  
15 presented the highest ability to extract caffeine to the ZI-rich phase, while N<sub>222</sub>C4S showed the  
16 worst result.[20] It was proposed that this behavior was related with the absence of favorable  $\pi$ - $\pi$   
17 interactions between the biomolecule and the ammonium-based ZI. However, the results presented  
18 here suggest that, despite specific interactions have an important role in the biomolecules partition,  
19 several other effects can influence this behavior.



1  
2 **Figure 2.** Alkaloids partition as function of octanol-water partition coefficients (log) of ZI in ABS  
3 composed of ZI + K<sub>2</sub>CO<sub>3</sub> + H<sub>2</sub>O: caffeine (●) and nicotine (◆).

4 The results obtained for the partition of the phenolic compounds – gallic acid and vanillic acid –  
5 as a function of the log(K<sub>OW</sub>) of each ZI, are presented in **Figure 3**. Among all the families of  
6 biomolecules studied in this work, phenolic compounds were those that present the lower partition  
7 coefficients ranging between 6.92 to 47 and 1.15 to 3.7, for vanillic acid and gallic acid  
8 respectively. Vanillic acid differs from gallic acid on the number of hydroxyl groups present on  
9 the aromatic ring and it is comparatively more hydrophobic (*cf.* **Table 1**), justifying the higher  
10  $K_{Mol}$  values obtained. It was previously reported that the pH of the medium has a significant impact  
11 on the partition of phenolic compounds due to their speciation.[30] At the alkaline pH of the  
12 studied ZI-based ABS, both phenolic compounds exist mostly in the form of their charged  
13 conjugated bases. It is expected that these charged species preferentially partition to the most  
14 hydrophilic phases in order to ensure effective solvation of these ions. This was previously  
15 reported by Cláudio et al.[30] in IL-based ABS. Even in presence of a strong salting-out agent  
16 such as K<sub>3</sub>PO<sub>4</sub>, gallic acid was extracted mainly to salt-rich phase ( $K < 1$ ) in alkaline IL-based  
17 ABS.[30] However, here both phenolic compounds still present  $K_{Mol} > 1$ , meaning a preferential  
18 partition to the ZI-rich phase. These results suggest that ZI-based ABS could be a more suitable  
19 alternative to extract phenolic compounds in alkaline medium than IL-based ABS. Nevertheless,  
20 the obtained partition coefficients are still much lower for phenolic compounds when compared to  
21 the remaining biomolecules.



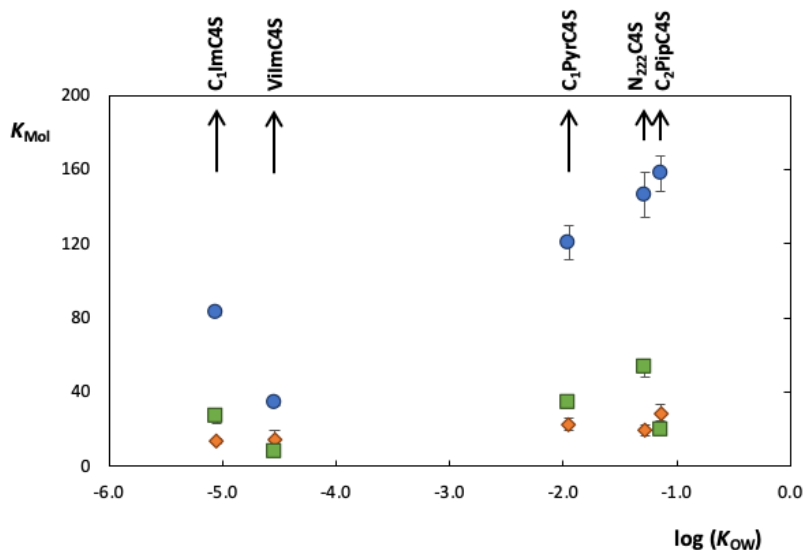
1  
 2 **Figure 3.** Phenolic compounds partition as function of octanol-water partition coefficients (log)  
 3 of ZI in ABS composed of ZI + K<sub>2</sub>CO<sub>3</sub> + H<sub>2</sub>O: gallic acid (●) and vanillic acid (◆).

4 In what concerns the influence of ZI nature in the partition of the phenolic compounds, it is not  
 5 possible to observe a well-defined trend in the data presented in the **Figure 3**. Nevertheless,  
 6 considering the hydrophilic character of phenolic compounds at alkaline pH, it is not expected to  
 7 see an improvement on their partition to ZI-rich phase with the increase of ZI hydrophobicity (high  
 8 log(K<sub>OW</sub>)). Thus, the decrease observed in vanillic acid partition coefficient in the systems  
 9 composed of the ZI C<sub>1</sub>PyrC<sub>4</sub>S, N<sub>222</sub>C<sub>4</sub>S and C<sub>2</sub>PipC<sub>4</sub>S could be related with its lower affinity for  
 10 more hydrophobic phases.

11 In **Figure 4** are presented the experimental data obtained for the partition of the amino acids *L*-  
 12 tryptophan, *L*-tyrosine and *L*-phenylalanine. As expected, and previously discussed, K<sub>Mol</sub> values  
 13 follow the trend  $K_{\text{Tyr}} > K_{\text{Phe}} > K_{\text{Tyr}}$  which is based on the differences in the hydrophobicity of these  
 14 amino acids – *cf.* **Table 1** and **Figure 1**. From the data presented in **Figure 4** it is also clear that  
 15 K<sub>Mol</sub> of the amino acids increases with the hydrophobicity of ZI – higher log (K<sub>OW</sub>) – meaning that  
 16 amino acids partition in ZI-based ABS is by the hydrophobic/hydrophilic character of the ZI that  
 17 compose the system. In fact, considering the partition coefficients obtained for *L*-tryptophan, it is  
 18 possible to observe that this increases regardless ZI nature – aromatic, non-aromatic, quaternary  
 19 ammonium, etc. – being mainly dependent on the log (K<sub>OW</sub>) of the ZI. This is in good agreement  
 20 with data previously reported for amino acids partition in polymer-based ABS, in which it was  
 21 demonstrated that amino acids partition is mainly driven by hydrophobic effects.[21,31]



1 Nevertheless, *L*-tryptophan showed exceptionally high  $K_{Mol}$  values resulting in its complete  
2 partition into the ZI-rich phase. Its partition was even higher than the partition of caffeine that  
3 present a high hydrophobic character (*cf.* **Table 1**), as can be observed in **Figure 1**.



4  
5 **Figure 4.** Amino acids partition coefficients as function of octanol-water partition coefficients  
6 (log) of ZI in ABS composed of ZI +  $K_2CO_3$  +  $H_2O$ : *L*-tryptophan (●), *L*-tyrosine (◆) and *L*-  
7 phenylalanine (■).

8 These results are also similar to what was previously reported for *L*-tryptophan extraction in ABS  
9 composed of IL and salts, [5,32] suggesting that, despite the structural differences between IL and  
10 ZI, there are some similarities on the way how both type of compounds driven the partition of  
11 biomolecules in ABS.

#### 1 **4. Conclusions**

2 The ability of ABS composed of ZI and  $K_2CO_3$  to partition 7 different biomolecules - 2 phenolic  
3 compounds, 2 alkaloids and 3 amino acids - was studied in this work. By a careful selection of the  
4 ternary mixture points used in the extractions (similar TLL) it was possible to evaluate the  
5 influence of ZI nature in the biomolecules partition without relevant interferences that could result  
6 from the differences observed in the systems phases composition. Furthermore,  $K_2CO_3$  was  
7 selected as a moderate salting-out agent to avoid strong salting-out effects on the biomolecules  
8 partition. In all studied systems, partition coefficients were always higher than 1, meaning that all  
9 biomolecules present a favorable partition to the ZI-rich phase. The obtained results show that the  
10 biomolecules partition is mainly ruled by hydrophobic/hydrophilic effects and only in some cases  
11 specific interactions between the biomolecules and the ZI have some influence. Thus, the octanol-  
12 water partition coefficients of both biomolecules and ZI could be used in the explanation of the  
13 obtained results. In general the higher is the octanol-water partition coefficient of the biomolecules,  
14 considering their speciation at the pH of the studied systems (pH ~ 12), the higher are their partition  
15 coefficients. Moreover, when in the presence of more hydrophobic biomolecules, namely nicotine  
16 and *L*-tryptophan, their partition increases with the  $K_{OW}$  of the ZI, while the opposite trend is  
17 observed with more hydrophilic compounds, such as phenolic compounds. Despite the structural  
18 differences between IL and ZI, the obtained results suggest that ZI behave in a similar way to IL,  
19 still conferring to the system phases some properties that make these systems suitable alternatives  
20 for the extraction of more hydrophilic compounds, such as phenolic compounds at alkaline  
21 conditions.  
22

1 **5. Acknowledgements**

2 This work was developed within the scope of the project CICECO-Aveiro Institute of Materials,  
3 UIDB/50011/2020 & UIDP/50011/2020, financed by national funds through the Foundation for  
4 Science and Technology/MCTES. This work is funded by national funds through FCT – Fundação  
5 para a Ciência e a Tecnologia, I.P., under the Scientific Employment Stimulus - Individual Call -  
6 CEECIND/00831/2017 - under the CEEC Individual 2017. Authors would like acknowledge  
7 funding support from Indo-Portuguese Program for Cooperation in Science and Technology  
8 through DST/INT/Portugal/P-01/2017, Department of Science and Technology, India. A.  
9 Basaiahgari and R.L. Gardas would like to acknowledge IIT Madras for financial support and S.K.  
10 Yadav for synthesis of some of the ZIs.

11

12

## 6. References

- [1] P.A. Albertsson, Partition of cell particles and macromolecules, 3rd ed., Wiley, New York, 1986.
- [2] M.G. Bogdanov, Alternative solvents for natural products extraction, Eds, Springer, Berlin, 2014.
- [3] E. V. Capela, J.A.P. Coutinho, M.G. Freire, Application of Ionic Liquids in Separation and Fractionation Processes, *Encycl. Sustain. Sci. Technol.*, Springer New York, 2018: pp. 1–29. [https://doi.org/10.1007/978-1-4939-2493-6\\_1005-1](https://doi.org/10.1007/978-1-4939-2493-6_1005-1).
- [4] G. Johansson, Partition of salts and their effects on partition of proteins in a dextran-poly(ethylene glycol)-water two-phase system, *BBA - Protein Struct.* 221 (1970) 387–390. [https://doi.org/10.1016/0005-2795\(70\)90283-7](https://doi.org/10.1016/0005-2795(70)90283-7).
- [5] M.G. Freire, A.F.M. Cláudio, J.M.M. Araújo, J.A.P. Coutinho, I.M. Marrucho, J.N. Canongia Lopes, L.P.N. Rebelo, Aqueous biphasic systems : a boost brought about by using ionic liquids, *Chem Soc Rev.* 41 (2012) 4966–4995. <https://doi.org/10.1039/c2cs35151j>.
- [6] K.E. Gutowski, G.A. Broker, H.D. Willauer, J.G. Huddleston, R.P. Swatloski, J.D. Holbrey, R.D. Rogers, Controlling the aqueous miscibility of ionic liquids: aqueous biphasic systems of water-miscible ionic liquids and water-structuring salts for recycle, metathesis, and separations, *J. Am. Chem. Soc.* 125 (2003) 6632–6633. <https://doi.org/10.1021/ja0351802>.
- [7] N. Schaeffer, H. Passos, M. Gras, V. Mogilireddy, J.P. Leal, G. Pérez-Sánchez, J.R.B. Gomes, I. Billard, N. Papaiconomou, J.A.P. Coutinho, Mechanism of ionic-liquid-based acidic aqueous biphasic system formation, *Phys. Chem. Chem. Phys.* 20 (2018) 9838–9846. <https://doi.org/10.1039/c8cp00937f>.
- [8] M.G. Freire, C.L.S. Louros, L.P.N. Rebelo, J.A.P. Coutinho, Aqueous biphasic systems composed of a water-stable ionic liquid + carbohydrates and their applications, *Green Chem.* 13 (2011) 1536–1545. <https://doi.org/10.1039/c1gc15110j>.
- [9] V.P. Priyanka, A. Basaiahgari, R.L. Gardas, Enhanced partitioning of tryptophan in aqueous biphasic systems formed by benzyltrialkylammonium based ionic liquids: Evaluation of thermophysical and phase behavior, *J. Mol. Liq.* 247 (2017) 207–214. <https://doi.org/10.1016/j.molliq.2017.09.111>.
- [10] N. Schaeffer, M. Gras, H. Passos, V. Mogilireddy, C.M.N. Mendonça, E. Pereira, E.

- 1 Chainet, I. Billard, J.A.P. Coutinho, N. Papaiconomou, Synergistic Aqueous Biphasic  
2 Systems: A New Paradigm for the “One-Pot” Hydrometallurgical Recovery of Critical  
3 Metals, ACS Sustain. Chem. Eng. 7 (2019) 1769–1777.  
4 <https://doi.org/10.1021/acssuschemeng.8b05754>.
- 5 [11] S.P.M. Ventura, F.A. E Silva, M. V. Quental, D. Mondal, M.G. Freire, J.A.P. Coutinho,  
6 Ionic-Liquid-Mediated Extraction and Separation Processes for Bioactive Compounds:  
7 Past, Present, and Future Trends, Chem. Rev. 117 (2017) 6984–7052.  
8 <https://doi.org/10.1021/acs.chemrev.6b00550>.
- 9 [12] S. Ji, Y. Wang, X. Shao, C. Zhu, Y. Lin, S. Gao, D. Tang, Extraction and purification of  
10 triterpenoid saponins from licorice by ionic liquid based extraction combined with in situ  
11 alkaline aqueous biphasic systems, Sep. Purif. Technol. 247 (2020) 116953.  
12 <https://doi.org/10.1016/j.seppur.2020.116953>.
- 13 [13] A.I. Pratiwi, T. Yokouchi, M. Matsumoto, K. Kondo, Extraction of succinic acid by aqueous  
14 two-phase system using alcohols/salts and ionic liquids/salts, Sep. Purif. Technol. 155  
15 (2015) 127–132. <https://doi.org/10.1016/j.seppur.2015.07.039>.
- 16 [14] Y. Pei, J. Wang, K. Wu, X. Xuan, X. Lu, Ionic liquid-based aqueous two-phase extraction  
17 of selected proteins, Sep. Purif. Technol. 64 (2009) 288–295.  
18 <https://doi.org/10.1016/j.seppur.2008.10.010>.
- 19 [15] A.M. Ferreira, H. Passos, A. Okafuji, A.P.M. Tavares, H. Ohno, M.G. Freire, J.A.P.  
20 Coutinho, An integrated process for enzymatic catalysis allowing product recovery and  
21 enzyme reuse by applying thermoreversible aqueous biphasic systems, Green Chem. 20  
22 (2018) 1218–1223. <https://doi.org/10.1039/c7gc03880a>.
- 23 [16] A.M. Ferreira, H. Passos, A. Okafuji, M.G. Freire, J.A.P. Coutinho, H. Ohno, Designing  
24 the thermal behaviour of aqueous biphasic systems composed of ammonium-based  
25 zwitterions, Green Chem. 19 (2017) 4012–4016. <https://doi.org/10.1039/c7gc02262j>.
- 26 [17] M. Yoshizawa, M. Hirao, K. Ito-Akita, H. Ohno, Ion conduction in zwitterionic-type molten  
27 salts and their polymers, J. Mater. Chem. 11 (2001) 1057–1062.  
28 <https://doi.org/10.1039/b101079o>.
- 29 [18] P. Fischer, H. Rehage, B. Grüning, Linear flow properties of dimer acid betaine solutions  
30 with and without changes ionic strength, J. Phys. Chem. B. 106 (2002) 11041–11046.  
31 <https://doi.org/10.1021/jp0127263>.

- 1 [19] A. Wu, Y. Gao, L. Zheng, Zwitterionic amphiphiles: Their aggregation behavior and  
2 applications, *Green Chem.* 21 (2019) 4290–4312. <https://doi.org/10.1039/c9gc01808e>.
- 3 [20] A. Basaiahgari, S.K. Yadav, R.L. Gardas, Zwitterions as novel phase forming components  
4 of aqueous biphasic systems, *Pure Appl. Chem.* 91 (2019) 1279–1294.  
5 <https://doi.org/10.1515/pac-2018-0921>.
- 6 [21] R. de C.S. Sousa, M.M. Pereira, M.G. Freire, J.A.P. Coutinho, Evaluation of the effect of  
7 ionic liquids as adjuvants in polymer-based aqueous biphasic systems using biomolecules  
8 as molecular probes, *Sep. Purif. Technol.* 196 (2018) 244–253.  
9 <https://doi.org/10.1016/j.seppur.2017.07.018>.
- 10 [22] F.O. Farias, H. Passos, M.G. Sanglard, L. Igarashi-Mafra, J.A.P. Coutinho, M.R. Mafra,  
11 Designer solvent ability of alcohols in aqueous biphasic systems composed of deep eutectic  
12 solvents and potassium phosphate, *Sep. Purif. Technol.* 200 (2018) 84–93.  
13 <https://doi.org/10.1016/j.seppur.2018.02.029>.
- 14 [23] MarvinSketch 20.3.0, 2020, ChemAxon (<http://www.chemaxon.com>).
- 15 [24] ChemSpider - The free chemical database, (2015). [www.chemspider.com](http://www.chemspider.com).
- 16 [25] J.C. Merchuk, B. a Andrews, J. a Asenjo, Aqueous two-phase systems for protein  
17 separation. Studies on phase inversion., *J. Chromatogr. B. Biomed. Sci. Appl.* 711 (1998)  
18 285–93.
- 19 [26] M.L. Mesquita, W.F. Leão, M.R.A. Ferreira, J.E. de Paula, L.S. Espindola, L.A.L. Soares,  
20 Reversed-phase-liquid chromatography method for separation and quantification of gallic  
21 acid from hydroalcoholic extracts of *Qualea grandiflora* and *Qualea parviflora*,  
22 *Pharmacogn. Mag.* 11(Suppl2) (2015) S316-S321. [https://doi.org/10.4103/0973-](https://doi.org/10.4103/0973-1296.166062)  
23 [1296.166062](https://doi.org/10.4103/0973-1296.166062).
- 24 [27] Q. Shao, Y. He, A.D. White, S. Jiang, Difference in hydration between carboxybetaine and  
25 sulfobetaine, *J. Phys. Chem. B.* 114 (2010) 16625–16631.  
26 <https://doi.org/10.1021/jp107272n>.
- 27 [28] Y. He, J. Hower, S. Chen, M.T. Bernards, Y. Chang, S. Jiang, Molecular simulation studies  
28 of protein interactions with zwitterionic phosphorylcholine self-assembled monolayers in  
29 the presence of water, *Langmuir.* 24 (2008) 10358–10364.  
30 <https://doi.org/10.1021/la8013046>.
- 31 [29] A.M. Ferreira, H. Passos, A. Okafuji, M.G. Freire, J.A.P. Coutinho, H. Ohno, Designing

- 1 the thermal behaviour of aqueous biphasic systems composed of ammonium-based  
2 zwitterions, *Green Chem.* 19 (2017) 4012–4016. <https://doi.org/10.1039/c7gc02262j>.
- 3 [30] A.F.M. Cláudio, A.M. Ferreira, C.S.R. Freire, A.J.D. Silvestre, M.G. Freire, J.A.P.  
4 Coutinho, Optimization of the gallic acid extraction using ionic-liquid-based aqueous two-  
5 phase systems, *Sep. Purif. Technol.*, 97 (2012) 142–149.  
6 <https://doi.org/10.1016/j.seppur.2012.02.036>.
- 7 [31] B.Yu. Zaslavsky, N.M. Mestechkina, L.M. Miheeva, S. V. Rogozhin, Measurements of  
8 relative hydrophobicity of amino acid side-chains by partition in an aqueous two-phase  
9 polymeric system: hydrophobicity scale for non-polar and inogenic side-chains, *J.*  
10 *Chromatogr. A.* 201 (1982) 21–28. [https://doi.org/10.1016/s0021-9673\(01\)84003-6](https://doi.org/10.1016/s0021-9673(01)84003-6).
- 11 [32] C.M.S.S. Neves, S.P.M. Ventura, M.G. Freire, I.M. Marrucho, J.A.P. Coutinho, Evaluation  
12 of cation influence on the formation and extraction capability of ionic-liquid-based aqueous  
13 biphasic systems, *J. Phys. Chem. B.* 113 (2009) 5194–5199.  
14 <https://doi.org/10.1021/jp900293v>.